

CORE LABORATORIES, INC.

Petroleum Reservoir Engineering

DALLAS, TEXAS 75207

February 22, 1971

RESERVOIR FLUID ANALYSIS

Phillips Petroleum Company - Norway
P. O. Box 72
Stavanger, Norway

Attention: Mr. P. W. Reynolds

Subject: Reservoir Fluid Studies
2/4-4AX Well
DST Nos. 1 and 4
Ekofisk Field
North Sea, Norway
Our File Numbers: RFL 6653 and
RFL 6654

Gentlemen:

Samples of separator liquid and vapor collected during DST No. 1 and DST No. 4 were submitted to our laboratory in Dallas for use in reservoir fluid studies. Presented on the following pages are the results of these studies as requested by Phillips Petroleum Company - Norway.

After correction for the gas gravity and supercompressibility factors, the separator gas-liquid ratio during DST No. 1 was calculated to be 1222 standard cubic feet of separator gas per barrel of separator liquid at 570 psig and 74° F. This ratio was used in conjunction with the measured compositions of the separator products to calculate the composition of the well stream material. The separator products were then physically re-combined in this producing gas-liquid ratio and the bubble point pressure of this resulting fluid was measured to be 5886 psig at the reservoir temperature of 266° F. The results of the tests that were performed using these separator products are presented on pages one through four of the report.

The producing gas-liquid ratio during DST No. 4 was calculated to be 1703 standard cubic feet of separator gas per barrel of separator liquid. After

Phillips Petroleum Company - Norway
2/4-4AX Well, DST Nos. 1 and 4

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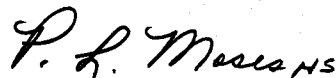
physically recombining the separator products to this producing gas-liquid ratio the resulting fluid was determined to have a bubble point pressure of 6228 psig at 258° F. The results of the tests performed on these samples are presented on pages five through eight of the report.

A preliminary report issued November 4, 1970 contained the results of a hydrocarbon analyses of the separator products, the calculated well stream compositions and the bubble point pressure of each mixture at reservoir temperature. At that time we were requested to hold all remaining gas and liquid samples collected during these tests until these preliminary data had been fully analyzed by Phillips Petroleum Company - Norway. On February 12, 1971 we were instructed by telex that no further testing would be required using these samples, and that any remaining gas and liquid samples could be discarded at this time.

As always, it has been our pleasure to cooperate with Phillips Petroleum Company - Norway in performing these studies. If you have any questions regarding these data, please do not hesitate to contact us.

Very truly yours,

Core Laboratories, Inc.
Reservoir Fluid Analysis



P. L. Moses
Manager

PLM:HS:dl

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File RFL 6653

Company Phillips Petroleum Co. - Norway Date Sampled August 10, 1970

Well 2/4-4AX, DST No. 1 County _____

Field Ekofisk State North Sea, Norway

FORMATION CHARACTERISTICS

Formation Name	<u>Danian</u>
Date First Well Completed	<u>August 10</u> , 19 <u>70</u>
Original Reservoir Pressure	<u>7085</u> PSIG @ <u>10530</u> Ft.
Original Produced Gas-Liquid Ratio	_____ SCF/Bbl
Production Rate	_____ Bbls/Day
Separator Pressure and Temperature	_____ PSIG _____ ° F
Liquid Gravity at 60° F.	<u>36.0</u> _____ ° API
Datum	_____ Ft. Subsea

WELL CHARACTERISTICS

Elevation	<u>89 RKB</u> _____ Ft.
Total Depth	<u>10848</u> _____ Ft.
Producing Interval	<u>10380-10510</u> _____ Ft.
Tubing Size and Depth	<u>2-1/2</u> In. to <u>10321</u> Ft.
Open Flow Potential	_____ MMSCF/Day
Last Reservoir Pressure	_____ PSIG @ _____ Ft.
Date	_____, 19 _____
Reservoir Temperature	<u>266</u> ° F. @ <u>10445</u> Ft.
Status of Well	<u>Flowing DST 1</u>
Pressure Gauge	_____

SAMPLING CONDITIONS

Flowing Tubing Pressure	<u>4120</u> _____ PSIG
Flowing Bottom Hole Pressure	_____ PSIG
Primary Separator Pressure	<u>570</u> _____ PSIG
Primary Separator Temperature	<u>74</u> _____ ° F.
Secondary Separator Pressure	_____ PSIG
Secondary Separator Temperature	_____ ° F.
Field Stock Tank Liquid Gravity	_____ ° API @ 60° F.
Primary Separator Gas Production Rate	<u>909.0</u> _____ MSCF/Day
Pressure Base	<u>14.696</u> PSIA
Temperature Base	<u>60</u> ° F.
Compressibility Factor (F _{pv})	<u>1.0576</u>
Gas Gravity (Laboratory)	<u>0.663</u>
Gas Gravity Factor (F _g)	<u>1.2281</u>
Separator Liquid Production Rate @ 74° F. & 570 psig	<u>744</u> _____ Bbls/Day
Primary Separator Gas/Separator Liquid Ratio	<u>1222</u> _____ SCF/Bbl
or	_____ Bbls/MMSCF

Core Laboratories, Inc., Engineer

REMARKS:

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Well 2/4-4AX, DST No. 1

Hydrocarbon Analyses of Separator Products and Calculated Well Stream

<u>Component</u>	<u>Separator Liquid Mol Per Cent</u>	<u>Separator Gas Mol Per Cent</u>	<u>GPM</u>	<u>Well Stream * Mol Per Cent</u>
Hydrogen Sulfide				
Carbon Dioxide	0.43	1.51		1.11
Nitrogen	0.04	0.34		0.23
Methane	14.12	85.65		59.17
Ethane	6.83	8.27	2.083	7.74
Propane	6.86	2.76	0.758	4.28
iso-Butane	1.50	0.31	0.101	0.75
n-Butane	4.35	0.63	0.198	2.01
iso-Pentane	1.52	0.12	0.044	0.64
n-Pentane	2.07	0.15	0.054	0.86
Hexanes	5.92	0.11	0.045	2.26
Heptanes plus	56.36	0.15	0.068	20.95
	<u>100.00</u>	<u>100.00</u>	<u>3.351</u>	<u>100.00</u>

Properties of Heptanes plus

API gravity @ 60° F.	<u>33.3</u>		
Specific gravity @ 60/60° F.	<u>0.8584</u>		<u>0.858</u>
Molecular weight	<u>228</u>	<u>103</u>	<u>227</u>

Calculated separator gas gravity (air = 1.000) = 0.663

Calculated gross heating value for separator gas = 1136 BTU

per cubic foot of dry gas @ 14.696 psia and 60° F.

Primary separator gas collected @ 570 psig and 74 °F.

Primary separator liquid collected @ 570 psig and 74 °F.

Primary separator gas/separator liquid ratio 1222 SCF/Bbl @ 74° F.

* Bubble point pressure = 5886 psig at 266° F.

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Well 2/4-4AX, DST No. 1

VOLUMETRIC DATA OF Reservoir Fluid SAMPLE

1. Saturation pressure (bubble-point pressure) 5886 PSIG @ 266 °F.

2. Thermal expansion of saturated oil @ 7500 PSI = $\frac{V @ 266 \text{ } ^\circ\text{F}}{V @ 72 \text{ } ^\circ\text{F}}$ = 1.14249

3. Compressibility of saturated oil @ reservoir temperature: Vol/Vol/PSI:

From 7500 PSI to 6500 PSI = 20.40 x 10⁻⁶

From 6500 PSI to 6200 PSI = 24.32 x 10⁻⁶

From 6200 PSI to 5886 PSI = 25.62 x 10⁻⁶

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Well 2/4-4AX, DST No. 1

Pressure-Volume Relations of Reservoir Fluid at 266° F.

<u>Pressure,</u> <u>PSIG</u>	<u>Relative</u> <u>Volume</u>
7500	0.9646
7000	0.9742
6500	0.9847
6300	0.9790
6200	0.9920
6100	0.9943
6000	0.9968
5900	0.9996
<u>5886</u>	1.0000
5836	1.0025
5796	1.0045
5696	1.0095
5510	1.0194
5178	1.0396
4887	1.0600
4528	1.0907
4147	1.1321
3698	1.1947
3264	1.2789
2767	1.4162
2315	1.6073
1737	2.0140
1274	2.6539
888	3.7017

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Company Phillips Petroleum Co. - Norway Date Sampled August 23, 1970
 Well 2/4-4AX, DST No. 4 County _____
 Field Ekofisk State North Sea, Norway

FORMATION CHARACTERISTICS

Formation Name	<u>Danian</u>
Date First Well Completed	<u>August 23</u> , 19 <u>70</u>
Original Reservoir Pressure (2/4-2X Well)	<u>7085</u> PSIG @ <u>10530</u> Ft.
Original Produced Gas-Liquid Ratio	_____ SCF/Bbl
Production Rate	_____ Bbls/Day
Separator Pressure and Temperature	_____ PSIG _____ ° F.
Liquid Gravity at 60° F.	<u>37.5</u> _____ ° API
Datum	_____ Ft. Subsea

WELL CHARACTERISTICS

Elevation	<u>89 RKB</u> _____ Ft.
Total Depth	<u>10110</u> _____ Ft.
Producing Interval	<u>9980-10090</u> _____ Ft.
Tubing Size and Depth	<u>3-1/2</u> In. to <u>9922</u> Ft.
Open Flow Potential	_____ MMSCF/Day
Last Reservoir Pressure	_____ PSIG @ _____ Ft.
Date	_____, 19____
Reservoir Temperature	<u>258</u> _____ ° F. @ <u>10035</u> Ft.
Status of Well	<u>Flowing DST 4</u>
Pressure Gauge	_____

SAMPLING CONDITIONS

Flowing Tubing Pressure	<u>560</u> _____ PSIG
Flowing Bottom Hole Pressure	_____ PSIG
Primary Separator Pressure	<u>460</u> _____ PSIG
Primary Separator Temperature	<u>83</u> _____ ° F.
Secondary Separator Pressure	_____ PSIG
Secondary Separator Temperature	_____ ° F.
Field Stock Tank Liquid Gravity	<u>37.5</u> _____ ° API @ 60° F.
Primary Separator Gas Production Rate	<u>643.6</u> _____ MSCF/Day
Pressure Base	<u>14.696</u> PSIA
Temperature Base	<u>60</u> _____ ° F.
Compressibility Factor (F _{pv})	<u>1.0494</u>
Gas Gravity (Laboratory)	<u>0.700</u>
Gas Gravity Factor (F _g)	<u>1.1952</u>
Separator Liquid Production Rate @ 83° F. & 460 psig	<u>378</u> _____ Bbls/Day
Primary Separator Gas/ Separator Liquid Ratio	<u>1703</u> _____ SCF/Bbl
or	_____ Bbls/MMSCF

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Well 2/4-4AX, DST No. 4

Hydrocarbon Analyses of Separator Products and Calculated Well Stream

<u>Component</u>	<u>Separator Liquid Mol Per Cent</u>	<u>Separator Gas Mol Per Cent</u>	<u>GPM</u>	<u>Well Stream * Mol Per Cent</u>
Hydrogen Sulfide	0.22	1.42		1.09
Carbon Dioxide	0.07	0.47		0.36
Nitrogen	9.58	82.12		61.90
Methane	4.84	9.32	2.348	8.07
Ethane	5.38	4.01	1.101	4.39
Propane	1.35	0.51	0.166	0.74
iso-Butane	4.09	1.17	0.368	1.98
n-Butane	1.65	0.27	0.099	0.65
iso-Pentane	2.00	0.32	0.116	0.79
n-Pentane	7.41	0.19	0.077	2.20
Hexanes	<u>63.41</u>	<u>0.20</u>	<u>0.091</u>	<u>17.83</u>
Heptanes plus	100.00	100.00	4.366	100.00

Properties of Heptanes plus

API gravity @ 60° F.	<u>35.5</u>		
Specific gravity @ 60/60° F.	<u>0.8475</u>		<u>0.847</u>
Molecular weight	<u>225</u>	<u>103</u>	<u>224</u>

Calculated separator gas gravity (air = 1.000) = 0.700

Calculated gross heating value for separator gas = 1194 BTU

per cubic foot of dry gas @ 14.696 psia and 60° F.

Primary separator gas collected @ 460 psig and 83 °F.

Primary separator liquid collected @ 460 psig and 83 °F.

Primary separator gas/separator liquid ratio 1703 SCF/Bbl @ 83° F.

* Bubble point pressure = 6228 psig at 258° F.

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Well 2/4-4AX, DST No. 4

VOLUMETRIC DATA OF Reservoir Fluid SAMPLE

1. Saturation pressure (bubble-point pressure) 6228 PSIG @ 258 °F.

2. Thermal expansion of saturated oil @ 7500 PSI = $\frac{V @ 258 \text{ } ^\circ\text{F}}{V @ 70 \text{ } ^\circ\text{F}}$ = 1.15380

3. Compressibility of saturated oil @ reservoir temperature: Vol/Vol/PSI:

From 7500 PSI to 7000 PSI = 23.14 x 10⁻⁶

From 7000 PSI to 6600 PSI = 26.16 x 10⁻⁶

From 6600 PSI to 6228 PSI = 31.58 x 10⁻⁶

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Well 2/4-4AX, DST No. 4

Pressure-Volume Relations of Reservoir Fluid at 258° F.

<u>Pressure,</u> <u>PSIG</u>	<u>Relative</u> <u>Volume</u>
7500	0.9666
7000	0.9779
6800	0.9827
6700	0.9854
6600	0.9883
6500	0.9912
6400	0.9942
6300	0.9974
<u>6228</u>	1.0000
6183	1.0020
6139	1.0040
6028	1.0090
5769	1.0227
5443	1.0428
5030	1.0732
4582	1.1143
4083	1.1763
3588	1.2597
3112	1.3752
2712	1.5122
2397	1.6601
1833	2.0641
1370	2.7006
970	3.7469

Core Laboratories, Inc.
Reservoir Fluid Analysis

P. L. Moses HS

P. L. Moses
Manager

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