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15/9-11 Testevaluering

L.nr. 06084360013		Støtteil			
Avd.	Sentralarkiv				
S.bh.	Avd arkiv				
Mott.	Spes. arkiv				
5 SEPTEMBER 1984					
Kode 15/9-11					
O.pr. Testevaluering					
M. film					
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Emneord:					

WELL TEST REPORT

PL 046

WELL NO: 15/9-11

JUNE 1982

BY: LET-SVG

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WELL TEST REPORT 15/9-11

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ENCLOSURES:

- Petrophysical log summary and evaluation plot, well 15/9-11, Paleocene and Mesozoic.

WELL DATA

Operator: Den norske stats oljeselskap a.s  
Well name: 15/9-11  
Classification: Appraisal well  
Drilling rig: Ross Rig  
Spudded: 17 September, 1981  
Completed: 23 December, 1981  
KB elevation: 25 meters  
Water depth: 87.5 meters  
Total depth: 2950 m RKB  
Objectives: Sandstone of lower Paleocene age  
(Heimdal formation) and of Jurassic/  
Triassic age (lower Mesozoic)  
Results: Discoveries in Paleocene sandstone and  
in Mesozoic sand.

## WELL SUMMARY

Well 15/9-11 was spudded by Ross Rig on 17th September 1981 and reached TD of 2950 m RKB within Triassic sediments. After a period of logging and testing the well was abandoned on 23rd December 1981. The 15/9-11 well was the second well to be drilled on the Gamma structure.

One of the objectives with 15/9-11 was to delineate the hydrocarbon accumulation found in the Heimdal formation of Paleocene age in 15/9-9. The Heimdal formation was encountered at a depth of 2387 m RKB. The sand is hydrocarbon bearing between 2387 and 2442 m RKB and below approximately 2425 m RKB water is also mobile. This is verified by two DST's, and by RFT and log interpretations.

The Mesozoic sand was encountered at a depth of 2795 m RKB. The sand is hydrocarbon bearing down to the GWC at 2825 m RKB. One DST was performed in this interval.

#### 1. REPEAT FORMATION TESTER (RFT)

Two RFT runs were conducted in the Heimdal Fm., and two RFT runs were completed in Lower Mesozoic (Jurassic/Triassic).

Run no. 1., Heimdal Fm.:

2349.5 - 2522.0 m RKB

31 pretests records out of 35 were obtained. One segregated sample was taken at 2387.5 m RKB.

Run no. 2., Heimdal Fm.:

The purpose of run 2 was sampling, but was not successful due to slow response. Two sampling attempts at 2434.0 m RKB and 2431.5 m RKB were done.

Run no. 1., Jurassic/Triassic:

2790.5 - 2830.5 m RKB

22 pretests records out of 23 were obtained. One segregated sample was taken at 2812.0 m RKB.

Run no. 2., Jurassic/Triassic:

2925.0 - 2938.0 m RKB

6 pretests records out of 8 were obtained. One segregated sample was taken at 2825.8 - 2826.5 m RKB

A discussion of these RFT runs and the results of the analysis performed on some of the samples are given in an own report:

RFT-report 15/9-11, Heimdal and Jurassic/Triassic formation, March 1982.

A summary of the RFT results is presented in appendix 1.

#### DRILL STEM TESTS (DST)

One DST-test was carried out in Lower Mesozoic (Jurassic and/or Triassic sand) and two in the Heimdal sand.

Results of the tests are presented in appendix 2, 3 and 4. A discussion of each test follows below.

2. DST NO. 1

2.1. Objectives

- Fluid samples
- Reservoir pressure/temperature
- Permeability
- Gas inurities
- Sand stability

Interval perforated: 2797 - 2807 m RKB.

2.2. Test string

The test string used was 5 in VAM tubing with Halliburton APR-N tester valve, drill pipe tester valve and an APR-M valve situated above the 244.5 mm (9 5/8 inch) RTTS packer. The packer was set at 2764.5 m RKB. The test string was run with fresh water except for the upper 500 m which was air. Two Flopetrol SSDR and two Sperry Run MRPG pressure/temperature gauges were run with the string.

2.3. Test operation

DST no. 1. was successfully completed. The test consisted of an initial flow and an intial shut-in followed by a main flow period. The test was terminated by a final shut-in period.

2.4. Fluid production and sampling

During the main flow on 16.7 mm (42/64") choke an average rate of 571 000 Sm<sup>3</sup>/D (20.2 MMSCF/D) of gas and 238 Sm<sup>3</sup>/D (1500 STB/D) of condensate was obtained. Total water production was 1.6 m<sup>3</sup> (10 bbl). The water was fresh and interpreted to be associated with the gas.

Gas and condensate rates were stable at the end of the flow period. The gas rates between 18:30 hrs. and 20:00 hrs are probably erroneous due to blockage in the Daniel orifice box.

Fluid samples were taken at the separator during the flow period. The specific gravity of the condensate was 0.75 ( $57^{\circ}$  API) and the gas specific gravity was 0.73 at separator conditions 31.72 bara (460 psia) and  $35.6^{\circ}\text{C}$  ( $96^{\circ}\text{F}$ ).

No  $\text{H}_2\text{S}$  was observed, but 2%  $\text{CO}_2$  was measured.

No sand production was detected.

Three sets of PVT-samples were taken from the separator.

Shrinkage was measured by using the shrinkage tester and by using the stock tank. The result from the latter has been used for the condensate production rate calculations. The stock tank shrinkage was 15%. The shrinkage from the shrinkage tester was 11% and this value is used to correct the gas rate for the gas solubility of the condensate leaving the separator (260 SCF/STB).

#### 2.5. Interpretation of DST no. 1.

Interpretation of the test is carried out by using the Flopetrol SSDR gauge no. 81049. The resolution of the Sperry Sun MRPG gauges is not good enough for the pressure build-up analysis.

The stabilized bottom hole temperature recorded during the final build up is  $102.8^{\circ}\text{C}$  ( $217^{\circ}\text{F}$ ) which is believed to represent the reservoir temperature.

##### - Initial build-up

Fig. 2.2. and 2.5. indicate that the APR-N valve did not close completely when the annulus pressure was bled off. First after 5 minutes the pressure starts to build up to static pressure. The start and the end of semilog straight line used in the Horner plot occurs after 8 and 14 minutes respectively (Fig. 2.3. and 2.4.). The extrapolated pressure  $P^*$  is 299.80 bara (4348.3 psia). After the semilog straight line the build-up curve flattens.

- Final build-up.

The pressure build-up is analysed by the Horner method (Fig. 2.8. - 2.9.). The anomalous pressure build-up in fig. 2.9. is probably caused by phase redistribution. Phase redistribution produce a pressure overshoot or hump of small magnitude. The semilog straight line starts 169 minutes after shut in and ends after 780 minutes where the curve flattens. An extrapolated pressure  $P^*$  of 299.48 bara (4343.6 psia) and a slope of 0.1108 bar/cycle (1.607 psi/cycle) are obtained from the plot. A permeability thickness of 16235 md m (53266 md ft) is calculated. Assuming that the whole gas bearing sand section (30 m, 98.4 ft) is contributing flow to the wellbore gives a permeability of 541 md. The estimated total skin factor is 147 and the skin due to partial penetration is 5. One of the reasons for this high total skin may be due to condensate accumulation around the wellbore. The dew point pressure which is 292 bar (4235 psi), is 7.5 bar (109 psi) below initial reservoir pressure, and the drawdown during the test was approximately 17.2 bar (250 psi). Another reason may be that the number of effective perforations were small. Such a completion has excess pressure drop from both turbulence and a large partial penetration skin effect.

#### 2.4. Conclusion

DST no. 1. was successful according to the objectives and also mechanically. Three sets of PVT samples were obtained and they are analysed at our laboratories.

Initial reservoir pressure is 299.48 bara (4343.6 psia, 1.093 g/cc e.m.w.) and the reservoir temperatures is  $102.8^\circ\text{C}$  ( $217^\circ\text{F}$ ) at 2783.73 m RKB. The permeability is estimated to be 541 md. No  $\text{H}_2\text{S}$  was observed, but 2%  $\text{CO}_2$  was measured. No sand production was detected.

3. DST NO. 2.

3.1.Objectives

- Check the potential gas/water contact
- Fluid sampling
- Pressure/temperature
- Permeability
- Check for sandproduction

Interval perforated: 2432 - 2440 m RKB.

3.2.Test string

A standard Halliburton test string was run with an APR-N tester valve, Drill Pipe tester valve and APR-M valve situated above the 245 mm (9 5/8") RTTS packer. The packer was set at 2395 m. A water cushion of 1500 m was run above the DP Tester valve.

3.3.Test operation

The test was planned to consist of one long flow period, followed by a build-up period. Because of a leak in the heater outlet, the well had to be shut in before stable separator conditions were obtained.

7 minutes after the APR-N valve was open, the well was opened on the choke manifold on 25.4 mm (64/64") choke.

After flowing for 10 minutes on 25.4 mm (64/64") choke, the choke was reduced to 19.1 mm (48/64") and 20 minutes later it was reduced to 11.1 mm (28/64") because of water and sand production. No water was produced on 11.1 mm (28/64") choke. The flow was led through the heater and the separator on a 12.7 mm (32/64") choke.

No glycol was injected to the wellstream.

### 3.4. Fluid production and sampling

When flowing on 12.7 mm (32/64") choke an average rate of 229  $\text{MSm}^3/\text{D}$  (8.1 MMSCF/D) of gas, 100  $\text{Sm}^3/\text{D}$  (630 STB/D) of condensate and 114  $\text{Sm}^3/\text{D}$  (720 BBLS/D) of water was obtained. On 12.7 mm (28/64") choke no water was produced.

During the flow, fluid samples were taken on "Goose Neck" for BSW measurements. 60% - 75% of water and 0.3% - 0.5% of sand was observed.

A condensate specific gravity of 0.75 ( $57.4^\circ \text{ API}$ ) and gas gravity of 0.72 was measured on separator at 9.6 barg (140 psig).

No  $\text{H}_2\text{S}$  or  $\text{N}_2$  and just traces of  $\text{CO}_2$  was detected.

Separator samples of water and condensate were taken during flow and after shut-in.

Only one set of PVT sample was taken, because of a leak in the heater outlet.

### 3.5. Interpretation of DST no. 2

The interpretation of DST no. 2. is based upon pressure data from the Sperry Sun MK III 2 gauge (Fig. 3.1. - 3.3.). Stabilized bottom hole temperature recorded after shut in is  $87.2^\circ \text{C}$  ( $189^\circ \text{F}$ ), and this temperature is believed to represent the reservoir temperature. Six gauges were run and the initial reservoir pressure from four of these fall on a straight line, which correlate very well to pressures and the gradient from RFT.

Wellhead data during the build-up indicate a slight leak in the APR-N valve, which does not seem to affect the quality of the downhole pressure data.

Factors which are difficult to control, affect the interpretation and the results.

The well was shut in before stabilized separator conditions were obtained. At this time the condensate rate is still increasing while the water rate is decreasing.

In addition, the two phase flow (here, water and gas) is difficult to interpret, and in this case a water saturation gradient occurs, which complicates the problem. The water saturation increases from top to bottom of the test interval. This implies that the phase mobility and total mobility change through the whole section.

When flowing on 11.1 mm (28/64") choke no water was produced at surface, but it is obvious that water has been flowing to the wellbore where it has been accumulated. After the choke was increased to 12.7 mm (32/64") the well started to produce water. While the accumulated water in and around the wellbore was drained, the water rate and the saturation decreased, while the gas saturation and the gas mobility increased. It is reasonable to assume that the well was shut in when the accumulated water still was drained.

- Build up

The Horner method is used for the pressure build up analysis.

A  $P^*$  of 244.2 bar (3541.8 psia) and a slope of 0.1329 bar/cycle (1.928 psi/cycle) was estimated from the Horner plot. The semi-log straight line starts 72 minutes after shut in, and continues through out the build-up (Fig. 3.4. - 3.5.).

An effective gas permeability of 424.5 md and an effective water permeability of 555 md is calculated, assuming the hole sand section (12 m, 39.4 ft) is contributing to the flow.

Estimated total skin factor is 55.3, and the skin due to partial penetration is estimated to 1.43.

Accumulation of water and presence of two phase flow is probably the main contribution to the skin factor.

### 3.6. Conclusion

The results are restricted because of aborted flow, but seems to be in agreement with results from 15/9-9 test in Heimdal sand. Logs indicate the zone to be mostly water bearing ( $S_w = 80\%$ ), with some gas, which was confirmed by the test. An average water rate of  $114 \text{ Sm}^3/\text{D}$  (720 BPD) was obtained.

Some sand was produced, at high rates about 8% and on 12.7 mm (32/64") choke 0.3 - 0.5%. No  $\text{H}_2\text{S}$  and only traces of  $\text{CO}_2$  was proved. The reservoir pressure is normal, 1.022 g/cc emv.

Permeability is good, effective gas permeability is 424.5 md and effective water permeability is 555 md.

Only one set of PVT sample was taken, while the objective was two sets.

Except of the aborted flow due to mechanical problems, the test was successful according to the objectives.

4. DST NO. 3.

4.1.Objectives

- Permeability
- Fluid samples
- Reservoir pressure/temperature
- Sand stability
- Determination of trace elements

Interval perforated: 2395 - 2415 m RKB.

4.2.Test string

The test string was the same as for DST no. 1 and 2. The RTTS packer was set at 2361 m and 2000 m of water cushion was originally filled on top of the drill pipe tester valve. Flopetrol and Sperry Sun pressure gauges were run with the string.

4.3.Test operation

No major problems occurred during the test. The RTTS circulating valve was accidentally opened while setting the packer. Mud u-tubed into the tubing and compressed the air cushion from originally 350 m to approximately 5 m. This would not have allowed the well to flow. Therefore 61 bbls of water and 60 bbls of diesel was pumped into the tubing, and the mud displaced back in the annulus.

When shutting the well in for first build-up and second build-up, there was no indications that the APR-N valve was closed. Therefore both must be considered as surface shut-in.

4.4.Fluid production and sampling

The main problem concerning production was the correction factors for the metered condensate flow rate. Tank readings indicated significant correction and shrinkage tester indicated high shrinkage. The condensate rates used for

this test is only corrected for shrinkage from skrinkage tester assuming meter factor to be 1.0. This is to avoid a doble correction for shrinkage.

Otherwise, separator and wellhead conditions were satisfactory stable during most of the test.

Traces of water was produced (1 - 2 %). This was analysed on the rig by the mud engineer and by Schlumberger and was found to be fresh (4 - 6000 ppm Cl<sup>-</sup>). It is probably vapor associated with the gas.

PVT sampling at the separator was not successful. Two out of three samples were invalide due to gas in the liquid container. Third set was good.

KSLA (Shell) did trace analysis for us, and found 0.2 - 0.3 % CO<sub>2</sub> in the gas. No H<sub>2</sub>S or mercury was found. Separate report will follow from KSLA.

#### 4.5. Interpretation of DST no. 3

This test was performed in the best part of the reservoir (ref. attached CPI). The sand is fairly clean with an average porosity of 20 % and water saturation of 23 %. This zone is equivalent to DST no. 3. in 15/9-9.

The test analysis is based on analysis of the two build-ups, the last one after a multiple rate flow.

The Flopetrol SSDR-no 81049 gauge at 2365.7 m RKB is used for the pressure build-up analysis.

The stabilized bottom hole temperature recorded during the first build up is 85.6°C (186°F) which is believed to represent the reservoir temperature.

##### - First build-up

The build up followed a 1005 minutes flow period of which 971 minutes were on 19.1 mm (48/64") choke. The flow was fairly stable at the end of this period.

The pressure build-up was analysed using the Horner method. Fig. 4.3. and 4.4. shows Horner plots with a  $P^*$  of 242.83 bara (3522 psia) and a slope of 0.1055 bar/cycle (1.53 psi/cycle). The build-up is dominated by afterflow the first 4 minutes (Fig. 4.5.). End of semi-log straight line occurs after approximately 210 minutes.

A permeability thickness of 15672 md-m (51714 md-ft) is calculated. Assuming the whole sand section 38 m (124.7 ft) is contributing, this gives a permeability of 415 md.

A total positive skin of 57 and a partial penetration skin factor of 3.6 are calculated. The dew point pressure is measured to be 234 bar (3394 psi) in 15/9-9, DST 3. The flowing bottom hole pressure is 2.76 bar (40 psi) above this dew point. This may indicate that condensate accumulation is not present. The flowing bottom hole pressure during DST 2 in well 15/9-9 was approximately 15 bar (220 psi) below this dew point and the calculated total skin was 335. All the other estimated skin factors in the Heimdal formation are between 50 and 60.

- Multiple rate build-up

The interpretation was carried out by using the multiple rate build-up technique (Fig. 4.7. - 4.8.). An extrapolated pressure  $P^*$  of 242.88 bar (3522.7 psia) and a slope of 0.1610 bar/cycle (2.335 psi/cycle) are obtained from the plot.

The build up is affected by afterflow the first 2 minutes and the interval used for the semi-log straight line is 15 - 134 minutes.

The analysis gave a positive skin of 55 and a permeability thickness of 16327 mdm (53566 mdft). Assuming that the entire sand section (38 m) is contributing flow to the wellbore gives a permeability of 430 md.

Both the permeability and the skin values match very well to the same parameters obtained from the first build-up.

It is not possible to performe deliverability calculations. The flowing bottom hole pressure increases during all three flow periods.

#### 4.6. Conclusions

No major problems occured during the test, but the APR-N tester valve did not close when the annulus pressure was bled off for first and second build up. Therefore both must be considered as surface shut in.

Two of three sets of PVT samples were invalid due to gas in the liquid bottle.

Initial reservoir pressure is 242.83 bara (3522 psia, 1.047 g/cc emw.) and the reservoir temperature is 85.6°C (186°F) at 2365.7 m RKB. The permeability is estimated to be in the range of 400 md. No H<sub>2</sub>S was observed, but 0.3 % CO<sub>2</sub> was measured. No sand production was detected.

APPENDIX 1

## REPEAT FORMATION TESTER (RFT)

### Content:

- Pretest recorded data
- Fig. 1.1.: 15/9-11 Formation pressure, Heimdal Fm.
- Fig. 1.2.: Formation pressure comparison 15/9-9 and 15/9-11, Heimdal Fm.
- Fig. 1.3.: 15/9-11 Formation pressure Jurassic/Triassic Fm.

WELL: 15/9-11  
 DATE: 21/10-81  
 RUN NO.: 1

PRESSTEST CORES DATA

HEIMDAL FORMATION

Max. rec. temp.: 66.7°C (152°F)

Test No.	Depth	Log hydr. pr. before/after test	Log pretest pressure	Cor. pretest pressure	Cor. hydr.pr. after test	Remarks
	mRKB	psig	psig	gm/cc	psi/g, gm/cc	
1	2349.5	4157 / 4163	3531	3505 / 1.049	4138 / 1.24	
2	2361.0	4177 / 4180	3535	3509 / 1.045	4155 / 1.24	Lista Formation
3	2388.5	4230 / 4232	3546	3520 / 1.036	4207 / 1.24	Lista Formation
4	2395.0	4243 / 4242	3548	3522 / 1.034	4217 / 1.24	
5	2401.0	4254 / 4258	3554	3528 / 1.033	4233 / 1.24	
6	2405.0	4268 / 4275	3564	3538 / 1.035	4250 / 1.24	Supercharge
7	2405.0	4269 / 4276	3564	3538 / 1.035	4251 / 1.24	Supercharge
8	2410.0	4291 / 4298	-	-	4273 / 1.25	Supercharge
9	2416.0	4294 / 4296	3573	3547 / 1.032	4271 / 1.24	
10	2423.0	4299 / 4303	3572	3546 / 1.029	4278 / 1.24	
11	2431.0	4309 / 4318	3577	3551 / 1.027	4293 / 1.24	
12	2436.5	4316 / 4322	3578	3552 / 1.025	4297 / 1.24	
13	2439.0	4316 / 4319	3577	3551 / 1.024	4294 / 1.24	
14	2444.0	4321 / 4331	3589	3563 / 1.025	4306 / 1.24	
15	2446.0	4324 / 4332	3590	3564 / 1.025	4307 / 1.24	
16a	2469.5	4369 / 4373	-	-	4348 / 1.24	
16b	2469.5	4369 / 4373	3621	3595 / 1.024	4348 / 1.24	
17	2475.5	4373 / 4376	3623	3597 / 1.022	4351 / 1.24	
18	2483.0	4386 / 4392	3637	3611 / 1.023	4367 / 1.24	
19a	2488.5	4397 / -	-	-	-	Power shut down
19b	2488.5	4396 / 4404	3697	3671 / 1.037	4379 / 1.24	Supercharge
19c	2488.5	4404 / 4405	3650	3624 / 1.024	4380 / 1.24	

HELL: 15/9-11  
DATE: 21/10-81  
UN NO.: 1

## HEIMDAL FORMATION

Max. rec. temp.: 66.7°C (152°F)

Test	Depth	Log hydr. pr. before/after test	Log pretest pressure	Cor. pretest pressure	Cor. hydr.pr. after test	Remarks
tc	mRKB	psig	psig	psig, gm/cc	psig, gm/cc	
20a	2495.3	4409 / 4414	3729	3703 / 1.044	4389 / 1.24	Supercharge
20b	2495.3	4414 / 4413	3660	3634 / 1.024	4388 / 1.24	
21a	2500.0	4412 / -	-	-	-	Lost seal
21b	2500.0	4419 / 4422	3666	3640 / 1.024	4397 / 1.24	
22	2517.0	4443 / 4446	3683	3657 / 1.022	4421 / 1.24	
23	2522.0	4452 / 4457	3693	3667 / 1.023	4432 / 1.24	Supercharge Blocked eq. valve
24	2414.0	4341 / -	-	-	-	
25	2410.0	4248 / 4253	3559	3533 / 1.031	4228 / 1.23	
26a	2388.5	4205 / 4224	3556	3530 / 1.039	4199 / 1.24	
26b	2388.5	- / 4225	3560	3534 / 1.040	4200 / 1.24	
27	2351.0	4136 / 4152	3603	3577 / 1.070	4127 / 1.23	Supercharge
28	2436.5	4301 / 4299	3563	3537 / 1.021	4274 / 1.23	
29	2435.0	4294 / -	3563	3537 / 1.021	-	Att. sampling
30	2436.0	4296 / 4301	3569	3543 / 1.023	4276 / 1.23	Att. sampling
31	2434.0	4295 / -	3567	3541 / 1.023	-	Att. sampling
32	2437.0	4296 / -	3568	3542 / 1.022	-	Att. Sampling
33	2432.0	4287 / 4286	3566	3540 / 1.024	4261 / 1.23	Att. Sampling
34	2388.5	4201 / 4206	3548	3522 / 1.037	4181 / 1.23	Att. Sampling
35	2387.5	4203 / 4205	3547	3521 / 1.037	4180 / 1.23	Sampling

WELL: 15/9-11  
DATE: 21/10-81  
RUN NO.: 2

## HEIMDAL FORMATION

Max. rec. temp.:

Test	Depth	Log hydr. pr. before/after test	Log pretest pressure	Cor. pretest pressure	Cor. hydr.pr. after test	Remarks
No.	mRKB	psig	psig	psig, gm/cc	psig, gm/cc	
1	2434.0	4305 / -	3564	3538 / 1.022	-	Att. sampling
2	2431.5	4294 / -	3559	3533 / 1.022	-	Att. sampling

WELL: 15/9-11  
DATE: 1/11-81  
RUN NO.: 1

PART TEST COR. DATA  
JURASSIC/TRIASSIC FM.

Max. rec. temp.: 190°F (87.8°C)

Test	Depth	Log hydr. pr. before/after test	Log pretest pressure	Cor. pretest pressure	Cor. hydr.pr. after test	Remarks
IC	mRKB	psig	psig	psig, gm/cc	psig, gm/cc	
1	2790.5	5124 / 5126	-	-	5097 / 1.284	Tight, Heather Fm.
2	2796.0	5045 / 5048	4367	4336 / 1.090	5019 / 1.262	Heather Formation
3	2791.0	5036 / 5040	4373	4342 / 1.094	5011 / 1.262	
4	2798.0	5051 / 5050	4368	4337 / 1.090	5021 / 1.262	
5	2801.0	5057 / 5055	4370	4339 / 1.089	5026 / 1.262	
6	2804.0	5059 / 5058	4370	4339 / 1.088	5029 / 1.261	
7	2806.0	5061 / 5062	4372	4341 / 1.088	5033 / 1.262	
8	2809.0	5065 / 5067	4373	4342 / 1.087	5038 / 1.262	
9	2812.0	5069 / 5071	4374	4343 / 1.086	5042 / 1.261	
10	2816.0	5081 / 5081	4377	4346 / 1.085	5052 / 1.262	
11	2820.0	5086 / 5088	4380	4349 / 1.085	5059 / 1.262	
12	2823.0	5090 / 5094	4383	4352 / 1.084	5065 / 1.262	
13	2825.0	5092 / 5093	4384	4353 / 1.084	5064 / 1.261	
14	2826.0	5094 / 5096	4386	4355 / 1.084	5067 / 1.261	
15	2827.0	5098 / 5098	4388	4357 / 1.084	5069 / 1.261	
16	2829.0	5100 / 5101	4397	4366 / 1.085	5072 / 1.261	
17	2830.0	5102 / 5106	4397	4366 / 1.085	5077 / 1.262	
18	2830.5	5104 / 5105	4398	4367 / 1.085	5076 / 1.262	
19	2828.0	5099 / 5099	4392	4361 / 1.085	5070 / 1.262	
20	2822.0	5088 / 5092	4382	4351 / 1.084	5063 / 1.262	
21	2813.5	5074 / 5079	4379	4348 / 1.087	5050 / 1.262	
22	2790.8	5036 / 5038	4380	4349 / 1.096	5009 / 1.262	Heather Formation
23	2812.0	5075 / 5060	4372	4341 / 1.086	5031 / 1.258	Sample

PLATEAU CORAL DATA

WELL: 15/9-11  
DATE: 1/11-81  
LIN NO.: 2

JURASSIC/TRIASSIC FM.

Max. rec. temp.: 190°F (87.8°C)

Test	Depth	Log hydr. pr. before/after test	Log pretest pressure	Cor. pretest pressure	Cor. hydr.pr. after test	Remarks
no	mRKB	psig	psig	psig, gm/cc	psig, gm/cc	
1	2925.0	5269 / 5269	-	-	5240 / 1.260	Tight
2	2926.5	5270 / 5271	-	-	5242 / 1.260	Tight
3	2927.5	5272 / 5275	4585	4554 / 1.094	5246 / 1.260	
4	2929.0	5275 / 5275	4586	4555 / 1.093	5246 / 1.260	
5	2934.0	5284 / 5279	4589	4558 / 1.092	5250 / 1.258	
6	2938.0	5289 / 5289	4597	4566 / 1.093	5260 / 1.259	
7	2936.0	5286 / 5287	4596	4565 / 1.093	5358 / 1.260	
8	2932.5	5275 / 5279	4590	4559 / 1.093	5250 / 1.259	
9	2826.5	5099 / 5153	4389	4358 / 1.084	5124 / 1.275	Sampling, plugging
10	2826.0	5092 / 5084	4384	4353 / 1.083	5055 / 1.258	Sampling, plugging
11	2825.8	5089 / 5088	4380	4349 / 1.082	5059 / 1.259	Sampling

Fig. 1.1.

15/9-11 FORMATION PRESSURE  
HEIMDAL FM

DEPTH  
m RKB

2350

RFT

2400

\* DST No. 2  
(PRESSURE AT GAUGE  
DEPTH)

2450

WATER GRADIENT: 0.0941 bar/m  
0.960 g/cc  
0.416 psw/ft

2500

242.5

245

247.5

250

252.5 bar

2550

3500

3520

3540

3560

3580

3600

3620

3640

3660 psig

PRESSURE

Fig. 1.2.

FORMATION PRESSURE COMPARISON  
15/9-9 AND 15/9-11, HEIMDAL FM

DEPTH  
m RKB

2350

2400

2450

2500

★ 15/9-9

● 15/9-11

GAS GRADIENT: 0.0276 bar/m

0.261 g/cc

0.122 psi/ft

WATER GRADIENT: 0.004 bar/m

0.000 g/cc

0.416 psi/ft

240

242.5

245

247.5

250

bar

3480

3500

3520

3540

3560

3580

3600

3620

3640 psig

PRESSURE

Fig. 1.3.

15/9-11 FORMATION PRESSURE  
JURASSIC / TRIASSIC FM

DEPTH  
m RKB

2800

GAS GRADIENT: 0.0401 bar/m  
0.409 g/cc  
0.177 psi/ft

GAS / WATER CONTACT: 2825 mRKB

2850

2900

2950

300

305

310

315

bar

4300

4400

4500

4600 psig

PRESSURE

APPENDIX 2

DST NO. 1

Content:

- Summary of DST no. 1.
- Lay out of test string
- Pressure recorders
- Diary of events
- Pressure, choke and flowdiagram
- Flow data
- Separator sampling
- Surface sampling
- Test analysis

Figures:

Bottom hole pressures during initial and final build up from SSDR 81049 gauge are listed and plotted:

- Flopetrol plot: P,T vs time
- $P_{ws}$  vs  $\Delta t$
- $P_{ws}$  vs  $\log((t + \Delta t)/\Delta t)$
- Log  $\Delta P$  vs  $\log \Delta t$

The figures are with two different pressure scales.

SUMMARY OF DST NO. 1.

Perforated interval: 2797 - 2807 m RKB.

- Initial flow: 2 minutes
- Initial build-up: 61 minutes
- Second flow
  - 12.7 mm (32/64") choke: 3 minutes
  - 15.9 mm (40/64") choke: 41 minutes
  - 16.7 mm (42/64") choke: 754 minuets
- Final build-up: 971 minutes

Average flow rate on 16.7 mm (42/64") choke:

- 517 000 Sm<sup>3</sup>/D  
(20.2 MMSCF/D) of gas
- 238 Sm<sup>3</sup>/D  
(1500 STB/D) of condensate

Gravities:

- Gas: 0.73 sp.gr.
- Condensate: 0.75 sp.gr (57°API)

Separator conditions:

- Pressure: 31.72 bara (460 psia)
- Temperature: 35.6°C (96°F)

Gauges:

Two Flopetrol SSDR and two Sperry Sun MRPG gauges were run with the string. SSDR 8148 did not work.

TEST STRING TALLY      ROSS RIG      15/9-11      DST no. 1.

All measurements to top of each item

	EQUIPMENT DESCRIPTION	MIN	MAX	LENGTH	DEPTH
		ID ("")	OD ("")	(m)	(m)
Otis STT w/X-over					
2	Jnts 5" VAM tbg. 18 lbs/ft	4.25	5.56	20.02	- 6.05
1	Pupjnt. 5" VAM tbg	4.25	5.56	4.53	13.93
1	X-over 5" VAM box x 4½" SA pin (0-22)	4.25	5.51	0.40	18.46
1	Otis lubricator valve	2.99	13.88	1.62	18.86
1	X-over 4½" SA box x 5" VAM pin (0-23)	4.25	5.51	0.41	20.48
1	Jnt. 5" VAM	4.25	5.56	10.32	20.89
1	Jnt. 5" VAM	4.25	5.56	9.43	31.21
2	Stds. 5" VAM	4.25	5.56	59.86	40.64
1	Pupjnt. 5" VAM	4.25	5.56	4.53	100.50
1	X-over 52 VAM box x 4½" SA pin (F-24)	3.00	6.00	0.29	105.03
1	Flopertrol EZ-tree	3.00	17.00	2.61	105.32
1	Flopertrol 5" OD Slick Jnt 4½"-4 SA pin x pin (F-17)	3.00	5.00	2.95	107.93
1	Flopertrol Fluted Hanger	3.00	16.00	0.29	110.88
1	X-over 4½"-4SA pin x 5" VAM pin (F-25)	3.00	6.00	0.31	111.17
1	Pupjnt. 5" VAM	4.25	5.56	1.22	111.48
1	Jnts. 5" VAM	4.25	5.56	9.67	112.70
78	Stds. 5" VAM	4.25	5.56	2296.41	122.37
1	X-over 5" VAM box x 3½" TDS pin	2.75	6.50	0.27	2418.78
3	Stds. 3½" TDS tbg 12.7 lbs/ft L-80	2.75	3.50	84.54	2419.05
1	X-over 3½" TDS box x 3½" IF pin	2.75	4.50	0.24	2503.59
1	Slip Jnt (open)	2.00	4.63	5.54	2503.83
1	Slip Jnt (closed)	2.00	4.63	4.01	2509.37
6	Stds Drill Collars	2.25	4.75	171.06	2513.38
1	X-over 3½" IF box x 2 7/8" EUE pin	2.50	4.75	0.20	2684.44
1	RTTS mech. circ valve	2.44	4.87	0.84	2684.64
1	X-over 2 7/8" EUE box x 3½" IF pin	2.62	4.75	0.20	2685.48
1	Std Drill Collar	2.25	4.75	28.60	2685.68
1	Slip Jnt (closed)	2.00	4.63	4.01	2714.28
1	Slip Jnt (closed)	2.00	4.63	4.01	2718.29
1	Std. Drill Collar	2.25	4.75	28.61	2722.30
1	APR-M Safety/circ. Valve	2.25	5.00	2.55	2750.91

	EQUIPMENT DESCRIPTION	MIN	MAX	LENGTH	DEPTH
		ID ("")	OD ("")	(m)	(m)
1	DP tester valve	2.25	5.00	1.46	2753.46
1	APR-N tester valve	2.25	5.00	3.89	2754.92
1	Ful Flo Hydr. Bypass	2.25	4.62	1.92	2758.81
1	Big John Jars	2.32	4.62	1.92	2760.73
1	RTTS Safety Joint	2.44	4.62	1.08	2762.65
1	RTTS Packer (above)	2.40	5.75	0.72	2763.73
1	RTTS Packer (below)	2.40	5.75	0.66	2764.45
1	Perf. Pupjnt. 2 7/8" EUE	2.44	2.88	3.54	2765.11
1	X-over 2 7/8" EUE box x 2 3/8" EUE pin	2.00	3.70	0.26	2768.65
1	Collar 2 3/8" EUE	-	2.88	0.13	2768.91
1	Otis XN-nipple 2 3/8" EUE box x 2 7/8" EUE pin	1.79	2.38	0.22	2769.04
1	X-over 2 3/8" EUE box x 2 7/8" EUE pin	2.00	3.70	0.26	2769.26
1	Jnt. 2 7/8" EUE tbg Flopetrol DST-hanger	2.44	2.88	9.41	2769.52
1	Jnt. 2 7/8" EUE tbg	2.44	2.88	8.93	2778.93
1	Perf. pupjnt. 2 7/8" EUE	2.44	2.88	2.05	2787.86
1	X-over 2 7/8" EUE box x 3 1/8" 8 N pin	2.25	4.25	0.31	2789.91
1	Halliburton APBT carrier	-	3.00	1.51	2790.22
1	X-over 3 1/8" 8 N box x 2 7/8" EUE pin	1.88	3.88	0.18	2791.73
1	Bullplug w/cross 2 7/8" EUE	-	4.00	0.21	2791.91
TOTAL DEPTH					2792.1

WELL NO.: 15/9-11 DST NO.: 1 DATE: 30.11.81.

- 30 -



WIRELINE NIPPLE XN at 2769.04 m

GAUGE TYPE AND NUMBER: SSDR 81048

DEPTH, PRESSURE ELEMENT: 2774.11 m RANGE: 10000 psi

MODE: 1 min DELAY: -

ACTUATED: time 1141 date: 30.11.81.

WILL RUN OUT: time 0041 date: 04.12.81.

GAUGE TYPE AND NUMBER: MRPG 0049

DEPTH, PRESSURE ELEMENT: 2777.63m RANGE: 6000 psi

MODE: 2 min DELAY: 512 min

ACTUATED: time: 1145 date: 30.11.81.

WILL RUN OUT: time: 0457 date: 03.11.81.

GAUGE TYPE AND NUMBER: \_\_\_\_\_

DEPTH, PRESSURE ELEMENT: \_\_\_\_\_ RANGE: \_\_\_\_\_

MODE: \_\_\_\_\_ DELAY: \_\_\_\_\_

ACTUATED: time: \_\_\_\_\_ date: \_\_\_\_\_

WILL RUN OUT: time: \_\_\_\_\_ date: \_\_\_\_\_

#### D.S.T. HANGER

GAUGE TYPE AND NUMBER: SSDR 81049

DEPTH, PRESSURE ELEMENT: 2783.73m RANGE: 10000 psi

MODE: 1 min DELAY: -

ACTUATED: time: 1144.5 date: 30.11.81.

WILL RUN OUT: time: 0044.5 date: 04.11.81.

GAUGE TYPE AND NUMBER: MRPG 0121

DEPTH, PRESSURE ELEMENT: 2787.24 m RANGE: 6000 psi

MODE: 2 min DELAY: 512 min

ACTUATED: time: 1147 date: 30.11.81.

WILL RUN OUT: time: 0459 date: 03.11.81.

GAUGE TYPE AND NUMBER: \_\_\_\_\_

DEPTH, PRESSURE ELEMENT: \_\_\_\_\_ RANGE: \_\_\_\_\_

MODE: \_\_\_\_\_ DELAY: \_\_\_\_\_

ACTUATED: time: \_\_\_\_\_ date: \_\_\_\_\_

WILL RUN OUT: time: \_\_\_\_\_ date: \_\_\_\_\_

DIARY OF EVENTS

---

WELL NO.: 15/9-11 DST NO.: 1  
ZONE TESTED: Lower Mesozoic PERFS.: 2797 - 2807 m

---

DATE/TIME OPERATIONS

---

30.11.81.

05:25 PERFORATING  
Schlumberger perforated test interval. Partial misrun lower 1/3 of zone only perforated.  
07:15 Run in hole to perforate remainder of zone  
07:55 Perforated remainder of zone, guns lost in hole.  
Rig up and run junk basket & gauge ring to 2795 m

RIH w/TEST STRING

11:30 Started to pick up test tools  
12:35 Gauges in hole, pick up test string

01.12.81.

09:04 Picked up to extend slip joints  
09:10 Set packer, land string in wear bushing  
09:17 Pressure annulus to 1400 psi, no response due to DPTV being shut  
09:21 Bleed annulus, pick up and cycle pipe to open DPTV  
09:34 String landed in wear bushing

INITIAL FLOW

09:38 Opened APR-N. Initial well head pressure 24 psi

INITIAL SHUT IN

09:40 Closed APR-N. Well head pressure 34 psia.  
Estimated production 8.5 bbl.  
Pressure rose to 975 psia then stabilized.

SECOND FLOW

10:41 Reopened APR-N  
10:42 Opened choke manifold to flare line.  
Adj. choke size 32/64"  
10:45 Adj. choke increased to 40/64"  
11:00 Gas to surface. WHP 1614 psia  
11:26 Switched to 42/64" fixed choke

DIARY OF EVENTS

---

WELL NO.: 15/9-11 DST NO.: 1  
ZONE TESTED: Lower Mesozoic PERFS.: 2797 - 2807 m

---

DATE/TIME	OPERATIONS
13:00	Switched flow through separator. WHP = 2379 psia
19:20	Commenced sampling PVT set no. 1.
21:10	Commenced sampling PVT set no. 2.
22:10	Commenced sampling PVT set no. 3.
22:32	Changed to starboard burner
23:05	Ran meter check to tank
23:55	Bypassed separator
24:00	Closed APR-N and choke manifold. WHP = 2474 psia

02.12.81

Pressure increased to 3171 psia then began decreasing

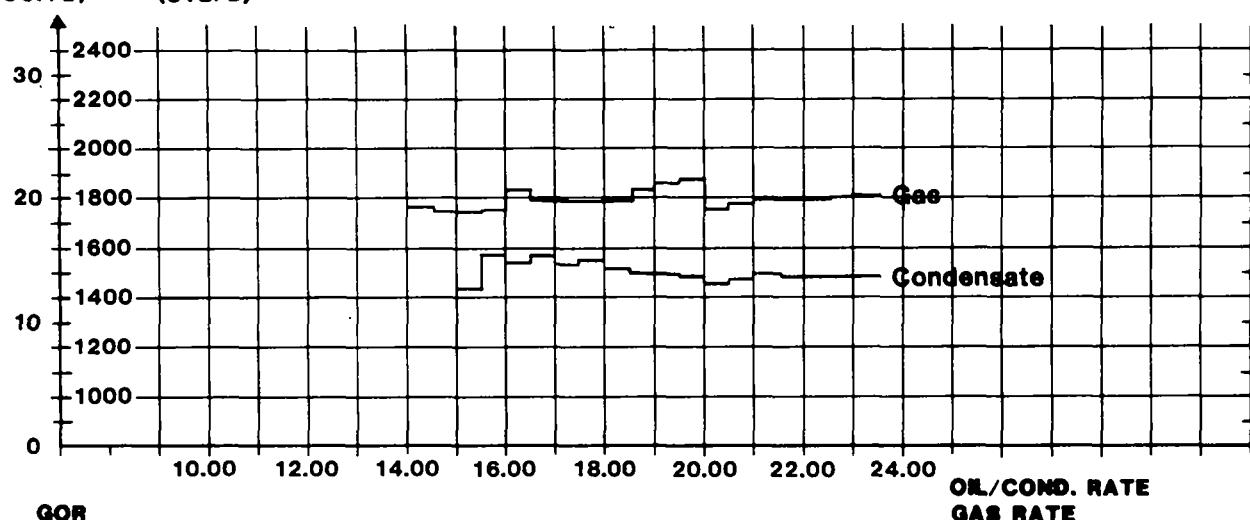
14:57	Began bleeding tubing through flare line. 24/64" choke
15:09	Increased to 42/64" choke
15:11	Shut in to observe
15:18	Continued bleeding tubing pressure 42/64" choke
15:40	Closed failsafe on surface test tree
15:50	Opened kill valve and pumped to fill tubing. 6 bbl water followed of mud
16:12	Opened APR-N. Commenced bullheading
16:57	Broke down formation with 3500 psig
17:12	Completed bullheading
17:27	Sheared APR-M and commenced reversing

Released packer and POOH

WELL NO : 15/9-11 DST NO.: 1

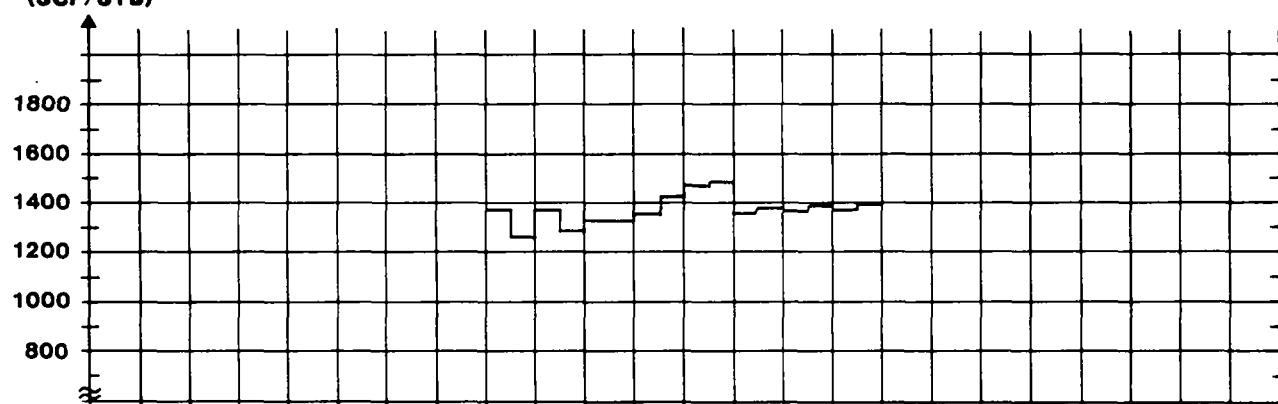
PRESSURE CHOKE AND FLOWDIAGRAM

GAS RATE OIL/COND. RATE  
(MMSCF/D) (STB/D)



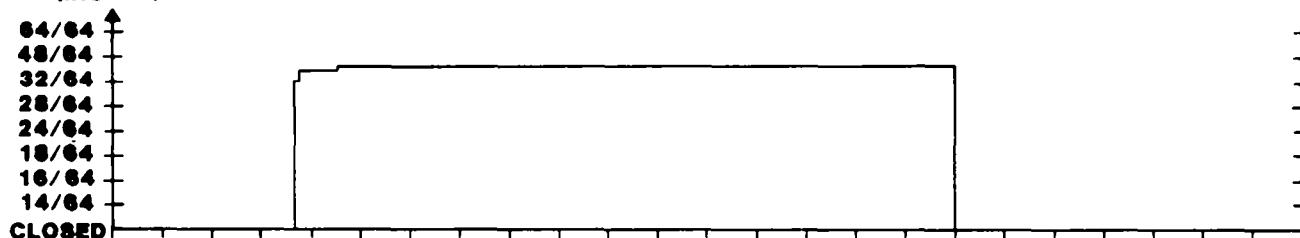
GOR  
(SCF/STB)

OIL/COND. RATE  
GAS RATE

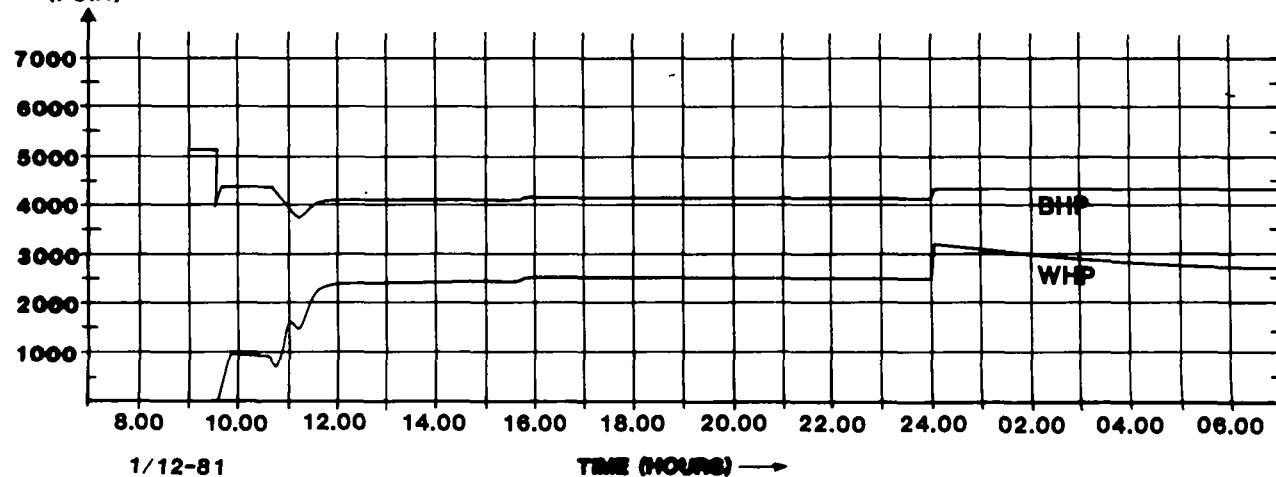


CHOKE SIZES  
(INCHES)

HEATER  
CHOKE MANIFOLD



PRESSURE  
(PSIA)



1/12-81

TIME (HOURS) —

**FLOW DATA**

Date/Time	Boring hole 1049			Well head			Chokes			Separator data						Liq. and gas analysis at goos neck, separator			
	Press. Psia	Temp. F	Press. Psia	Temp. F	Manifold 64. inc.	Heater 64. inc.	Press. Psi a	Temp. F	GEP scf/stb	Cond. API	Gas S.G.	Cond. API	Gas S.G.	Water %	pH	Sedim. %	Oil API	CO <sub>2</sub> %	H <sub>2</sub> S ppm
01.12.81			959																
1041																			
1042																			
1045	4229	215	778	50	32/64	40/64													
1100	3888	215	1614	68	"														
1126	3900	215	1734	84	42/64														
1300	4075	217	2379	98	"														
1430	4078	217	2395	102	"														
1500	4080	218	2405	104	"														
1530	4080	218	2401	106	"														
1600	4106	218	2479	107	"														
1630	4108	218	2490	110	"														
1700	4109	218	2497	110	"														
1730	4110	218	2495	110	"														
1800	4108	218	2490	110	"														
1830	4103	218	2471	111	"														
1900	4103	218	2474	112	"														
1930	4103	218	2471	114	"														
2000	4103	218	2472	115	"														
2030	4103	218	2472	117	"														
2100	4102	218	2472	118	"														
2130	4102	218	2472	118	"														
2200	4101	219	2472	118	"														
2230	4108	219	2473	118	"														
2300	4109	219	2474	120	"														
2330	4109	219	2474	120	"														
2355	4117	219	2474	"															
2400	4127	219	2475																

The gas rate is corrected for the gas solubility of the cond. leaving the separator (260 SCF/STB)

WELL no. 15/9-11      DST no. 1      DATE Dec. 1st 1981

1. Separator samples

Bottle no.	Oil/gas	Time	Cond. rate	Gas rate
			STB/D	MMSCF/D
9209-37	Cond.	1920/1945	1488	21.60
A-1556	Gas	1920/1945	1488	21.60
A-7220	Gas	1951/2011	1484	21.81
8088 86	Cond.	2110/2130	1494	20.32
A-7636	Gas	2110/2130	1494	20.32
A-4286	Gas	2140/2200	1490	20.45
8088 51	Cond.	2210/2225	1489	20.31
A-11342	Gas	2210/2225	1489	20.31
A-7148	Gas	2229/2245	1493	20.66

SURFACE SAMPLING

Condensate samples from separator during 2nd flow on  
16.7 mm (42/64") choke:

- 6 x 1 l bottles
- Three 20 l jerry cans
- 1 drum

## TEST ANALYSIS

Reservoir parameters:

Vapor volume equivalent:

$v_{CS} = 189 \text{ m}^3/\text{M}^3$  (1060 SCF/STB) at 57.0°API and 460 psia  
on separator

Main flow rate on 16.7 mm (42/64") choke:

$$Q_g = 20200000 \text{ SCF/D} + 1060 \text{ SCF/STB} \times 1500 \text{ STB/D} = 21.8 \text{ MMSCF/D}$$

(616 000  $\text{SM}^3/\text{D}$ )

$$t_{\text{eff}} = t_{\text{prod}} = 798 \text{ minutes}$$

Reservoir pressure, P:	299.48 bara (4343.6 psia)
Reservoir temperature, T:	102.8° C (217°F)
Specific gravity of reservoir gas, $\gamma_g$ :	0.939
Compressibility factor, Z:	0.961
Viscosity of reservoir gas, $\mu_g$ :	0.0319 cp
Gas formation volume factor, $B_g$ :	$4.25 \times 10^{-3} \text{ m}^3/\text{m}^3$ $(7.57 \times 10^{-4} \text{ RB/SCF})$
Compressibility of reservoir gas, $C_g$ :	$20.5 \times 10^{-4} \text{ bar}^{-1}$ $(1.41 \times 10^{-4} \text{ psi}^{-1})$
Compressibility of formation water, $C_w$ :	$39.0 \times 10^{-6} \text{ bar}^{-1}$ $(2.69 \times 10^{-6} \text{ psi}^{-1})$
Compressibility of the formation, $C_f$ :	$51.5 \times 10^{-6} \text{ bar}^{-1}$ $(3.55 \times 10^{-6} \text{ psi}^{-1})$
Water saturation, $S_w$ :	0.16
Hydrocarbon saturation, $S_g$ :	0.84
Porosity, $\phi$ :	0.215
Perforation height, $h_p$ :	10 m (32.8 ft)
Formation height, $h_t$ :	30 m (98.4 ft)
Wellbore radius, $r_w$ :	0.11 m (0.35 ft)
Total compressibility, $C_t$ :	$17.7 \times 10^{-4} \text{ bar}^{-1}$ $(1.22 \times 10^{-4} \text{ psi}^{-1})$

The compressibility factor and the specific gravity of the reservoir gas are PVT data from Statoil production lab.

The Flopetrol SSDR gauge no. 81049 at 2783.73 m is used for the analysis.

Results from Horner plot of final build-up:

$$\begin{aligned} p^* &= 299.48 \text{ bara (4343.6 psia)} \\ p_{1\text{hr}} &= 299.35 \text{ bara (4341.7 psia)} \\ m &= 0.1108 \text{ bar/cycle (1.607 psia)} \\ p_{wfs} &= 284.52 \text{ bara (4126.6 psia)} \end{aligned}$$

Permeability thickness:

$$Kh = \frac{162.6 \times Qg \times Bg \times ug}{m} = 16235 \text{ md m (53266 md-ft)}$$

The thickness of the zone which is contributing flow to the wellbore is assumed to be the formation height.

$$h = h_t = 30 \text{ m} \quad \text{Permeability } K = 541 \text{ md}$$

$$\text{Total skin factor } St = 147$$

$$\text{Partial penetration skin factor } Sp = 5$$

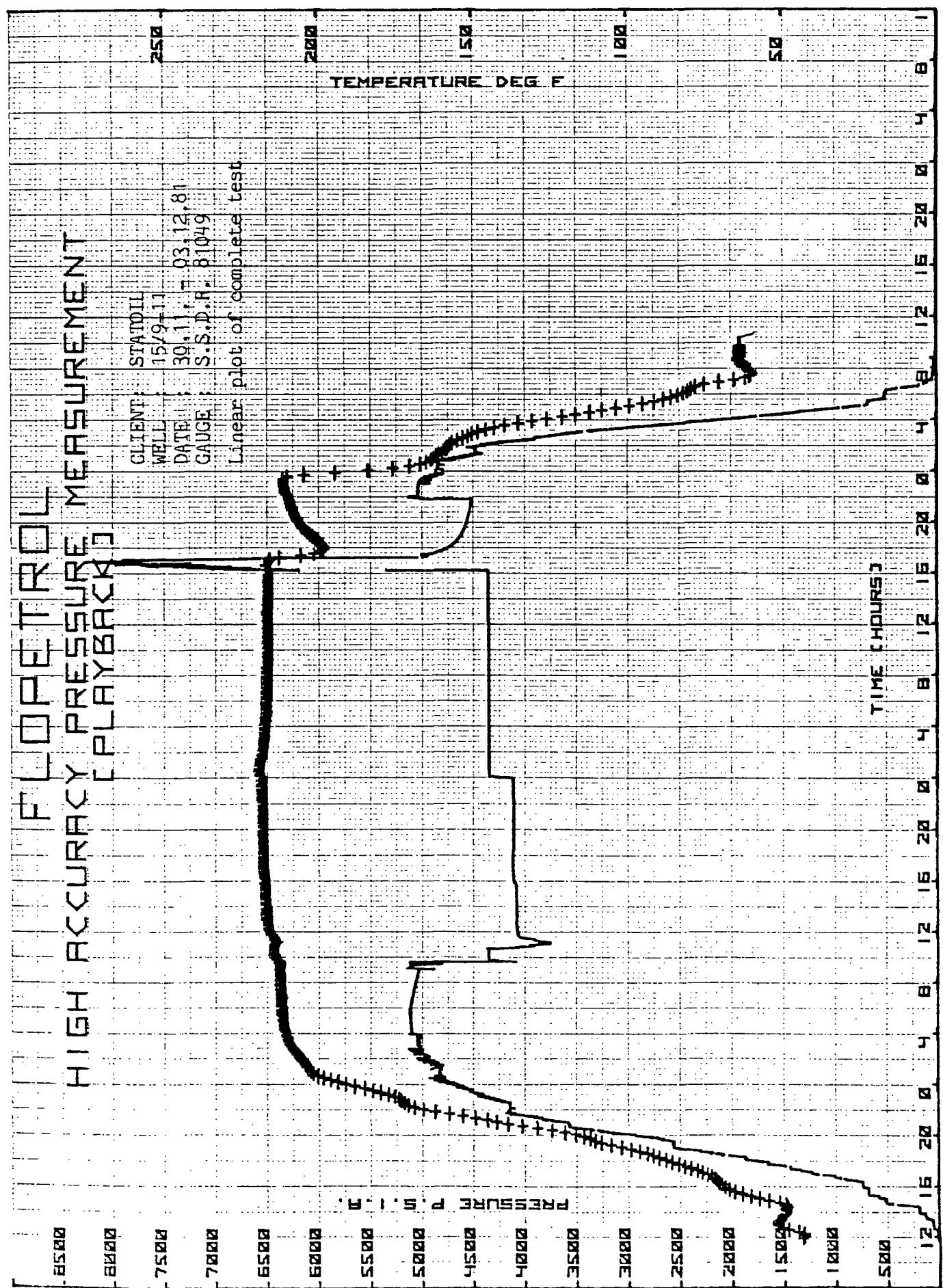
$$\text{Pressure drop due to skin: } \Delta Ps = 14.20 \text{ bar (206 psi)}$$

$$\begin{aligned} PI \text{ (real)} &= Qg / (p^* - p_{wfs}) = 41200 \text{ Sm}^3/D/\text{bar} \\ &\quad (100460 \text{ SCF/D/psi}) \end{aligned}$$

$$\begin{aligned} PI \text{ (ideal)} &= Qg / (p^* - p_{wfs} - \Delta Ps) = 810500 \text{ Sm}^3/D \\ &\quad (1.98 \text{ MMSCF/D/psi}) \end{aligned}$$

Fig. 2.1.

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BRONN 15-9-11 DST# 1  
BUILDUP NUMMER 1  
GAUGES 81049

NR.	TID	TRYKK
1	9.41	4216.730
2	9.42	4218.160
3	9.43	4217.170
4	9.44	4221.940
5	9.45	4253.260
6	9.46	4301.020
7	9.47	4338.770
8	9.48	4345.200
9	9.49	4345.480
10	9.50	4345.360
11	9.51	4346.040
12	9.52	4346.200
13	9.53	4346.270
14	9.54	4346.410
15	9.55	4346.430
16	9.56	4346.420
17	9.58	4346.410
18	10.00	4346.460
19	10.02	4346.480
20	10.04	4346.530
21	10.06	4346.500
22	10.08	4346.490
23	10.10	4346.500
24	10.12	4346.480
25	10.14	4346.490
26	10.16	4346.510
27	10.18	4346.490
28	10.20	4346.430
29	10.22	4346.470
30	10.24	4346.490
31	10.26	4346.490
32	10.28	4346.510
33	10.30	4346.380
34	10.32	4346.460
35	10.34	4346.470
36	10.36	4346.450
37	10.38	4346.460
38	10.40	4346.460

GI TYPE EDITERING

- 0 = SLUTT
- 1 = LISTING
- 2 = SLETTING
- 3 = ADDERING
- 4 = ERSTATTING

Fig. 2.2.

- 40

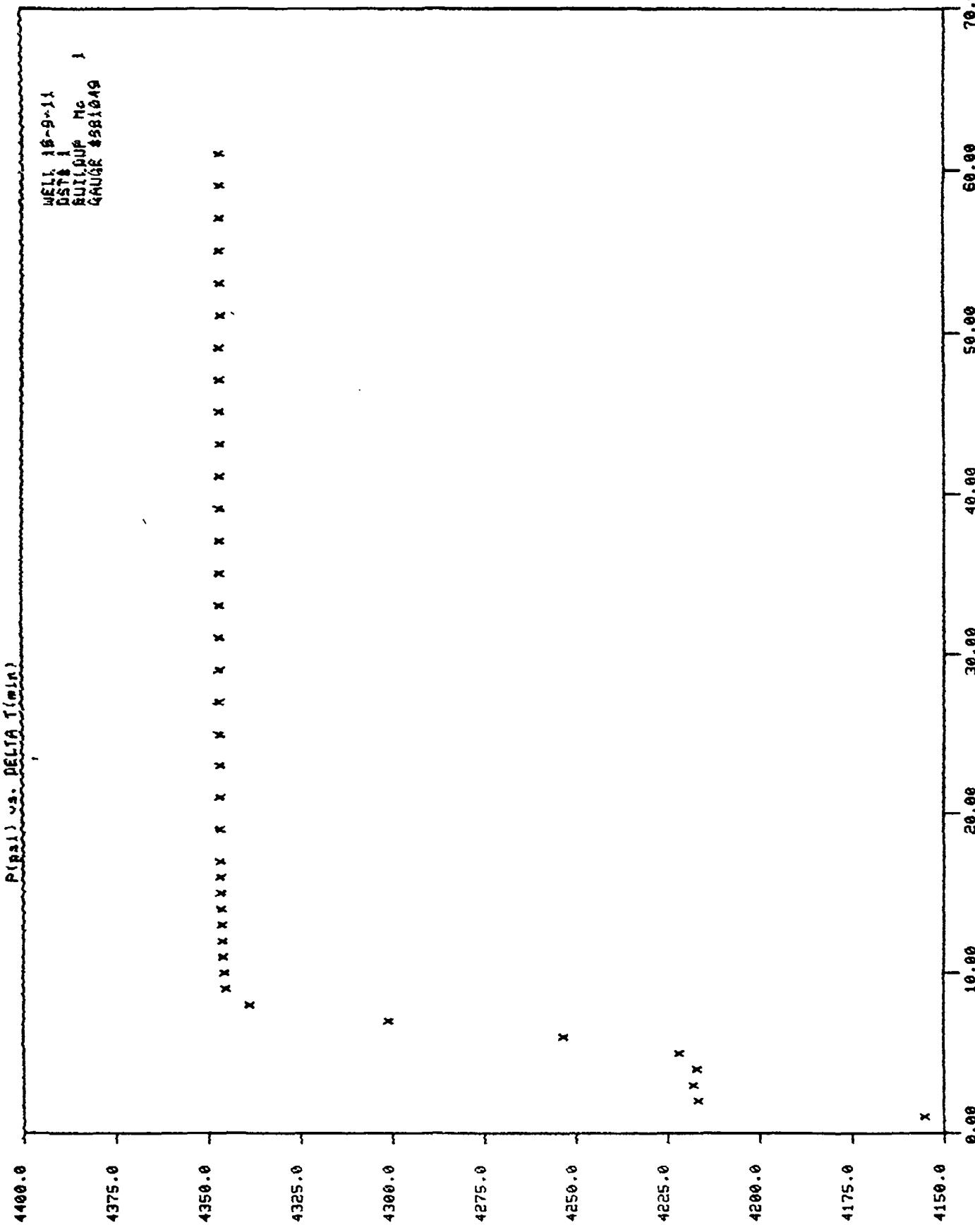


Fig. 2.3.

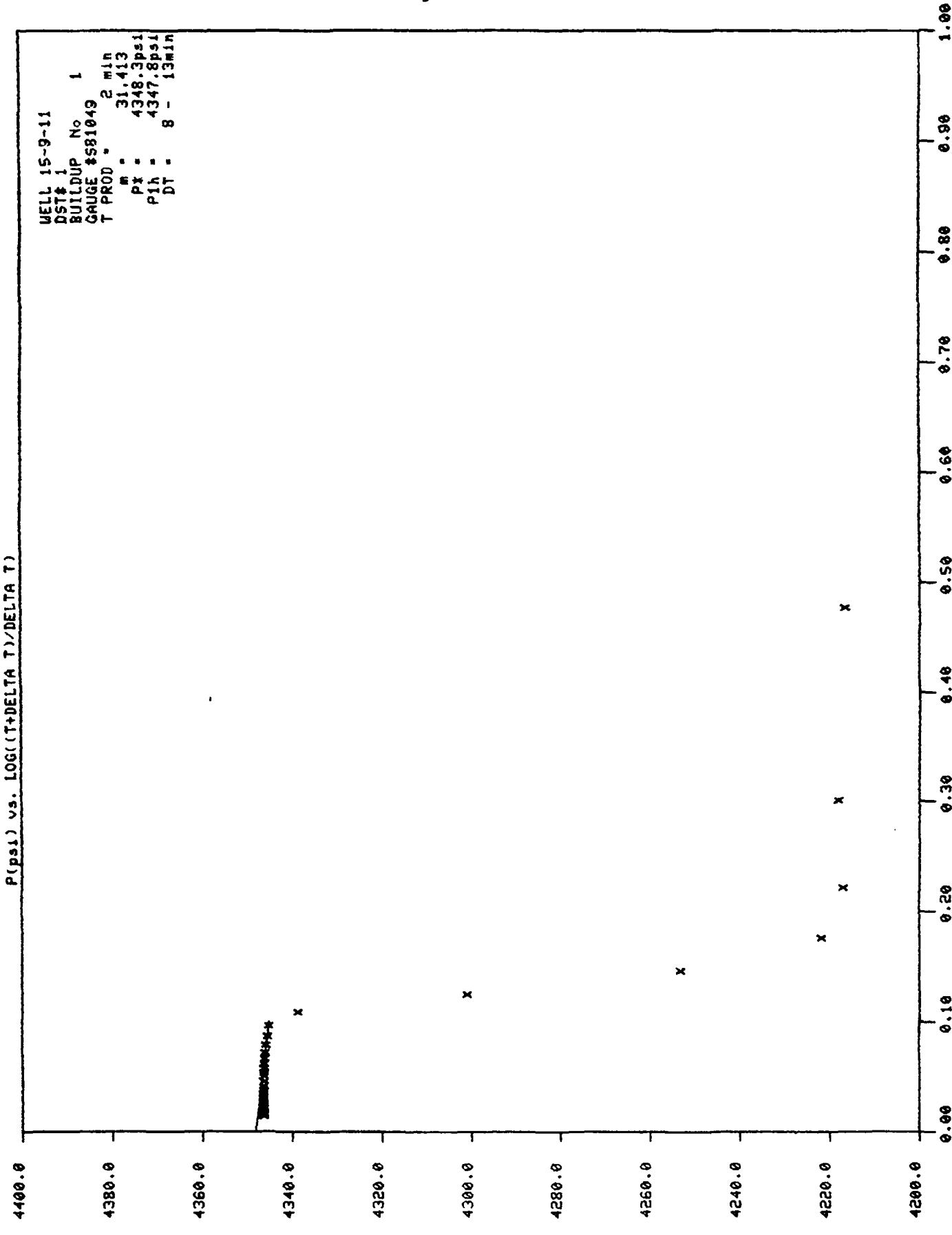


Fig. 2.4.

- 42 -

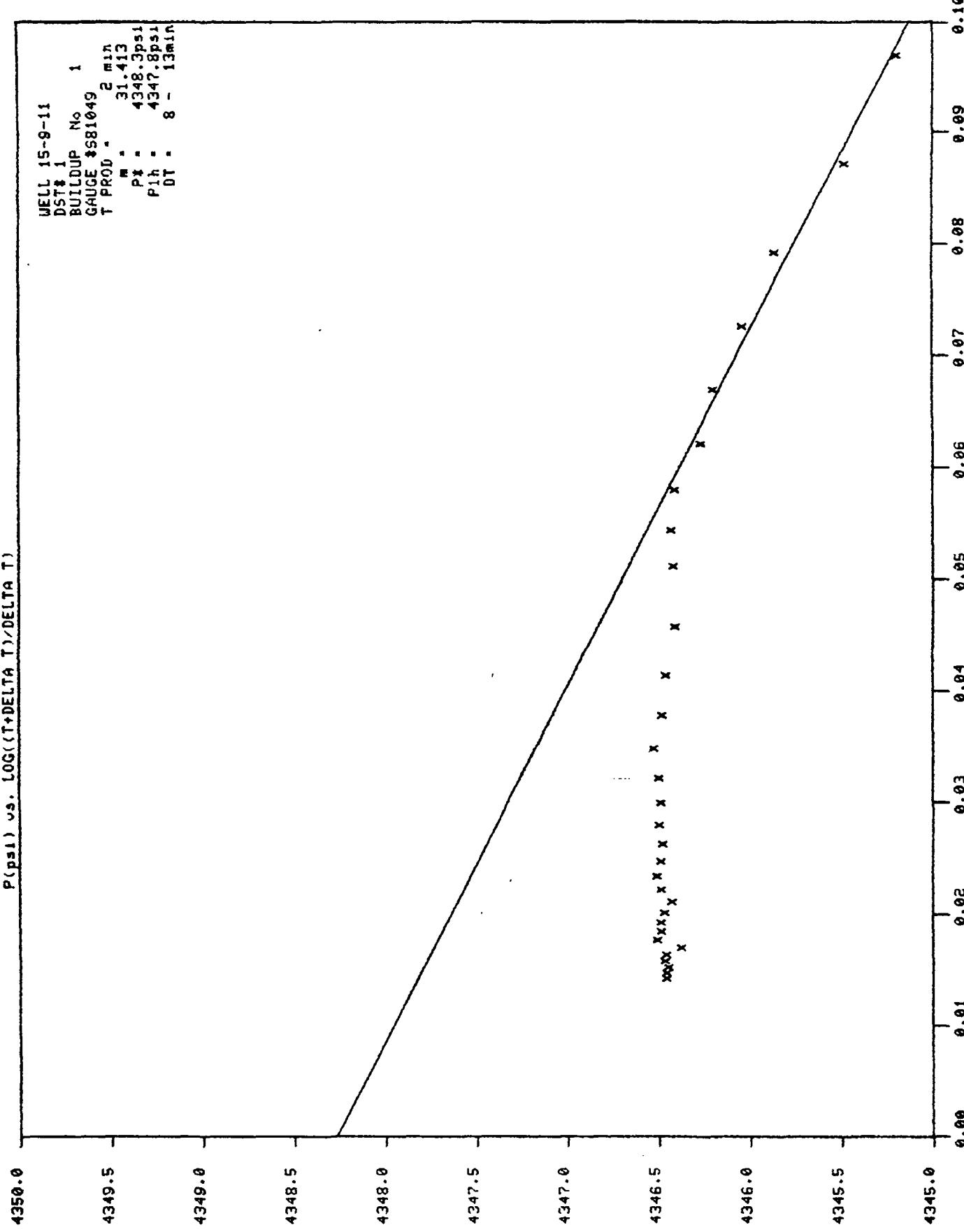
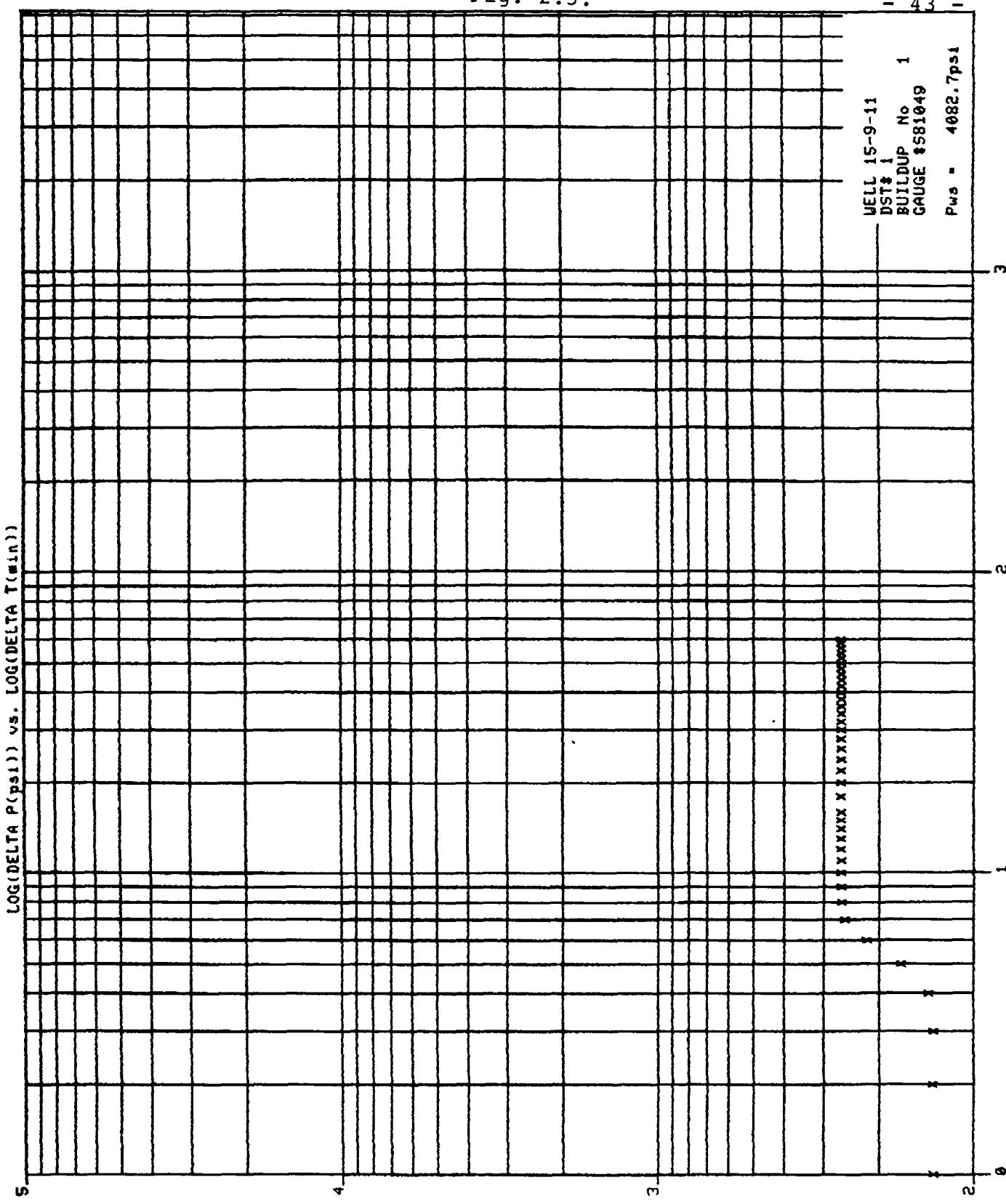


Fig. 2.5.

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BRÖNN 15-9-11 DST# 1  
 BUILDUP NUMMER 2  
 GAUGE SSDR 81049

NR.	TID	TRYKK			
1	0.01	4204.230	71	5.20	4342.700
2	0.02	4246.930	72	5.30	4342.690
3	0.03	4285.070	73	5.40	4342.730
4	0.04	4314.950	74	5.50	4342.760
5	0.05	4337.690	75	6.00	4342.740
6	0.06	4340.690	76	6.10	4342.740
7	0.07	4340.820	77	6.20	4342.780
8	0.08	4340.850	78	6.30	4342.820
9	0.09	4340.900	79	6.40	4342.790
10	0.10	4340.950	80	6.50	4342.800
11	0.11	4340.980	81	7.00	4342.820
12	0.12	4341.000	82	7.10	4342.860
13	0.13	4341.030	83	7.20	4342.880
14	0.14	4341.060	84	7.30	4342.850
15	0.15	4341.090	85	7.40	4342.840
16	0.16	4341.110	86	7.50	4342.860
17	0.17	4341.120	87	8.00	4342.890
18	0.18	4341.140	88	8.10	4342.890
19	0.19	4341.160	89	8.20	4342.910
20	0.20	4341.190	90	8.30	4342.930
21	0.22	4341.260	91	8.40	4342.950
22	0.24	4341.320	92	8.50	4342.920
23	0.26	4341.360	93	9.00	4342.910
24	0.28	4341.410	94	9.10	4342.930
25	0.30	4341.470	95	9.20	4342.950
26	0.32	4341.510	96	9.30	4342.970
27	0.34	4341.560	97	9.40	4342.970
28	0.36	4341.580	98	9.50	4342.990
29	0.38	4341.590	99	10.00	4342.990
30	0.40	4341.610	100	10.10	4343.030
31	0.42	4341.650	101	10.20	4343.030
32	0.44	4341.650	102	10.30	4342.980
33	0.45	4341.920	103	10.40	4342.970
34	0.46	4341.920	104	10.50	4342.990
35	0.50	4341.920	105	11.00	4342.990
36	0.55	4341.950	106	11.10	4343.010
37	1.00	4341.970	107	11.20	4343.030
38	1.10	4342.050	108	11.30	4343.030
39	1.20	4342.120	109	11.40	4343.050
40	1.30	4342.150	110	11.50	4343.050
41	1.40	4342.170	111	12.00	4343.050
42	1.50	4342.180	112	12.10	4343.070
43	2.00	4342.250	113	12.20	4343.070
44	2.10	4342.270	114	12.30	4343.090
45	2.20	4342.250	115	12.40	4343.090
46	2.30	4342.340	116	12.50	4343.110
47	2.40	4342.370	117	13.00	4343.110
48	2.42	4342.370	118	13.10	4343.110
49	2.44	4342.370	119	13.20	4343.080
50	2.46	4342.380	120	13.40	4343.080
51	2.48	4342.380	121	14.00	4343.070
52	2.50	4342.360	122	14.20	4343.080
53	2.52	4342.390	123	14.40	4343.080
54	2.54	4342.370	124	15.00	4343.080
55	2.56	4342.390	125	15.10	4343.100
56	2.58	4342.400	126	15.20	4343.070
57	3.00	4342.380	127	15.40	4343.020
58	3.10	4342.430	128	16.00	4343.120
59	3.20	4342.420	129	16.11	4343.160
60	3.30	4342.480			
61	3.40	4342.510			
62	3.50	4342.540			
63	4.00	4342.550			
64	4.10	4342.580			
65	4.20	4342.570			
66	4.30	4342.590			
67	4.40	4342.630			
68	4.50	4342.620			
69	5.00	4342.650			
70	5.10	4342.690			

Fig. 2.6.

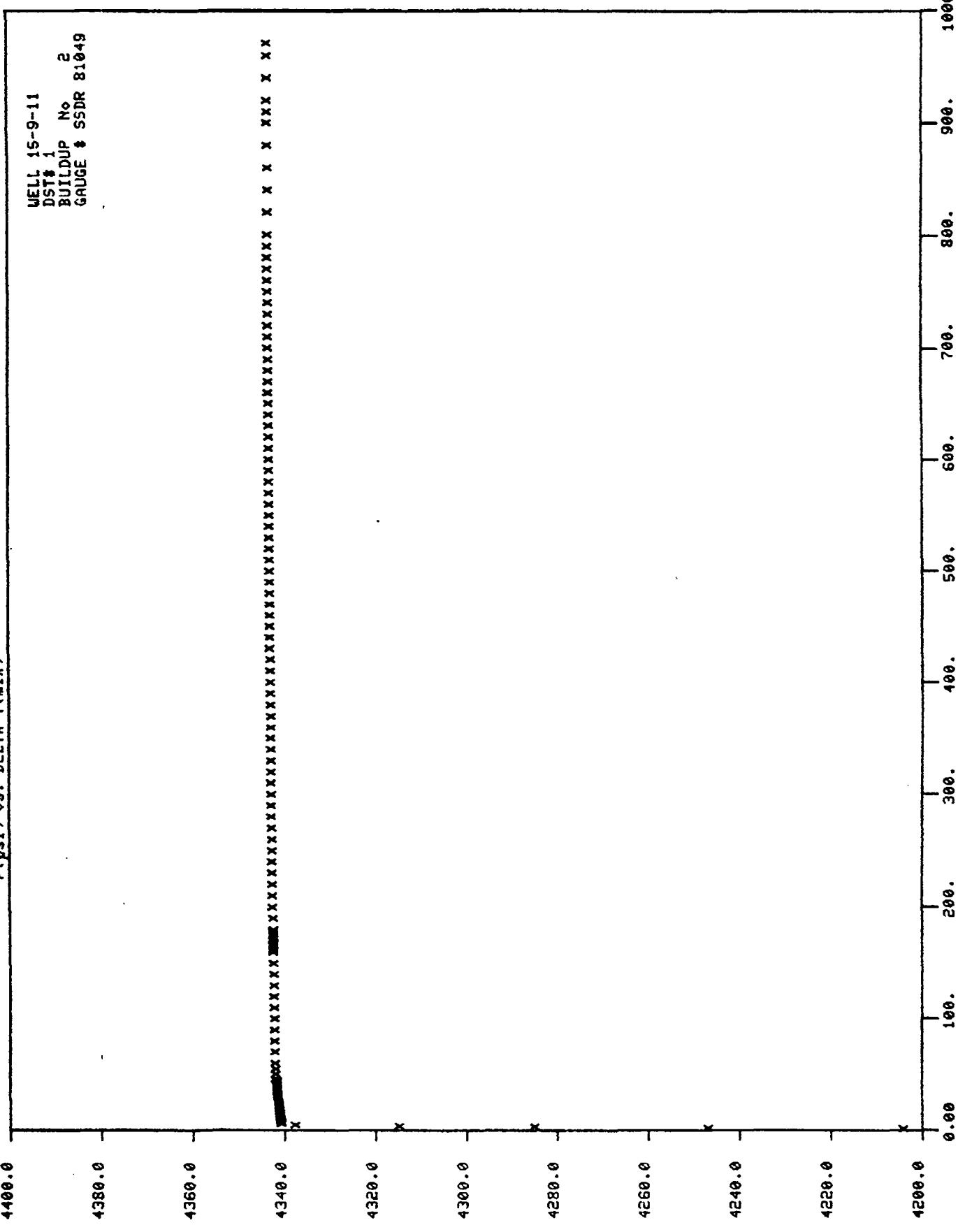


Fig. 2.7.

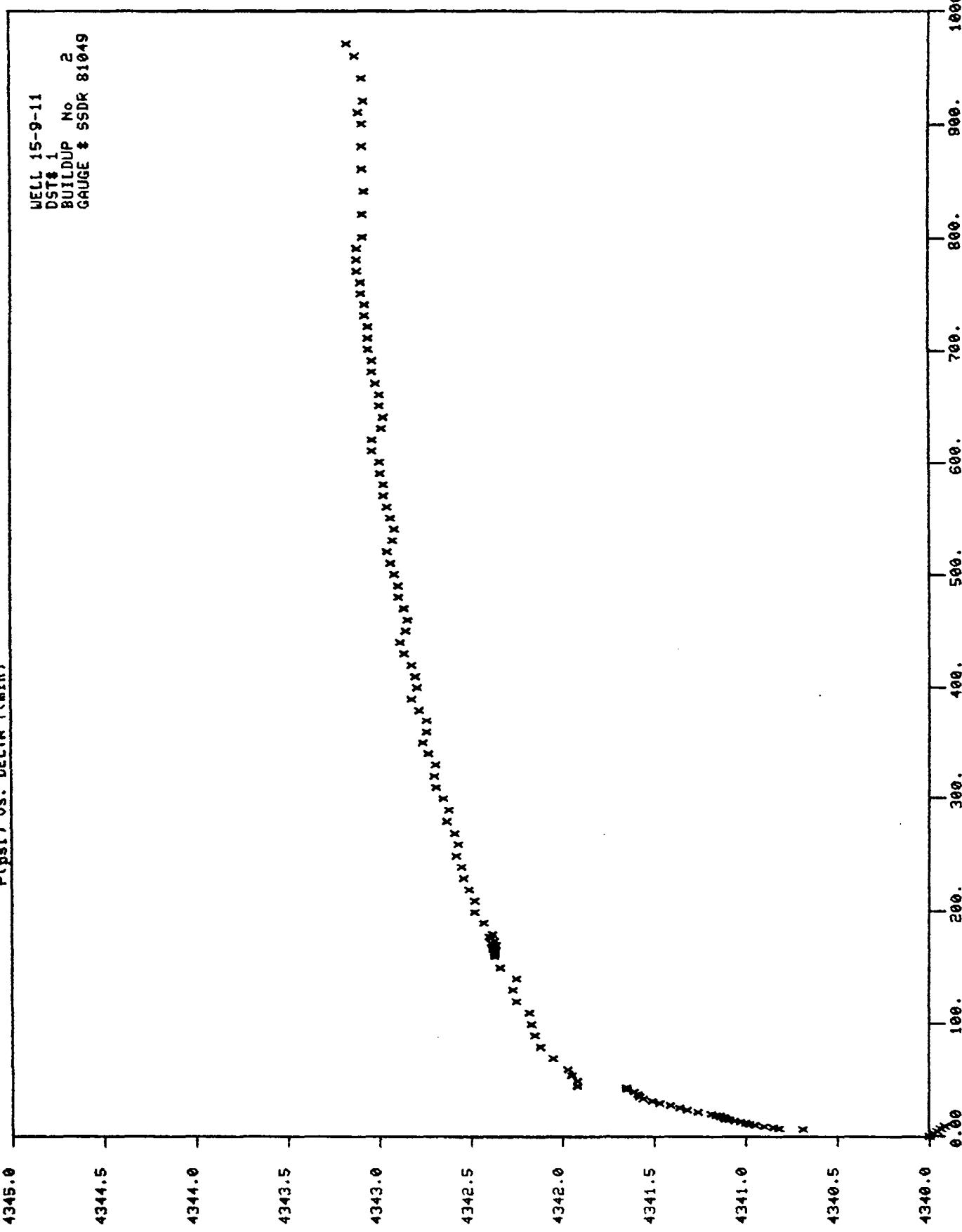


Fig. 2.8.

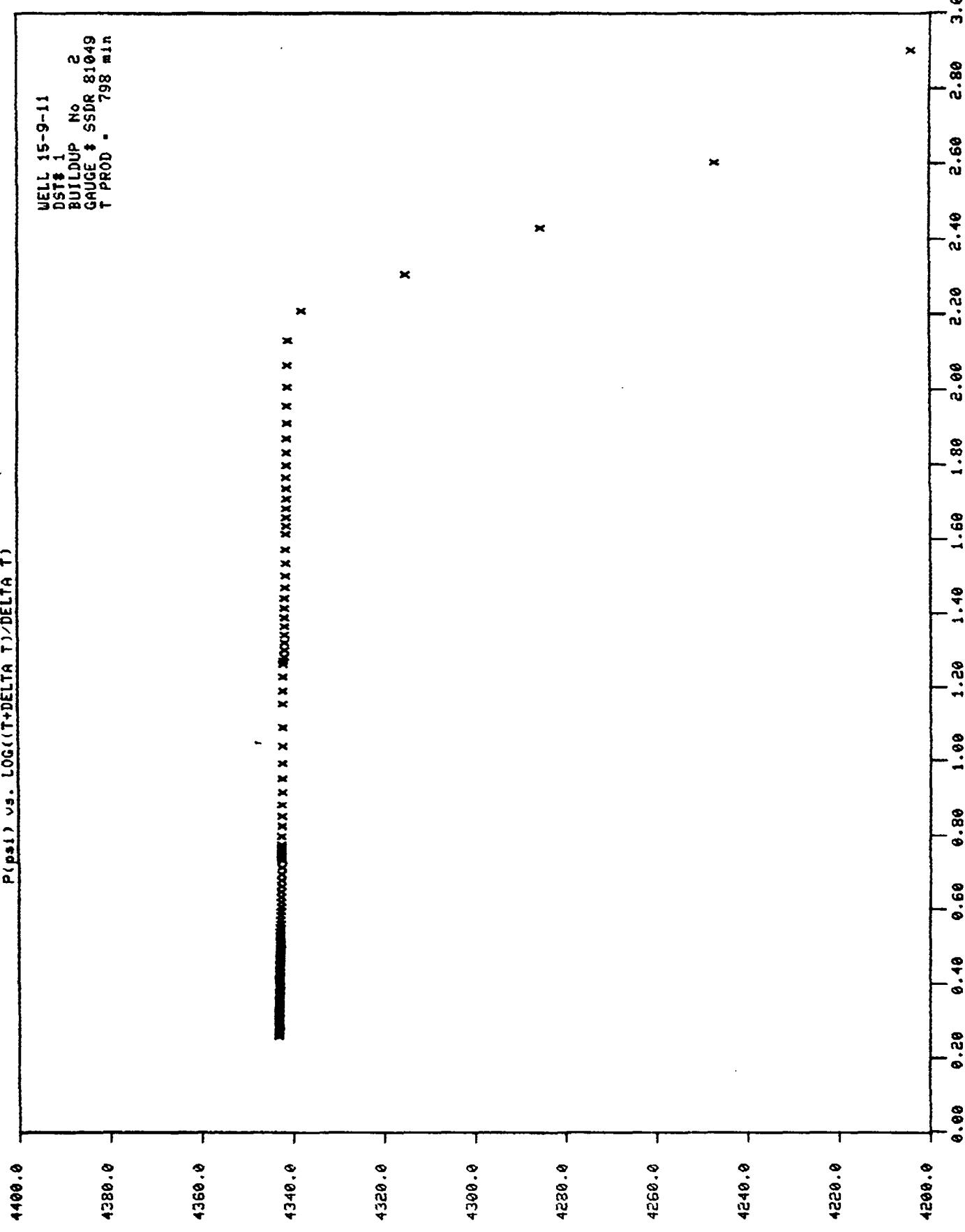


Fig. 2.9.

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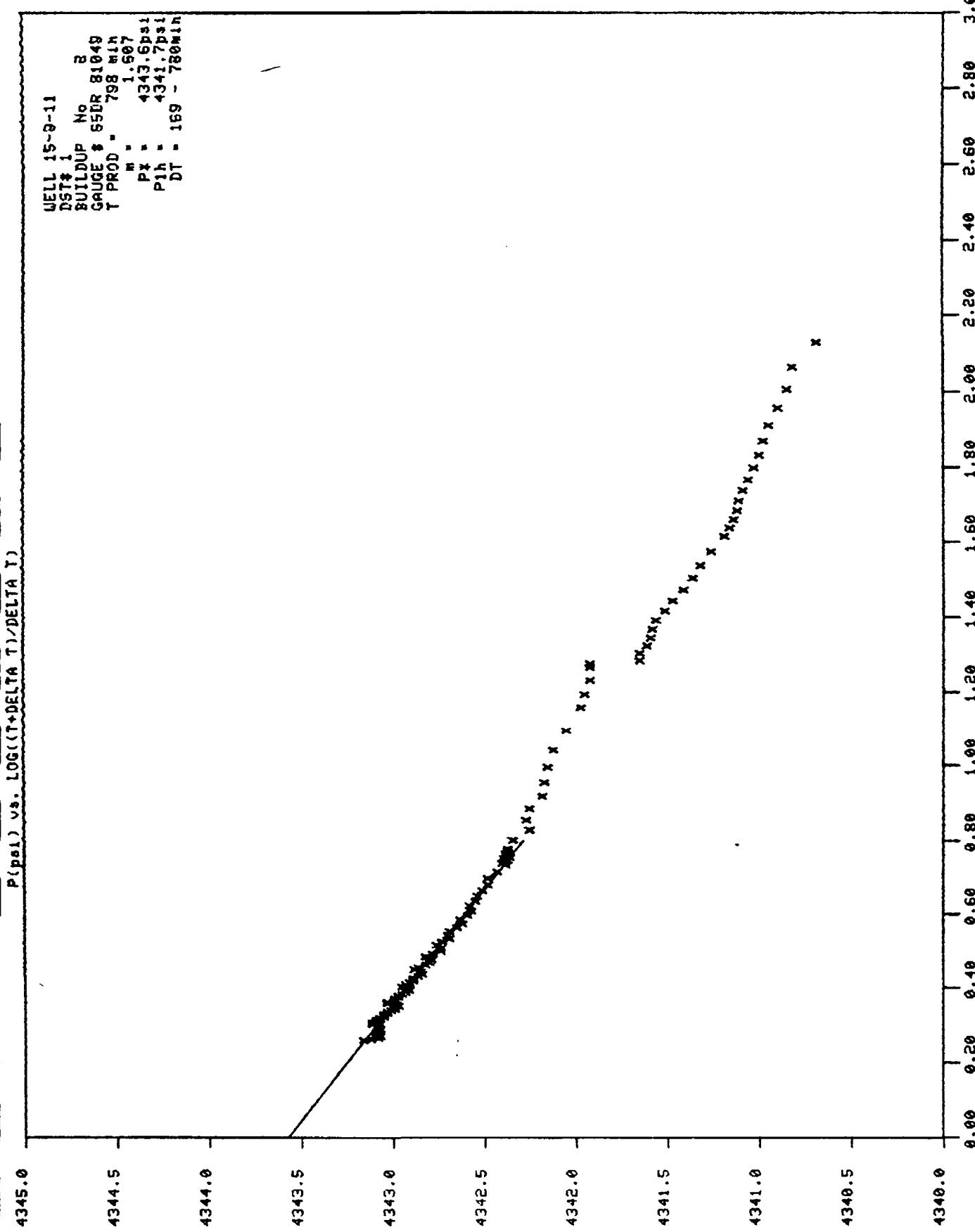
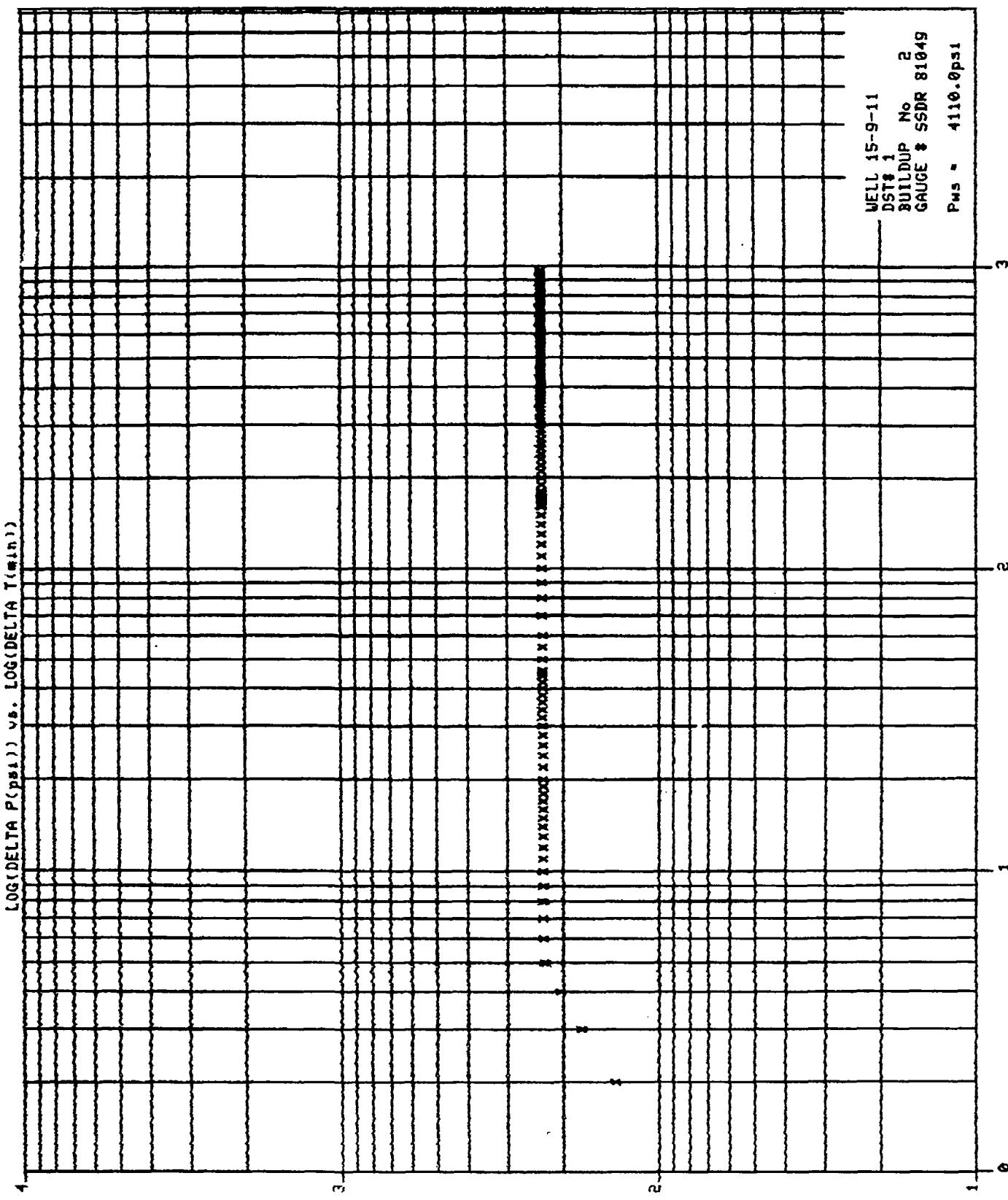


Fig. 2.10.

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APPENDIX 3

DST NO. 2

Content:

- Summary of DST no. 2.
- Lay out of test string
- Pressure recorders
- Diary of events
- Pressure, choke and flowdiagram
- Flow data
- Separator sampling
- Surface sampling
- Test analysis
- Water analysis

Figures:

- Listing of pressure data
- Sperry Sun: Pressure/Temp. vs. time plot
- $P_{ws}$  vs  $\Delta t$
- $P_{ws}$  vs  $\log((t + \Delta t)/\Delta t)$
- Log  $\Delta P$  vs  $\log \Delta t$

SUMMARY OF DST NO. 2.

Perforated interval: 2432 - 2440 m RKB

- Flow 600 min
  - 25.4 mm (64/64") choke: 10 min
  - 19.1 mm (48/64") choke: 20 min
  - 11.1 mm (28/64") choke: 121 min
  - 12.7 mm (32/64") choke: 435 min
- Build up 441 min

Average flowrates:

On 12.7 mm (32/64") choke:

- 233785 Sm<sup>3</sup>/D (8272000 SCF/D) of gas
- 104 Sm<sup>3</sup>/D (653 STB/D) of condensate
- 108 Sm<sup>3</sup>/D (680 BPD) of water

Gravities:

- Gas: 0.72 sp.gr. rel. to air
- Condensate: 0.75 sp.gr (57.4°API)
- Water: 1.042 g/cc

Separator conditions:

- Pressure: 11.07 bar (160.5 psia)
- Temperature: 17.2°C (63°F)

Gauges:

- Two Flopetrol SSDR, two Sperry Sun MRPG and two Sperry Sun MK III. One Sperry Sun MRPG erratic readings after five hours build up.

## TEST STRING TALLY, ROSS RIG 15/9-11 DST NO. 2

All measurements to top of each item

<u>Equipment description</u>	<u>ID (")</u>	<u>OD (")</u>	<u>Length (m)</u>	<u>Depth (m)</u>
<b>Otis SST w/x-over</b>				
2 jnts 5" vam tbg 18 lbs/ft 1-80	4.25	5.56	20.02	- 6.31
1 pupnjt 5" vam tbg	4.25	5.56	4.53	13.71
1 x-over 5" vam box x 4-1/2" sa pin	4.25	5.51	0.40	18.245
1 Otis lubricator valve	2.99	13.88	1.62	18.64
1 x-over 4-1/2" sa box x 5" vam pin (0-23)	4.25	5.51	0.41	20.26
1 jnt 5" vam tbg	4.25	5.56	10.32	20.67
1 jnt 5" vam tbg	4.25	5.56	9.65	30.99
2 stds 5" vam tbg	4.25	5.56	59.86	40.64
1 pupnjt 5" vam tbg	4.25	5.56	4.53	100.50
1 x-over 5 vam box x 4-1/2" 4 sa pin (f-24)	3.00	6.00	0.29	105.03
1 Flopetrol ez-tree	3.00	17.00	2.61	105.32
1 slickjnt 5" o.c. 4-1/2"-4 sa pin x pin (f-17)	3.00	5.00	2.95	107.93
1 Flopetrol fluted hanger	3.00	16.00	0.29	110.88
1 x-over 4-1/2"-4 pin x 5 vam pin (f-25)	3.00	6.00	0.31	111.17
1 pupnjt 5" vam tbg	4.25	5.56	1.22	111.48
2 jnts 5" vam tbg (no 44 and 45 from std no. 69)	4.25	5.56	19.61	112.70
68 stds 5" vam tbg	4.25	5.56	2001.92	132.31
1 x-over 5" vam box x 3-1/2" if pin	3.50	6.12	0.30	2134.23
1 slipjnt (open)	2.00	4.63	5.54	2134.53
1 slip jnt (closed)	2.00	4.65	4.01	2140.07
6 stds drill collars	2.25	4.75	171.08	2144.00
1 x-over 3-1/2" if box x 2-7/8 eue pin	2.50	4.75	0.20	2315.16
1 RTTS mech circ valve	2.44	4.87	0.84	2315.36
1 x-over 2-7/8" eue box x 3-1/2" if pin	2.62	4.75	0.20	2316.2
1 std drill collar	2.25	4.75	28.60	2316.4
1 slip jnt (closed)	2.00	4.63	4.01	2345.00
1 slip jnt (closed)	2.00	4.63	4.01	2349.01
1 std drill collar	2.25	4.75	28.61	2353.02
1 APR-M safety/circ valve	2.25	5.00	2.55	2381.63
1 dp-tester valve	2.25	5.00	1.46	2384.18

	<u>Equipment description</u>	ID ("")	OD ("")	Length (m)	Depth (m)
1	APR-N tester valve	2.25	5.00	3.86	2385.6
1	ful flo hydr. bypass	2.25	4.62	1.92	2389.5
1	big john jars	2.37	4.62	1.92	2391.42
1	x-over 3-1/2" if box x 4-1/2" if pin	3.00	6.12	0.40	2393.34
1	RTTS safety jnt	3.12	6.12	1.08	2393.74
1	RTTS packer (above)	3.75	8.25	0.98	2394.82
	RTTS packer (below)	3.75	8.25	0.80	2395.80
1	x-over 4-1/2" if x 3-1/2" fh	2.50	6.12	0.21	2396.60
1	x-over 3-1/2" fh x 2-7/8" eue	2.40	4.75	0.20	2396.81
1	perf. pupnjt 2-7/8" eue	2.44	2.88	3.54	2397.01
1	x-over 2-7/8" eue box x 2-3/8" eue pin	2.00	3.70	0.26	2400.55
1	collar 2-3/8" eue	-	2.88	0.13	2400.81
1	Otis xn-nipple 2-3/8" eue pin x pin	1.79	2.38	0.22	2400.94
1	x-over 2-3/8" eue box x 2-7/8" eue pin	2.00	3.70	0.26	2401.16
1	jnt 2-7/8" eue tbg	2.44	2.88	9.41	2401.42
1	pupnjt 2-7/8" eue	2.44	2.88	2.40	2410.83
	Flopertrol DST-hanger				
1	jnt 2-7/8" eue tbg	2.44	2.88	8.93	2413.23
1	perf. pupnjt 2-7/8" eue	2.44	2.88	2.05	2422.16
1	x-over 2-7/8" eue box x 3-1/8" eue pin	2.25	4.25	0.31	2424.21
1	Halliburton APBT carrier	-	3.00	1.51	2424.52
1	x-over 3-1/8" eue box x 2-7/8" eue pin	1.88	3.88	0.18	2426.03
1	bullplug w/cross 2-7/8" eue box	-	4.00	0.21	<u>2426.21</u>
					2426.42

WELL NO.: 15/9-11 DST NO.: 2 DATE: 7/12-81  
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WIRELINE NIPPLE OTIS XN-NIPPLE 2400.94m

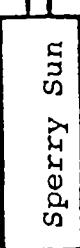
GAUGE TYPE AND NUMBER: Flopetrol SSDR no. 81048

DEPTH, PRESSURE ELEMENT: 2406.36 RANGE: 0 - 10 000 psi

MODE: 1 min. sampling DELAY: -

ACTUATED: time 04:41 date: 7.12.81

WILL RUN OUT: time 18:01 date: 10.12.81



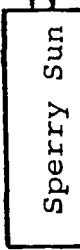
GAUGE TYPE AND NUMBER: MRPG 0041

DEPTH, PRESSURE ELEMENT: 2409.76 RANGE: 6000 psi

MODE: 2 min DELAY: 8.5 hrs

ACTUATED: time: 04.58 date: 7.12.81

WILL RUN OUT: time: 21:00 date: 9.12.81



GAUGE TYPE AND NUMBER: MRPG III no. 1-12-1731

DEPTH, PRESSURE ELEMENT: 2412.28 m RANGE: 10 000 psi

MODE: 2 min DELAY: 8.5 hrs

ACTUATED: time: 04:54 date: 7.12.81

WILL RUN OUT: time: 21:00 date: 9.12.81



D.S.T. HANGER 2413.23 m

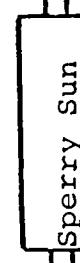
GAUGE TYPE AND NUMBER: Flopetrol SSDR no. 81049

DEPTH, PRESSURE ELEMENT: 2417.07 m RANGE: 0 - 10 000 psi

MODE: 1 min DELAY: -

ACTUATED: time: 04:26 date: 7.12.81

WILL RUN OUT: time: 17:46 date: 10.12.81



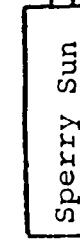
GAUGE TYPE AND NUMBER: MRPG 0136

DEPTH, PRESSURE ELEMENT: 2420.88 m RANGE: 6000 psi

MODE: 2 min DELAY: -

ACTUATED: time: 05:01 date: 7.12.81

WILL RUN OUT: time: 13:00 date: 9.12.81



GAUGE TYPE AND NUMBER: MRPG III no. 1-9-1751

DEPTH, PRESSURE ELEMENT: 2423.50 m RANGE: 10 000 psi

MODE: 2 min DELAY: 8.5 hrs

ACTUATED: time: 04:55 date: 7.12.81

WILL RUN OUT: time: 21:00 date: 9.12.81

DIARY OF EVENTS		WELL No. <u>15/9-11</u>	DST No. <u>2</u>
DATE	TIME	OPERATIONS	
071281	0330	<u>Perforation</u> Perforated 4sh/ft 2432 - 2440 m RKB. All shots fired.	
	0430	<u>RIH w/teststring</u> Started running teststring.	
	18:00	Held meeting with service people	
081281	0037	Sat packer	
	0100	<u>Flow</u> Opened APR-N valve	
	0107	13 psi increasing to 84 psi at wellhead Opened on 64/64" adjustable choke 202 psi on WH	
	0111	Changed to 48/64" adjustable choke	
	0117	Changed to 48/64" fixed choke	
	0121	Gas to surface. WHP = 1500 psi Backpressure 600 psi	
	0130	Sand = 8%	
	0137	Reduced to 28/64" adj. choke	
	0145	Changed to 28/64" fixed choke.. WHP = 2000 psi. Backpressure = 400 psi. Sand = 0.4%	
	0200	Sand = 0.5%. H <sub>2</sub> O = 40%. CO <sub>2</sub> = 0.5%	
	0338	Changed to 32/64" fixed choke	
	0415	Sand = 0.1%. H <sub>2</sub> O = 60%. WHP = 1994 psi. Backpressure = 700 psi	
	0427	Flow through separator. 3". orifice	
	0430	Sand = traces. H <sub>2</sub> O = 65%. CO <sub>2</sub> = 0.5%	
	0445	H <sub>2</sub> O = 70%	
	0500	H <sub>2</sub> O = 75%. Sand = 0.5%. CO <sub>2</sub> = 0.1% Condensate gravity = 0.736 at 10.3 °C.	
	0511	Stock tank: 35 bbls increase of H <sub>2</sub> O in 44 mins 1145 BPD of H <sub>2</sub> O	
	0521	WHP = 2030 psi	

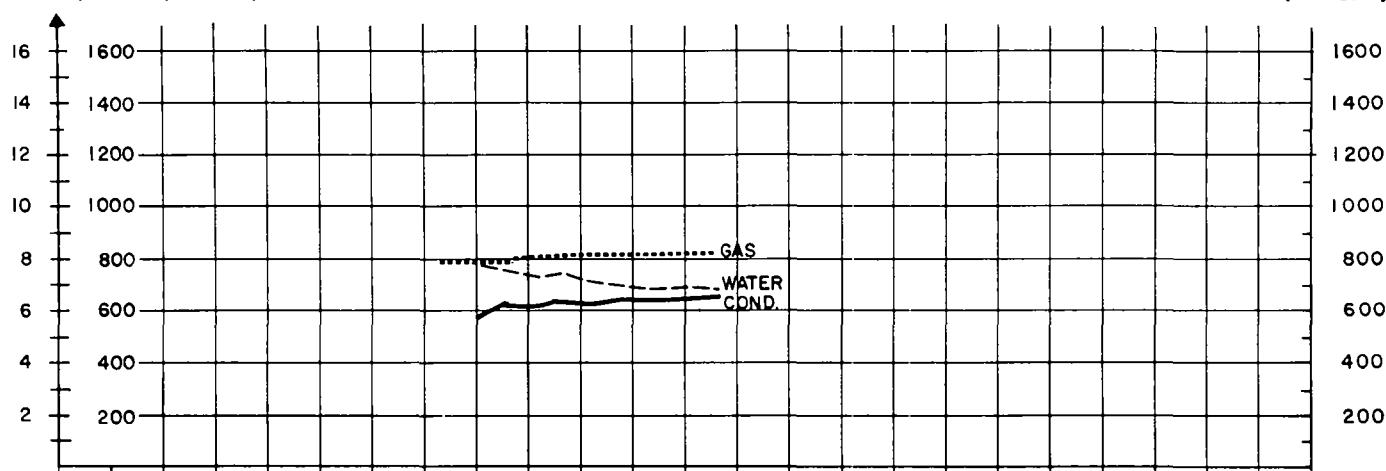
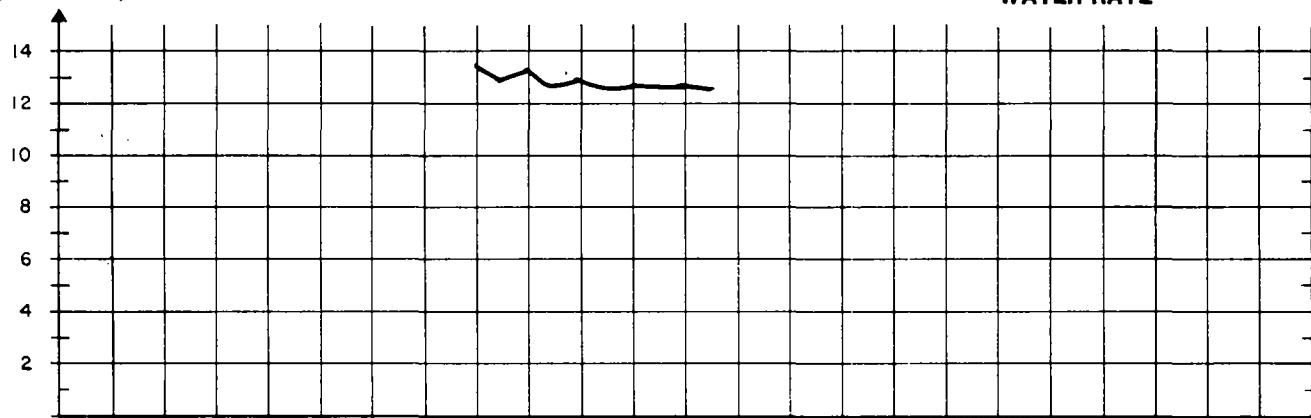
COMMENTS:

PE:

DIARY OF EVENTS		WELL No. <u>15/9-11</u>	DST No. <u>2</u>
ZONE TESTED <u>Heimdal</u>		PERFS. <u>2432 - 2440m</u>	
DATE	TIME	OPERATIONS	
081281	0645	Rates from separator: Gas = 7.9 MMSCFD. Condensate = 560 BPD. Water = 760 BPD Water meter factor = 0.98	
	0915	WHP = 2095 psi. Stable last hour	
	0930	Started taking PVT sample no. 1.	
	1035	Finished PVT sample no. 1.	
	1051	Leak in heater outlet. Tried to bypass heater, bypass valve stuck	
	1053	Shut in well on choke manifold	
	1100	Shut in APR-N valve	
		<u>Build-up</u>	
	1100	WHP = 2300 psig	
091281	0600	APR-N valve leaking	
	0800	WHP stabilized on 2440 psig	
		<u>Killing well</u>	
	0821	Bleed tubing through adj. choke to burner (48/64")	
	0835	Pressure down to 1500 psig at manifold	
	0836	Shut in well at choke manifold	
	0839	WHP increased to 2000 psig	
	0840	Bleed tubing through adj. choke to burner (48/64")	
	0847	Wellhead pressure bled to 1390 psig	
	0848	Shut in well at choke manifold. WHP build to 1600 psig	
	1003	Started bullheading.	
COMMENTS:			
PE:			

WELL NO : 15/9-II DST NO.: 2

## PRESSURE CHOKE AND FLOWDIAGRAM

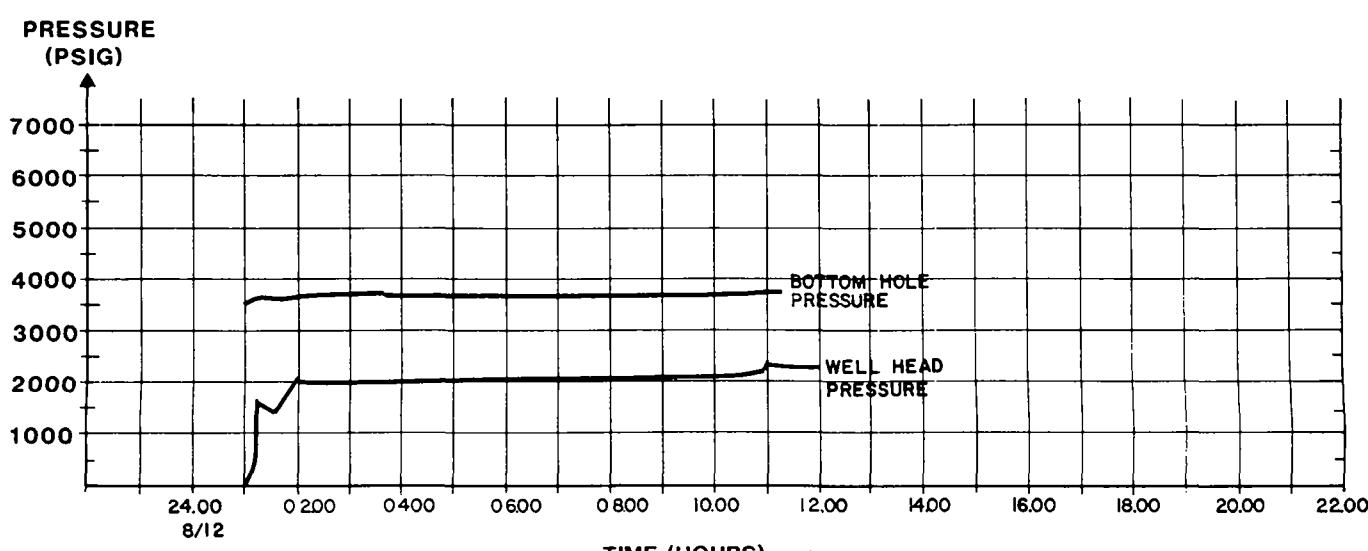
GAS RATE  
(MMSCF/D)WATER RATE  
(BBLs/D)GOR  
(SCF/STB)OIL/COND. RATE ——  
GAS RATE .....  
WATER RATE - - -CHOKE SIZES  
(INCHES)  
64/64  
48/64  
32/64  
28/64  
24/64  
18/64  
16/64  
14/64  
CLOSEDHEATER  
CHOKE MANIFOLD

0107 1053

PRESSURE  
(PSIG)BOTTOM HOLE  
PRESSUREWELL HEAD  
PRESSURE

8/12

TIME (HOURS) →



**FLOW DATA**  
15/9-11 DST no. 2. (2432 - 2440 m RKB)

Date/Time	Bottom hole	Well head	Chokes	Separator data								Liq. and gas analysis at goos neck									
				Press. Psi g	Temp. F	Press. Psi g	Temp. F	Manifold	Heater 64. inc.	Press. Psi g	Temp. F	Gas rat. mmscf/d	Oil rate stb/d	GOR scf/stb	Oil API	Gas S.G.	Water %	Water rate bbls/d	Sedim. %	Oil API	Co2
8.12.81																					
01:00	2666	1711.7	13																		
01:07	3236	194.3	250																		
01:11	3249	196.4	1150																		
01:17	3384	196.4	1600																		
01:21	3335	196.4	1600																		
01:37	3290	197.8	1550																		
01:45	3335	197.8	1800																		
03:38	3424	198.5	2000	72		32/64	"												60.7		
04:12	3417	198.5																	62.3		
04:27	3416	198.5																			
04:30	3417	198.5	2010	81	"	"												65	Trace		
04:45	3417	198.5	2015	82	"	"												70	Trace		
05:00	3416	199.2	2020	82	"	"												75	0.5		
05:15	3418	199.2	2030	82	"	"													0.5		
05:30	3418	199.2	2035	82	"	"														0.4	0.2
06:00	3418	199.2	2040	81	"	"												70	792.8	0.0	63.4
06:30	3419	199.2	2065	82	"	"												"	767.3	0.4	57.4
07:00	3420	199.2	2070	82	"	"												"	735.2	0.4	
07:30	3421	199.2	2080	86	"	"												"	751.77	0.4	48.5
08:00	3422	199.2	2085	86	"	"												"	713.02	0.4	
08:30	3422	199.2	2090	84	"	"												"	702.1	0.4	
09:00	3423	199.2	2095	86	"	"												"	688.86	0.3	"
09:30	3424	199.9	2095	86	"	"												"	679.88	0.3	"
10:00	3426	199.9	2100	84	"	"												"	685.08	0.4	"
10:30	3426	199.9	2110	86	"	"												"	674.88	0.4	"
10:50	3439	199.9																			
10:53	3477	199.9																			
11:00	3507	199.9																			

DST SUMMARY DATASHEET D: SEPARATOR AND BOTTOM HOLE SAMPLING

Well no.: 15/9-11 DST no.: 2 Date: 8.12.81

1. Separator samples

Bottle no.	Oil/Gas	Time	Oil rate	Gas rate
9209/100	Oil	09:30	647.01 bbls/d	8.237 MMSCFD
A-10915	Gas	09:30	"	"
A-4987	Gas	09:30	"	"

2. Bottom hole samples

Bottle no.	Sampling depth	Sampling presure	Opening pressure	Transfer BPP	True BPP (lab)
NONE					

## SAMPLING

### During flow:

- 1 x 20 l jerry-can of condensate from separator
- 6 x 1 l plastic bottles of water from separator

### After shut-in:

- 1 drum of condensate from separator
- 1 x 10 l jerry-can of condensate from separator
- 2 x 20 l plastic-cans of water from separator

### Note:

Few samples were taken during the flow because the well had to be shut-in too early as a result of leak in the heater-manifold.

## TEST ANALYSIS

### Input data, reservoir parameters:

Vapor volume equivalent:

$v_{cs} = 160 \text{ m}^3/\text{m}^3$  (900 SCF/STB) at 10.10 bar (146 psig) and  
0.749 sp.g. ( $57.4^\circ\text{API}$ ) on separator.

Last averaged rates on 12.7 mm (32/64") choke:

$$Q_g = 233785 \text{ Sm}^3 = 8272000 \text{ SCF/D}$$

$$Q_{cond} = 104 \text{ Sm}^3/\text{D} = 653 \text{ STB/D}$$

$$Q_w = 108 \text{ Sm}^3/\text{D} = 680 \text{ BPD}$$

$$Q_{geq} = 233785 + 104 \times 160 = 250425 \text{ Sm}^3/\text{D} = 8860767 \text{ SCF/D}$$

$$T_{eff} = T_{prod} = 600 \text{ minutes}$$

Reservoir temperature:  $T_{res} = 87.2^\circ\text{C} (189^\circ\text{F})$

Specific gravity of gas:  $\gamma_{res} = 0.927$

Compressibility factor:  $Z = 0.833$

Viscosity of formation water:  $\mu_w = 0.370 \text{ cp}$

Viscosity of reservoir gas:  $\mu_g = 0.029 \text{ cp}$

Compressibility of reservoir gas:  $C_g = 276.6 \times 10^{-5} \text{ bar}^{-1}$   
 $(1.907 \times 10^{-4} \text{ psi}^{-1})$

Compressibility of formation water:  $C_w = 4.4 \times 10^{-5} \text{ bar}^{-1}$   
 $(3.053 \times 10^{-6} \text{ psi}^{-1})$

Compressibility of the formation:  $C_f = 4.9 \times 10^{-5} \text{ bar}^{-1}$   
 $(3.358 \times 10^{-6} \text{ psi}^{-1})$

Gas formation volume factor:  $B_g = 4.34 \times 10^{-3} \text{ m}^3/\text{m}^3$   
 $(7.72 \times 10^{-4} \text{ RB/SCF})$

Water saturation:  $S_w = 80.1 \%$

Gas saturation:  $S_g = 19.9 \%$

Porosity:  $\phi = 24.4 \%$

Perforated height:  $h_p = 8 \text{ m} (26.2 \text{ ft})$

Formation height:  $h_f = 12 \text{ m} (39.4 \text{ ft})$

Wellbore radius:  $r_w = 0.155 \text{ m} (0.51 \text{ ft})$

NaCl: 5.6 %

PVT data, viscosities and compressibilities are calculated  
parameters.

NaCl is measured on water samples in Statoil Lab.

Results:

The Sperry Sun MK III 2 gauge is used for the analysis.

Horner analysis:

$$P^* = 244.20 \text{ bar (3541.8 psia)}$$

$$P_{1\text{hr}} = 244.06 \text{ bar (3539.8 psia)}$$

$$m = 0.1329 \text{ bar/cycle (1.928 psi/cycle)}$$

$$P_{wfs} = 236.8 \text{ bar (3434.5 psia)}$$

$$\text{Total compressibility: } C_t = 63.4 \times 10^{-5} \text{ bar}^{-1}$$
$$(4.375 \times 10^{-5} \text{ psi}^{-1})$$

Effective gas permeability:

$$\left(\frac{K}{u}\right)_g \times h = \frac{162.6 \times (1000) (Q_g - 0.001 (Q_{Rs} + Q_w R_{sw})) B_g}{m}$$

$$= \frac{576298 \frac{\text{md-ft}}{\text{CP}}}{m} = \frac{175655 \frac{\text{md-m}}{\text{CP}}}{m}$$

$$K_g = \underline{424.5 \text{ md}}$$

Effective water permeability:

$$\left(\frac{K}{u}\right)_w \times h = \frac{162.6 \times Q_w \times B_w}{m} = \frac{59069 \frac{\text{md-ft}}{\text{DP}}}{m} = \frac{18004 \frac{\text{md-m}}{\text{CP}}}{m}$$

$$K_w = \underline{555 \text{ md}}$$

For the permeability calculations,  $h = h_f = 12 \text{ m (39.4 ft)}$  has been used.

Total mobility:

$$\left(\frac{K}{u}\right)_t = \left(\frac{K}{u}\right)_g + \left(\frac{K}{u}\right)_w = \frac{16138 \frac{\text{md}}{\text{CP}}}{m}$$

Total skin factor:

$$St = \underline{55.3}$$

Pressure drop due to skin:

$$Ps = 0.87 \times m \times St = \underline{6.39 \text{ bar}} = \underline{92.8 \text{ psi}}$$

$$\text{PI (real)} = \frac{Qg}{(P^* - P_{wfs})} = \underline{33850 \text{ Sm}^3/\text{D/bar}} = \underline{82579 \text{ SCF/D/psi}}$$

$$\text{PI (ideal)} = \frac{Qg}{(P^* - P_{wfs} - Ps)} = \underline{250490 \text{ Sm}^3/\text{D/bar}} = \underline{611087 \text{ SCF/D/psi}}$$

Calculated initial reservoir pressures from the gauges used in the test.

<u>Gauge</u>	<u>Depth (mRKB)</u>	<u>P* (psig)</u>
Flopetroil SSDR 81048	2406.36	3525.2
Sperry Sun MRPG 0041	2409.76	3526.0
Sperry Sun MK III 2	2412.3	3527.3
Flopetroil SSDR 81049	2417.07	3527.3
Sperry Sum MRPG 0136	2420.88	3530.7
Sperry Sun MK III 1	2423.5	3536.0

These pressures have been used in the RFT-plot.

## WATER ANALYSIS

Analysis of water from separator taken December 8th at 11:30 - 1230 hours.

The water was sampled after shut-in.

Table 1. Results of ion analysis of water sample.

Density at 20°C, g/cm <sup>3</sup>	1.0420		
pH	6.69		
Total Dissolved solid, %	6.21		
Conductivity at 20°C, mmho/cm	80.0		
<b>Ion concentration</b>	<b>(ppm)</b>	<b>emp</b>	<b>RSD %</b>
Na <sup>+</sup>	20633.	897.5	2
K <sup>+</sup>	207.	5.3	1
Mg <sup>2+</sup>	273	22.5	1
Ca <sup>2+</sup>	2029	101.2	1.4
Ba <sup>2+</sup>	64	0.9	1.5
Sr <sup>2+</sup>	343	7.82	2
Fe <sup>n+</sup>	40.5	-	2
Li <sup>+</sup>	3.6	0.5	2
Zn <sup>2+</sup>	0.24	0.07	8
Mn <sup>n+</sup>	5.4	-	3
C <sub>r</sub> <sup>n+</sup>	9.3	1.3	4
Si <sup>n+</sup>	<0.1	-	10
Cl <sup>-</sup> including (Br <sup>-</sup> and i)	35495	1001.0	1
P <sub>2</sub> O <sub>5</sub> <sup>2-</sup>	0	-	1
SO <sub>4</sub> <sup>2-</sup>	15	0.4	1
CO <sub>3</sub> <sup>2-</sup>	0	0	1
HCO <sub>3</sub> <sup>-</sup>	403	6.6	1
Sum ion	5.95		0.9
Sum anion/cation		1008.0/1037.1	1/2
Deficiency in cation		29.1	

## DISCUSSION

### Ion analysis

A Good balance between the anions and cations was obtained as illustrated in table 1. The small difference observed is within the experimental uncertainty. The consistency in the analysis is also demonstrated by the agreement between calculated numbers for total dissolved solids (TDS). The calculated value is based on the equivalent amount (Table 2) of pure NaCl solutions found in Handbook (1).

Furthermore, there is a good agreement between TDS calculated either from the results in table 1, from the Cl<sup>-</sup> concentration, density or conductivity.

Table 2. Comparison of calculated and measured total dissolved solid data (%).

	RSD %
Residue after evaporation	6.21
Calculated from table 1	5.95
Calculated from Cl <sup>-</sup> (Cl <sup>-</sup> x 1.65)	5.86
Correlated from density	6.10
Correlated from conductivity	5.80
"Equivalent NaCl", from appendix 2	5.86

### Comparison with mud filtrate

Unfortunately we have not been able to compare the water analysis with similar analysis on mudfiltrate.

The information we have on mudfiltrate is an extract from the mud report.

Table 3. Data for mud filtrate from mud report.

<u>Ion</u>	<u>Concentration mg/l</u>
$\text{Ca}^{2+}$	160
$\text{Cl}^-$	23000

It is seen that:

$\text{Cl}^-$  sample >  $\text{Cl}^-$  filtrate  
 $\text{Ca}^{2+}$  sample >>  $\text{Ca}^{2+}$  filtrate

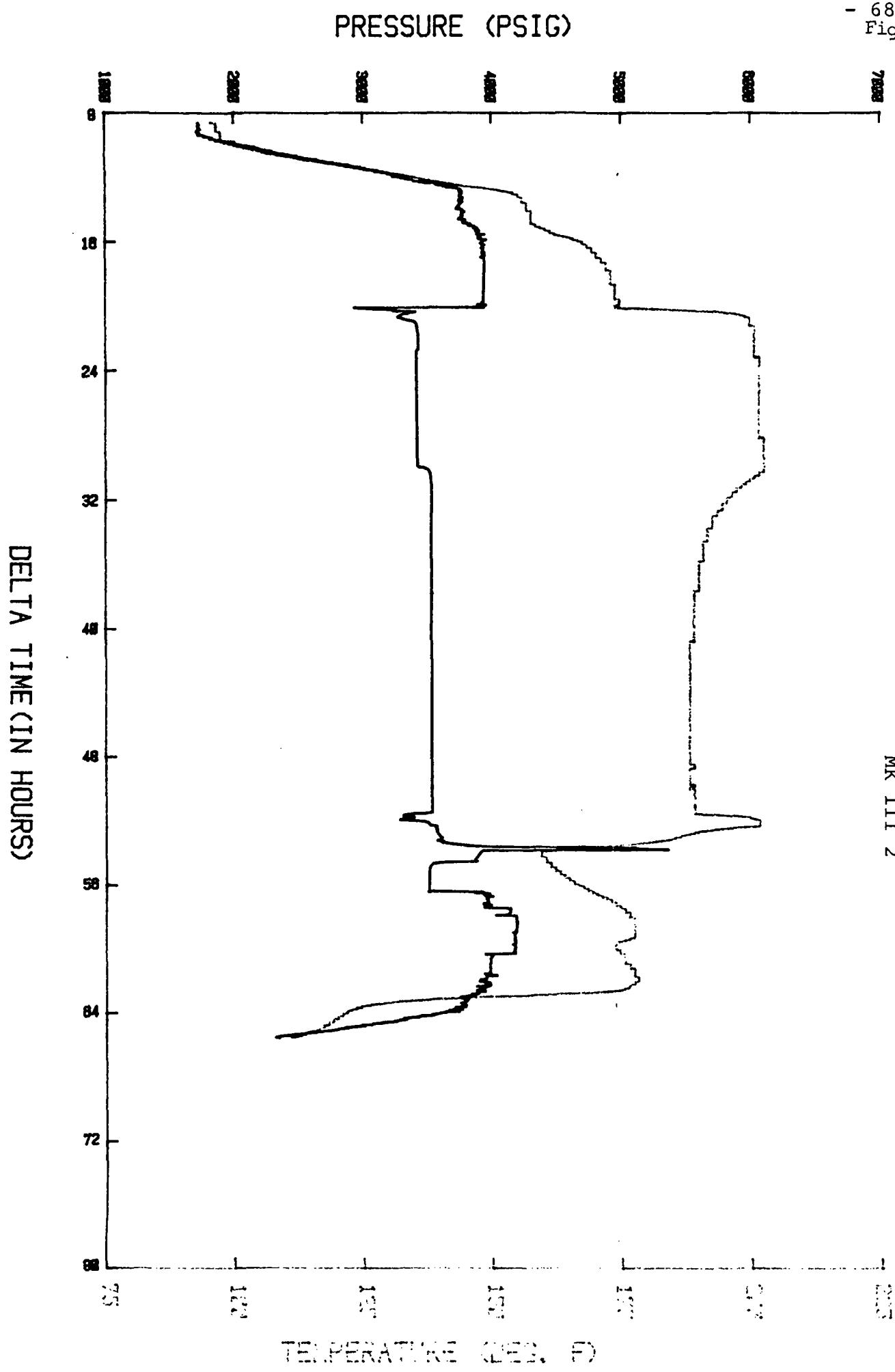
Table 1 Results from watersample taken at 0700 hours

Density at 20°C, g/cm <sup>3</sup>	1.0422
Conductivity at 20°C, m mho/cm	81.2
<u>Ion</u>	<u>Concentration ppm.</u>
$\text{Cl}^-$	35947

#### CONCLUSION

The water sample from 15/9-11 DST 2 contained no or a very low amount of mud filtrate and the water should therefore be representativ for the formation.

NL Sperry-Sun Inc. PRESS./TEMP. TIME PLOT  
MK III 2



BRONN 15-9-11  
BUILDUP NUMBER 1  
GAUGE SS MK III 2

NR.	TID	TRYKK
1	10.59	3501.700
2	11.01	3505.100
3	11.03	3509.000
4	11.05	3511.500
5	11.07	3513.200
6	11.09	3514.900
7	11.11	3516.400
8	11.13	3517.700
9	11.15	3518.100
10	11.17	3518.500
11	11.19	3519.400
12	11.21	3519.800
13	11.23	3520.200
14	11.25	3521.300
15	11.27	3521.700
16	11.29	3521.700
17	11.31	3521.700
18	11.33	3522.100
19	11.35	3522.800
20	11.37	3522.800
21	11.39	3523.200
22	11.41	3523.200
23	11.43	3523.200
24	11.45	3523.200
25	11.47	3523.200
26	11.49	3524.200
27	11.51	3524.200
28	11.53	3524.200
29	11.55	3524.200
30	11.57	3524.900
31	11.59	3524.900
32	12.01	3524.900
33	12.03	3524.900
34	12.05	3524.900
35	12.07	3524.400
36	12.09	3524.900
37	12.11	3525.500
38	12.13	3525.100
39	12.15	3525.500
40	12.17	3525.500
41	12.23	3525.100
42	12.27	3525.700
43	12.31	3525.700
44	12.35	3525.300
45	12.39	3525.700
46	12.43	3525.300
47	12.47	3525.900
48	12.51	3526.300
49	12.55	3525.900
50	12.59	3525.900
51	13.05	3525.900

Fig. 3.2.

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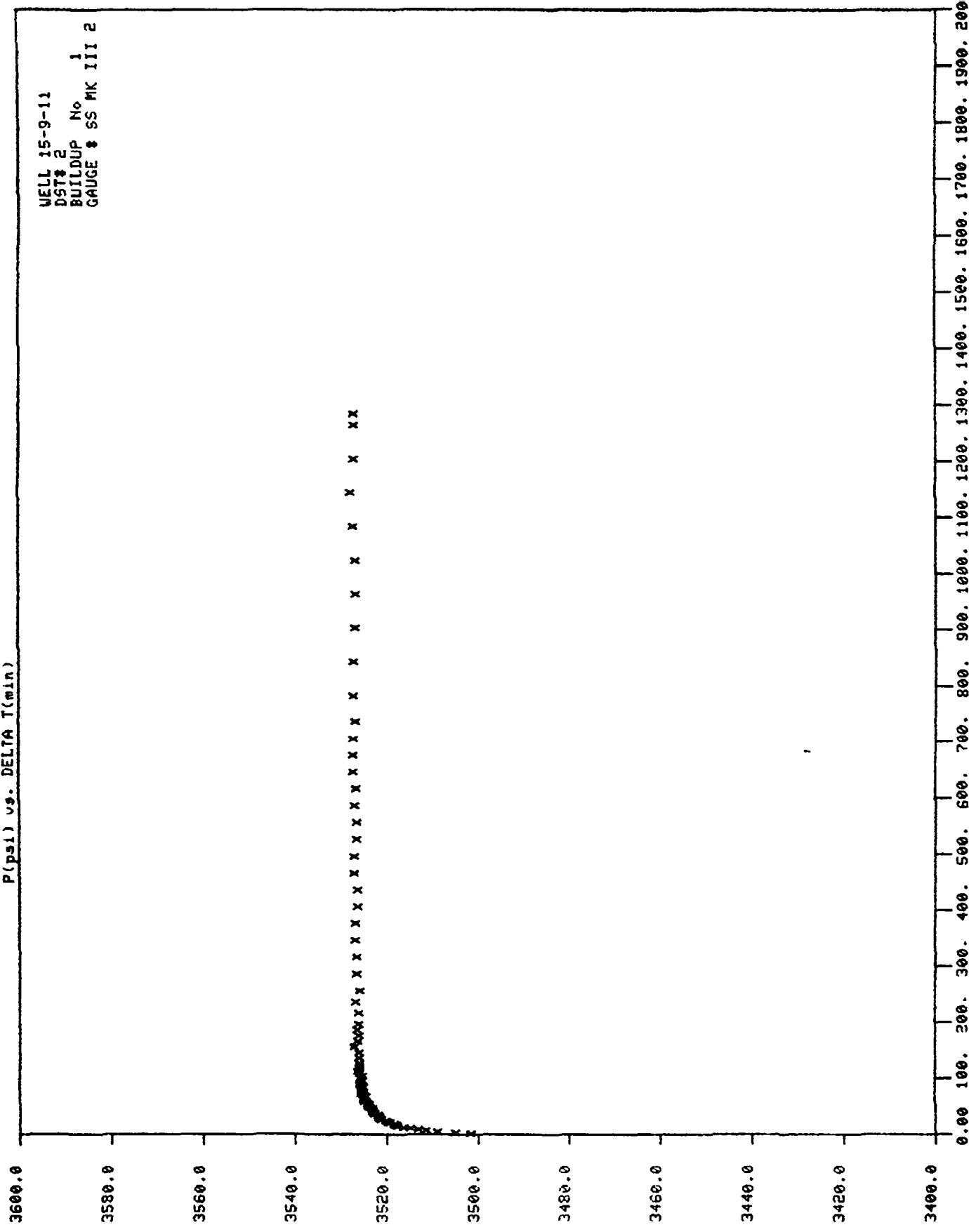


Fig. 3.3.

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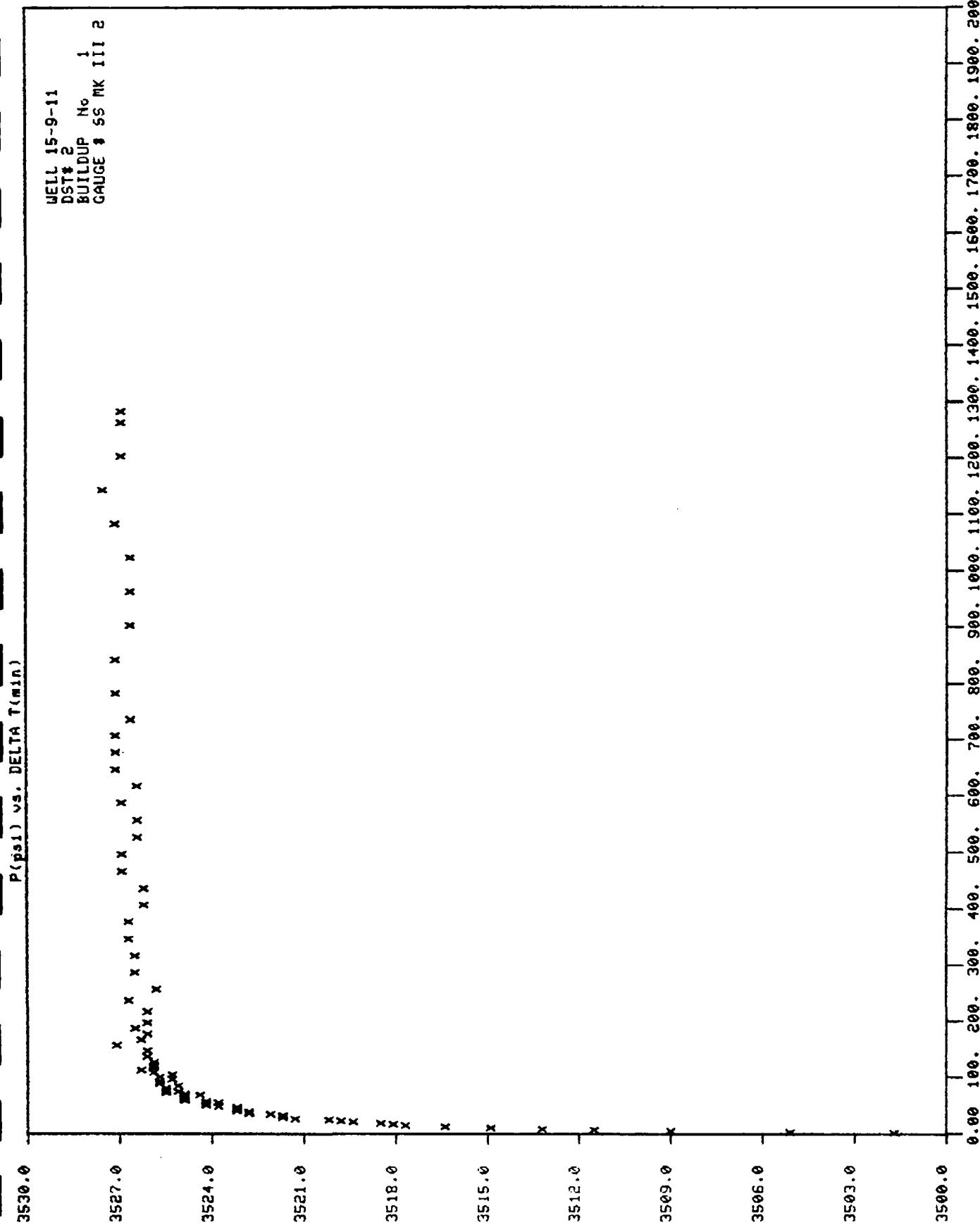


Fig. 3.4.

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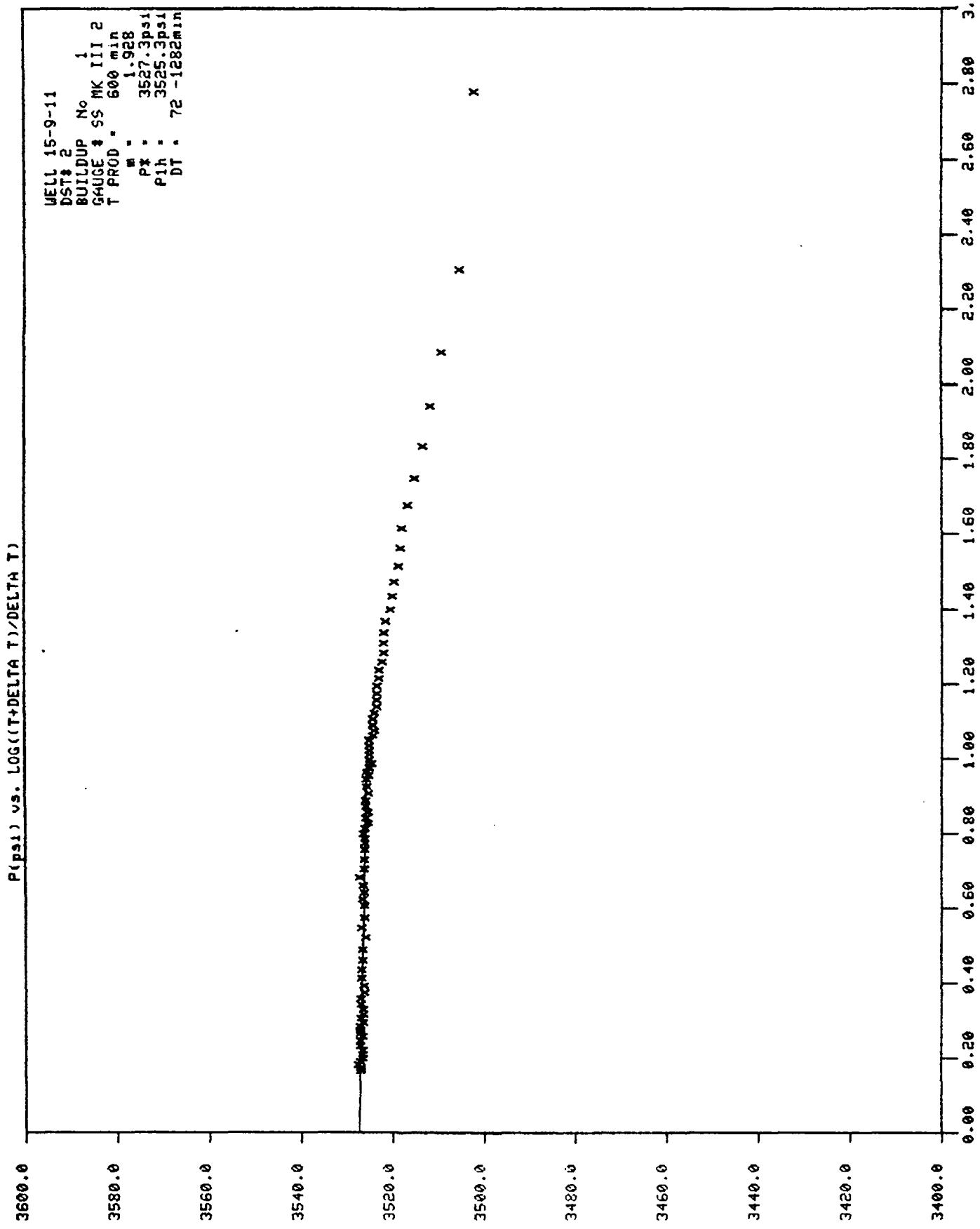


Fig. 3.5.

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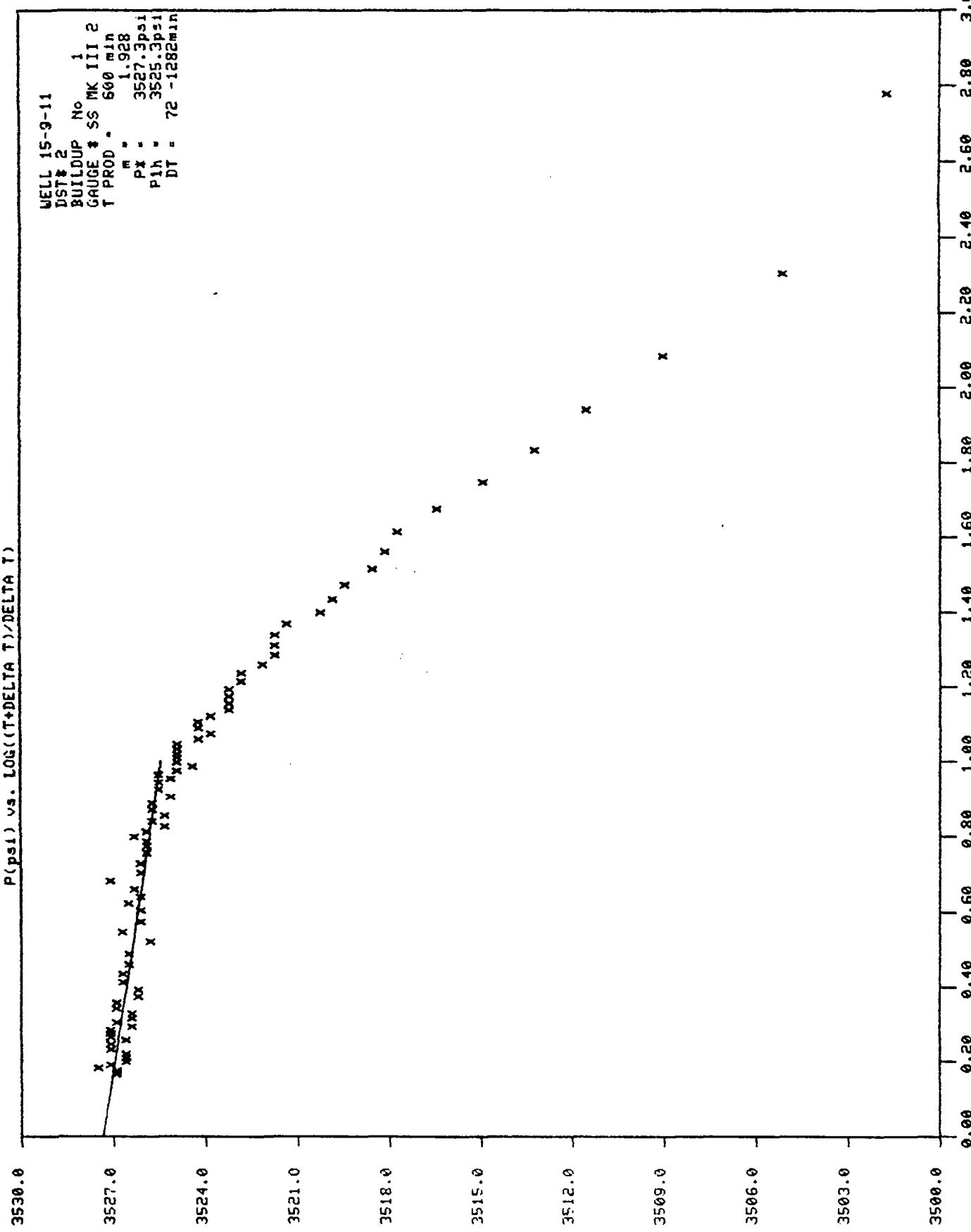
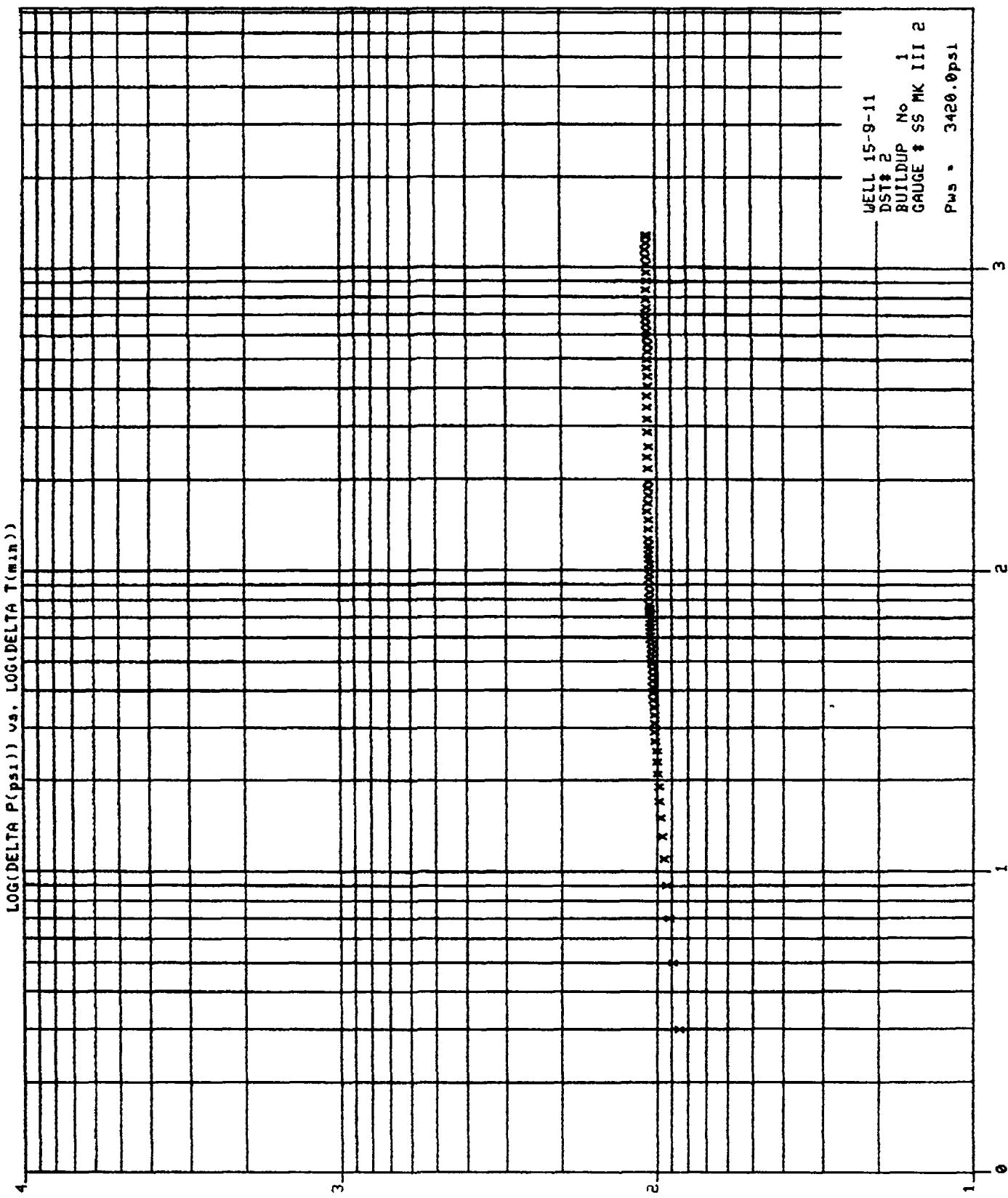


Fig. 3.6.

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APPENDIX 4

DST NO. 3

Content:

- Summary of DST no. 3.
- Lay out of test string
- Pressure recorders
- Diary of events
- Pressure, choke and flowdiagram
- Flow data
- Separator sampling
- Surface sampling
- Test analysis

Figures:

- Flopetrol P, T vs. time
  - First flow      - Listing of bottom hole pressure
  - $P_{ws}$  vs  $\Delta t$
  - $P_{ws}$  vs  $\log((t + \Delta t)/\Delta t)$
  - Log  $\Delta P$  vs  $\log \Delta t$
- Multirate  
flow      - Listing of bottom hole pressures
- $P$  vs.  $\Delta t$
- $P$  vs  $\sum_{j=1}^N \frac{q_i \log \left( \frac{t_n - t_{j-1} + \Delta t}{t_n - t_j + \Delta t} \right)}{q_n}$
- Log  $\Delta P$  vs.  $\log \Delta t$

SUMMARY OF DST NO. 3.

Perforated interval: 2395 - 2415 m RKB.

- First flow

9.5 mm (24/64") choke:	6 minutes
12.7 mm (32/64") choke:	28 minutes
19.1 mm (48/64") choke:	971 minutes

- First build-up: 960 minutes

- Multiple flow

9.5 mm (24/64") choke:	3 minutes
14.3 mm (36/64") choke:	231 minutes
22.2 mm (56/64") choke:	243 minutes
31.8 mm (80/64") choke:	236 minutes

- Multiple build-up: 534 minutes

Flowrates:

19.1 mm (48/64") choke: 569.8  $\text{MSm}^3/\text{D}$   
(20.16 MMSCF/D) of gas  
266  $\text{Sm}^3/\text{D}$   
(1671 STB/D) of condensate

14.3 mm (36/64") choke: 389.7  $\text{MSm}^3/\text{D}$   
(13.79 MMSCF/D) of gas  
187  $\text{Sm}^3/\text{D}$   
(1179 STB/D) of condensate

22.2 mm (56/64") choke: 714.2  $\text{MSm}^3/\text{D}$   
(25.27 MMSCF/D) of gas  
288  $\text{Sm}^3/\text{D}$   
(1811 STB/D) of condensate

31.8 mm (80/64") choke: 889.1  $\text{MSm}^3/\text{D}$   
(31.46  $\text{MMSCF/D}$ ) of gas  
435  $\text{Sm}^3/\text{D}$   
(2734 STB/D) of condensate

Gravities, first flow:

- Gas: 0.734 sp.gr
- Condensate: 0.75 sp.gr ( $57.2^\circ \text{ API}$ )

Separator conditions:

- Pressure: 36.54 bara (530 psia)
- Temperature:  $33.3^\circ \text{C}$  ( $92^\circ \text{F}$ )

Gauges:

- Two Flopetrol SSDR gauges, two Sperry Sun MK III gauges and one Sperry Sun MRPG gauge were run. All OK. The SSDR gauge no. 81049 was used for the test analysis.

TEST STRING TALLY      ROSS RIG      15/9-11      DST no. 3.

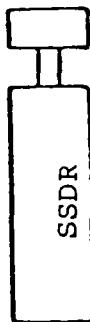
All measurements to top of each item

	EQUIPMENT DESCRIPTION	MIN	MAX	LENGTH	DEPTH
		ID ("")	OD ("")	(m)	(m)
1	Otis STT w/X-lver 5" vam				- 6.31
2	Jnts. 5" vam tbg. 18 lbs/ft L-80	4.25	5.56	20.02	13.71
1	Pupjnt. 5" vam tbg	4.25	5.56	4.53	18.24
1	X-over 5" VAM box x 4½" SA pin	4.25	5.51	0.40	18.64
1	Otis lubricator valve	2.99	13.88	1.62	20.26
1	X-over 4½" SA box x 5" VAM pin 0-23	4.25	5.51	0.41	20.67
1	Jnt. 5" VAM tbg	4.25	5.56	10.32	30.99
1	Jnt. 5" VAM tbg	4.25	5.56	9.65	40.64
2	Stds. 5" VAM tbg	4.25	5.56	59.86	100.50
1	Pupjnt. 5" VAM tbg	4.25	5.56	4.53	105.03
1	X-over 5" VAM box x 4½" SA pin F-24	3.00	6.00	0.29	105.32
1	Flopetroil EZ-tree	3.00	17.00	2.61	107.93
1	Slickjnt. 5" OD 4½" x 4 SA pin pin x	3.00	5.00	2.95	110.88
1	Flopetroil Fluted Hanger	3.00	16.00	0.29	111.17
1	X-over 4½"-4 SA pin x 5" VAM pin F-25	3.00	6.00	0.31	111.48
1	Pupjnt 5" VAM tbg	4.25	5.56	1.22	112.51
1	Jnt. 5" VAM tbg	4.25	5.56	9.81	122.51
1	Pupjnt. 5" VAM	4.25	5.56	3.00	125.51
67	STDS. 5" VAM tbg	4.25	5.56	1973.27	2098.7
1	X-over 5" VAM box x 3½" if pin	3.50	6.12	0.30	2099.08
1	Slipjnt. (open)	2.00	4.65	5.54	2104.62
1	Slipjnt. (closed)	2.00	4.63	4.01	2108.63
6	STDS drill collars	2.25	4.75	171.08	2279.71
1	X-over 3½" if box x 2 7/8" EUE pin	2.50	4.75	0.20	2279.91
1	RTTS mech. circ. valve	2.44	4.87	0.84	2280.73
2	X-over 2 7/8" EUE box x 3½" if pin	2.62	4.75	0.20	2280.95
2	STD drill collar	2.25	4.75	28.60	2309.55
1	Slipjnt (closed)	2.00	4.63	4.01	2313.56
1	Slipjnt (closed)	2.00	4.63	4.01	2317.57
1	STD drill collar	2.25	4.75	28.61	2346.18
1	APR-M safety/circ. valve	2.25	5.00	2.55	2348.73
1	DP-tester valve	2.25	5.00	1.46	2350.19
1	APR-N tester valve	2.25	5.00	3.86	2354.05

	EQUIPMENT DESCRIPTION	MIN	MAX	LENGTH	DEPTH
		ID ("")	OD ("")	(m)	(m)
1	Ful flo hydr. bypass	2.25	4.62	1.92	2355.97
1	Big John Jars	2.37	4.62	1.92	2357.89
1	X-over 3½" if box x 4½" if pin	3.00	6.12	0.40	2358.29
1	RTTS safety joint	3.12	6.12	1.08	2359.37
1	RTTS packer (above)	3.75	8.25	0.98	2360.35
	RTTS packer (below)	3.75	9.25	0.80	2361.15
1	X-over 4½" if x 3½" Fh	2.50	6.12	0.21	2361.36
1	X-over 3½" Fh x 2 7/8" EUE	2.40	4.75	0.20	2361.56
1	Perf. pupjnt 2 7/8" EUE	2.44	2.88	3.54	2365.10
1	X-over 2 7/8" EUE box x 2 3/8" EUE pin	2.00	3.70	0.26	2365.36
1	Collar 2 3/8" EUE	-	2.88	0.13	2365.49
1	OTIS XN-nipple 2 3/8" EUE pin x pin	1.79	2.38	0.22	2365.71
1	X-over 2 3/8" EUE box x 2 7/8" EUE pin	2.00	3.70	0.26	2365.97
1	Jnt. 2 7/8" EUE tbg	2.44	2.88	9.41	2375.38
1	Pupjnt. 2 7/8" EUE	2.44	2.88	2.40	2377.78
1	Flopetroil DST-hanger				
1	Jnt. 2 7/8" EUE tbg	2.44	2.88	8.93	2386.71
1	Perf. pupjnt. 2 7/8" EUE	2.44	2.88	2.05	2388.76
1	X-over 2 7/8" EUE box x 3 1/8" m pin	2.25	4.25	0.31	2389.07
1	Halliburton APBT carrier	-	3.00	1.51	2390.58
1	X-over 3 1/8" 8n box x 2 7/8" EUE pin	1.88	3.88	0.18	2390.76
1	Bull plug w/cross x 2 7/8" EUE box	-	4.00	0.21	2390.97

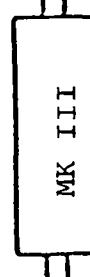
WELL NO.: 15/9-11 DST NO.: 3 DATE: 12.12.81.

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WIRELINE NIPPLE XN-nipple 2365.7 m

GAUGE TYPE AND NUMBER: SSDR no. 81049  
DEPTH, PRESSURE ELEMENT: 2370.9m RANGE: 0 - 10000 psi  
MODE: 1 min. sampling DELAY: No  
ACTUATED: time 0503 date: 12.12.81.  
WILL RUN OUT: time 1803 date: 15.12.81.



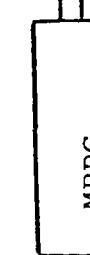
GAUGE TYPE AND NUMBER: MK III no. 3-10-1576  
DEPTH, PRESSURE ELEMENT: 2373.95m RANGE: 0 - 10000 psi  
MODE: 2 min. DELAY: 8 hrs.  
ACTUATED: time: 0452 date: 12.12.81  
WILL RUN OUT: time: 2204 date: 14.12.81.



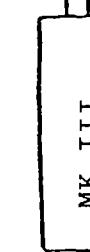
GAUGE TYPE AND NUMBER: \_\_\_\_\_  
DEPTH, PRESSURE ELEMENT: \_\_\_\_\_ RANGE: \_\_\_\_\_  
MODE: \_\_\_\_\_ DELAY: \_\_\_\_\_  
ACTUATED: time: \_\_\_\_\_ date: \_\_\_\_\_  
WILL RUN OUT: time: \_\_\_\_\_ date: \_\_\_\_\_



D.S.T. HANGER 2377.7 m  
GAUGE TYPE AND NUMBER: SSDR no. 81048  
DEPTH, PRESSURE ELEMENT: 2382.5m RANGE: 0 - 10000 psi  
MODE: 2 min. sampling DELAY: -  
ACTUATED: time: 0430 date: 12.12.81.  
WILL RUN OUT: time: 0400 date: 17.12.81.



GAUGE TYPE AND NUMBER: MRPG no. 41  
DEPTH, PRESSURE ELEMENT: 2386.2 m RANGE: 0 - 6000 psi  
MODE: 4 min DELAY: 8 hrs.  
ACTUATED: time: 0431 date: 12.12.81.  
WILL RUN OUT: time: 0623 date: 17.12.81.



GAUGE TYPE AND NUMBER: MK III no. 1-9.1751  
DEPTH, PRESSURE ELEMENT: 2388.6 m RANGE: 0 - 1000 psi  
MODE: 4 min DELAY: 8 hrs.  
ACTUATED: time: 0433 date: 12.12.81.  
WILL RUN OUT: time: 0625 date: 17.12.81.

DIARY OF EVENTS

---

WELL NO.: 15/9-11 DST NO.: 3  
ZONE TESTED: Heimdal PERFS.: 2395 - 2415

---

DATE/TIME OPERATIONS

---

11.12.81.

23.45 PERFORATING  
Start rig up Schlumberger

12.12.81.

00.35 RIH gun no. 1.  
01.25 Gun fired. Interval: 2415.0 - 2405.0 m  
02.00 POOH. All shots fired  
02.40 RIH gun no. 2.  
03.25 Gun fired. Interval: 2405.0 - 2395.0 m  
04.10 POOH. All shots fired. Rigged down Schlumberger  
RIH W/TEST STRING  
04.30 Start RIH w/test string  
04.40 Installed 1 SSDR, 1 MRPG and 2 MARK III in DST  
hanger  
05.20 Installed 1 SSDR, 1 MRK III in XN-nipple

13.12.81.

09.02 Set packer. Discovered 13 bbl drop in riser  
level. Opened mastervalve. WHP increased from 11  
- 780 psia. RTTS circulating valve open.  
10.40 Recycled RTTS circ. valve. Checked for pressure  
communication to annulus. Valve closed.  
11.15 Opened RTTS circ. valve, reversed mud into  
tubing. Displaced mud back with 61 bbl water and  
60 bbl diesel and 2 bbls of gel mud.  
FIRST FLOW  
15.24 Opened APR-N valve. WHP = 370 psia  
15.26 Opened choke manifold on 24/64" adjustable choke  
15.28 WHP = 215 psia  
15.30 Opened up to 32/64" adjustable choke  
15.32 WHP = 70 psia

COMMENTS: WHP reached a minimum of 36 psia

DIARY OF EVENTS

---

WELL NO.: 15/9-11 DST NO.: 3  
ZONE TESTED: Heimdal PERFS.: 2395 - 2415

---

DATE/TIME OPERATIONS

---

13.12.81.

15.40 WHP = 340 psia  
15.50 Started injecting methanol. WHP = 895 psia  
15.56 Gas to surface. WHP = 1420 psia  
15.58 Opened to 48/64" adjustable choke.  
Mud to surface.  
16.32 WHP = 1876 psia, BS&W: 8% mud, traces of water  
and sand  
18.00 WHP = 1917 psia  
20.00 WHP = 1957 psia, 5 - 6 % mud/water, 0.5% sand  
20.40 Directed flow through heater  
21.00 Directed flow through separator. Found relief  
valve leaking at 200 psi. Bypassed separator -  
repaired leak.  
22.06 Directed flow through separator  
22.40 WHP = 2000 psia, WHP = 108°F  
23.22 flow to stock tank to measure meter factor,  
f = 0.905  
23.47 Bypassed tank

14.12.81.

03.05 Started taking first set of PVT samples  
04.00 Finished first set of PVT samples  
06.10 Started taking second set of PVT samples  
07.25 Finished second set of PVT samples  
08.03 Bypassed separator. WHP = 1997 psia  
08.05 Attempted to close APR-N. Negative.  
WHP = 1997 psia  
FIRST BUILD-UP  
08.07 Closed choke manifold. Both Lynes probes plugged.  
22.42 Closed fail safe valve. Rep. leak in needle  
valve for Lynes probe.

COMMENTS: All WHP from Lynes

DIARY OF EVENTS

---

WELL NO.: 15/9-11

DST NO.: 3

ZONE TESTED: Heimdal

PERFS.: 2395 - 2415

---

DATE/TIME      OPERATIONS

---

15.12.81.

- 00.03      Opened fail safe valve. WHP = 2489 psia  
SECOND FLOW  
00.05      Opened APR-N. WHP = 2489 psia  
00.08      Opened on 24/64" adj. choke. Started injecting glycol  
00.10      36/64" adj. choke  
00.51      WHP = 2120, Went through heater  
00.53      37&64" pos. choke  
01.00      WHP = 2361 psi, indicating washed out adj. choke  
01.15      Went through separator  
01.20      WHP = 2364 psia. Downstream choke pressure = 850 psia. WHT = 80°F  
04.00      WHP = 2382 psia. WHT = 96°F  
04.01      Bypassed separator. Incr. to 56/64" adj. choke  
04.09      56/64" pos. choke  
04.30      WHP = 1887 psi. Went through separator  
08.00      WHP = 1914 psi. Downstream choke pressure = 1110 psi, WHP = 116°F  
08.01      Bypassed separator  
08.02      Bypassed heater  
08.04      56/64" adj. choke. Slowly incr. to 80/65" adj. choke  
08.07      80/64" pos. choke  
08.27      WHP = 1455 psi  
08.34      Went through separator  
09.00      WHP = 1465 psi. Downstream choke pressure = 1130 psi, WHT = 116°F

COMMENTS: All WHP from Lynes

DIARY OF EVENTS

---

WELL NO.: 15/9-11

DST NO.: 3

ZONE TESTED: Heimdal

PERFS.: 2395 - 2415

---

DATE/TIME            OPERATIONS

---

15.12.81.

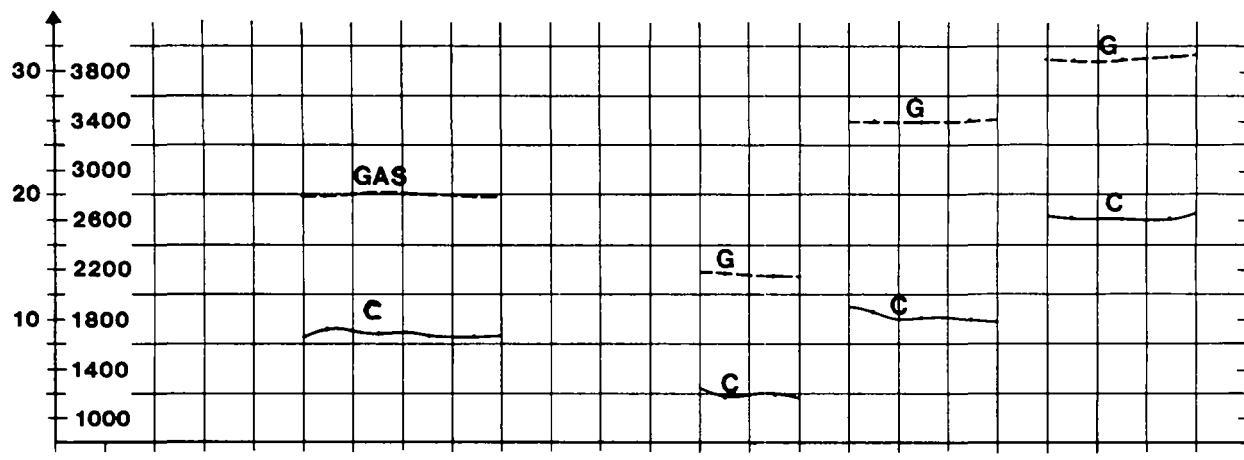
- 10.00        Started PVT sampling  
              Finished PVT sampling  
12.00        WHP = 1482 psi. Downstream choke pressure = 1135  
              psi, WHT = 118°F  
12.00        Bypassed separator  
              FINAL BUILD-UP  
12.01        Closed choke manifold  
12.02        Bleed off ann. pres. to close APR-N when WHP =  
              2200 psi  
              KILLING WELL  
20.54        Started bullheading

COMMENTS: All WHP from Lynes

WELL NO : 15-9-11 DST NO.: 3

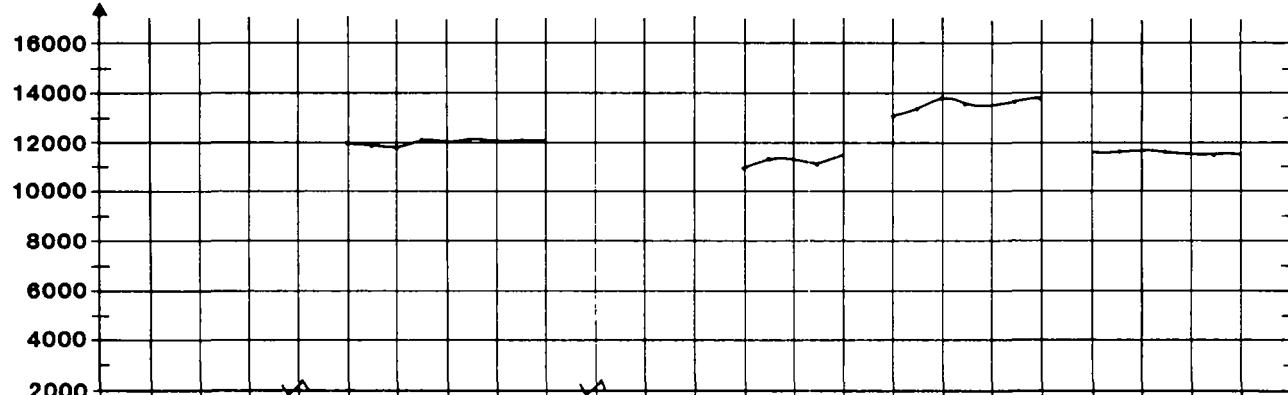
## PRESSURE CHOKE AND FLOWDIAGRAM

GAS RATE (MMSCF/D) OIL/COND. RATE (STB/D)

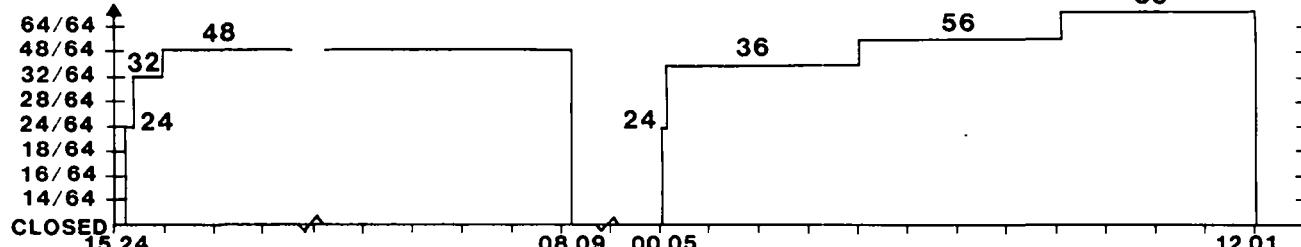


— OIL/COND. RATE  
--- GAS RATE

GOR (SCF/STB)

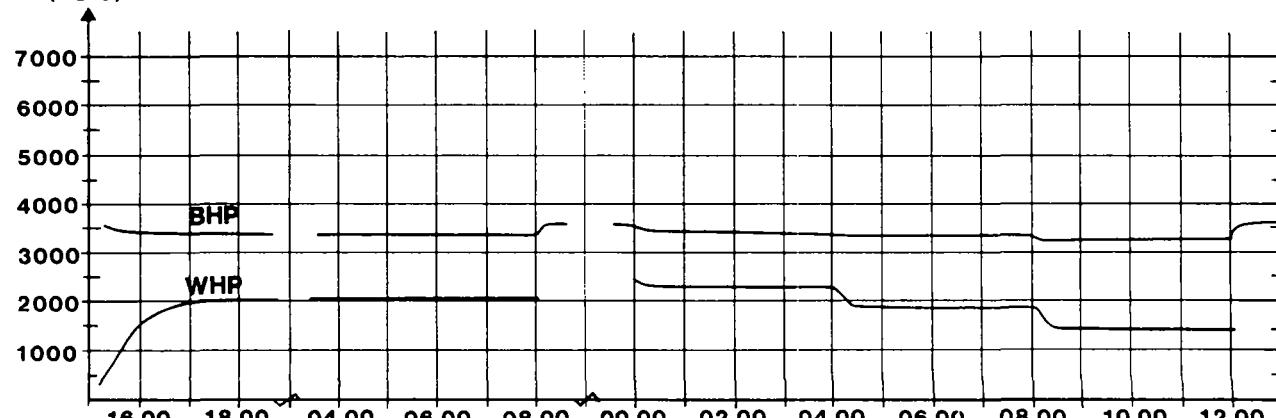


CHOKE SIZES (INCHES)



— HEATER  
— CHOKE MANIFOLD  
80

PRESSURE (PSIG)



TIME (HOURS) →  
13-12 →      14-12 →      15-12 →

**FLOW DATA**

**SSDR LINES**

Date/Time	SSDR LINES				Separator data						W=water M=mud			Liq. and gas analysis at goos neck				
	Bottom hole Press. Psi a	Temp. F	Well head Press. Psi a	Temp. F	Chokes	Heater Manifold 64. inc.	Press. Psig	Temp. F	Gas rat. mmscf/d	Oil rate stb/d	GOR scf/stb	Oil API	Gas S.G.	Water %	pH	Sedim. %	Oil API	CO2
13.12.81.																		
1524	3551	173	370	56														
1526	3505	"	325	"	24/64													
1530	3458	"	160	55	32/64													
1532	3463	"	70	"	"													
1550	3409	175	895	66	"													
1556	3401	177	1420	80	"													
1558	3387	"	1470	84	48/64													
2040	3425	195	"	"	"													
2206	3428	"	"	"	"													
2230	3430	196	1975	108	"													
2300	3429	"	1992	"	"													
2330	3430	"	"	1995	"													
2400	"	197	"	1997	"													
14.12.81.																		
0030	3431	"	"	109	"													
0100	"	"	"	"	"													
0130	3432	"	"	110	"													
0200	"	"	"	2000	"													
0230	"	"	"	2004	109	"												
0300	3433	"	"	2005	110	"												
0330	"	"	"	198	2004	"												
0400	"	"	"	"	"													
0430	3434	"	"	2000	"													
0500	"	"	"	"	109	"												
0530	"	"	"	"	"													
0600	"	"	"	2002	"													
0630	3435	"	"	2004	"													
0700	"	"	"	2005	"													

Trace 0 -  
0.1 0 -  
0.1 0 -

87 -  
0.1 0 -  
0.1 0 -

SSDR LINES

FLOW DATA

Date/Time	Bottom hole		Well head		Chokes		Separator data						Liq. and gas analysis at goos neck						
	Press. Psi.	Temp. F	Press. Psi	Temp. F	Manifold 64. inc.	Heater 64. inc.	Press. Psi/g	Temp. F	Gas rat. mmscf/d	Oil rate stb/d	GOR scf/stb	Oil API	Gas S.G.	Water %	pH	Sedim. %	Oil API	Co2	H2S
14.12.81.																			
0730	3435	198	2007	109	48/64		495	89	19.806	1642	12065	57.2	734	1.5mw	Trace	0.1	0		
"	"	199	"	"	"		"	"	20.158	1671	12064	"	"	2.8mw	"				
0803	3435	199																	
0807	"	"	1997	"															
0809	3483	"																	
15.12.81.																			
0005	3521	186	2473		24/64														
0008	3486	"																	
0010	3470	"	36/64																
0053	3442	196																	
0115	3472	198	2352	88															
0130	"	199	"	90	"		465	67	13.730	-	-	-	-	0.35w	Trace				
0200	3473	"	2351	94	"		"	68	13.766	1236	11141	"	734	1.3w	"				
0230	"	"	2355	91	"		460	72	13.770	1190	11575	56.5	"	1.5mw	0				
0300	"	"	2366	"	"		"	"	13.717	1192	11509	"	"	0.6w	7	Trace	"		
0330	"	"	"	92	"		"	73	13.699	1203	11388	"	"	2.0mw					
0400	"	"	2371	95	"		"	74	13.786	1179	11691	"	"						
0401	"	"																	
0402	3462	"																	
0405	3419	"	56/64																
0410	3393	"																	
0430	3411	"	1875	106															
0500	3412	"		"	112														
0530	3413	"	1886	114	"		"	93	24.981	1871	13352	-	-	1.5w	"	"	"		
0600	3414	"	1887	"			"	94	25.043	1789	13998	58	734	1.0w	7	"			
0630	3415	"	1889	115	"		"	97	25.037	1845	13567	"	"	1.3mw	"	0	"		
0700	3416	"	1893	116	"		"	"	25.124	1849	13591	"	"	0.6mw	0	"	"		
0730	"	"	1900	117	"		"	"	"	1838	13670	"	"	0.6mw	Trace	"	"		
0800	3417	"	"	118	"		"	98	25.266	1811	13949	"	"						

## FLOW DATA

SIXTY EIGHT

DST SUMMARY DATA

Well no. 15/9-11 DST no. 3 Date: 14-15/12-81

1. Separator samples

Bottle no.	Oil/gas	Time	Oil rate	Gas rate	
14.12.81					
9214/328	Oil	03:10	1598 BOPD	20.684	MMSCFD
A12060	Gas	03:13	" "	"	"
A12056	"	03:40	" "	"	"
A10229	"	06:10	1602 "	19.983	"
13266/99	Oil	"	" "	"	"
1911339	Gas	07:00	1610 "	"	"
15.12.81					
9214/371	Oil	09:57	2360 BOPD	31.212	MMSCFD
A7327	Gas	10:00	" "	"	"
A10033	"	10:35	2374 "	"	"

2. Bottom hole samples

None

OTHER SAMPLING

<u>TYPE</u>	<u>SAMPLING POINT</u>
1 Drum of condensate	Separator
6 x 1 liter bottles cond.	Goosneck
1 x 20 l. jerry can, cond.	Separator
Sample of mud filtrate	Mud pit
Sample of water	Separator

## TEST ANALYSIS

Input data, reservoir parameters:

Reservoir pressure, P : 242.83 bara (3522 psia)  
 Reservoir temperature, T : 85.6°C (186°F)  
 Specific gravity of reservoir gas,  $\gamma_g$ : 0.937  
 Compressibility factor, Z : 0.828  
 Viscosity of reservoir gas,  $\mu_g$  : 0.029 cp  
 Gas formation volume factor,  $B_g$  :  $4.29 \times 10^{-3} \text{ m}^3/\text{m}^3$   
                           :  $(7.64 \times 10^{-4} \text{ RB/SCF})$   
 Compressibility of reservoir gas,  $C_g$  :  $272 \times 10^{-5} \text{ bar}$   
                            $(18.75 \times 10^{-5} \text{ psi}^{-1})$   
 Comp. of formation water,  $C_w$  :  $37.7 \times 10^{-6} \text{ bar}^{-1}$   
                            $(2.6 \times 10^{-6} \text{ psi}^{-1})$   
 Compressibility of the formation,  $C_f$  :  $52.9 \times 10^{-6} \text{ bar}^{-1}$   
                            $(3.65 \times 10^{-6} \text{ psi}^{-1})$   
 Water saturation,  $S_w$  : 0.23  
 Hydrocarbon saturation,  $S_g$  : 0.77  
 Porosity,  $\phi$  : 0.20  
 Perforation height,  $h_p$  : 20 m (65.6 ft)  
 Formation height,  $h_t$  : 38 m (124.7 ft)  
 Wellbore radius,  $r_w$  : 0.155 m (0.51 ft)  
 Total compressibility,  $C_t$  :  $21.5 \times 10^{-4} \text{ bar}^{-1}$   
                            $(1.48 \times 10^{-4} \text{ psi}^{-1})$

First flow period, 19.1 mm (48/64") choke:

- Vapour volume equivalent:  
 $V_{CS} = 192 \text{ m}^3/\text{m}^3$  (1080 SCF/STB) at  
 0.75 sp.gr. (57.0°API) and 35.16 bara  
 (510 psia) on separator

- Flow rate  
 $Q_g = 20.16 \times 10^6 \text{ SCF/D} + 1080 \text{ SCF/STB} \times 1671 \text{ STB/D}$   
 $= 21.96 \text{ MMSCF/D} (620.6 \text{ MSm}^3/\text{D})$

- $t_{eff} = t_{prod} = 1005 \text{ minutes}$

Horner analysis, first build-up:

The Flopetrol SSDR no. 81049 is used for the analysis.

Results:

$$\begin{aligned} P^* &= 242.85 \text{ bara (3522.2 psia)} \\ P_{1\text{hr}} &= 242.72 \text{ bara (3520.3 psia)} \\ m &= 0.1055 \text{ bar/cycle (1.530 psi/cycle)} \\ P_{wfs} &= 236.83 \text{ bara (3435.0 psia)} \end{aligned}$$

Permeability thickness:

$$kh = \frac{162.6 Qg Bg ug}{m} = 15762 \text{ md m} = 51714 \text{ md ft}$$

The thickness of the zone which is contributing flow to the wellbore is assumed to be the formation height.

Permeability:

$$h = h_t = 38 \text{ m (124.7 ft)} \Rightarrow k = 415 \text{ md}$$

Total skin factor :  $S_t = 57.2$

Partial penetration skin factor :  $SP = 3.6$

Pressure drop due to skin:  $4 P_s = 5.25 \text{ bar (76 psi)}$

Real productivity index:

$$PI = \frac{Qg}{P^* - P_{wfs}} = 103400 \text{ Sm}^3/\text{D/bar (251900 SCF/D/psi)}$$

Ideal productivity index:

$$PI = \frac{Qg}{P^* - P_{wfs} - P_s} = 827500 \text{ Sm}^3/\text{D/bar (1.96 MMSCF/D/psi)}$$

Input data, multirate flow

Vapour volume equivalents:

$VCS_1 = 1050 \text{ SCF/STB at } 56.5^\circ\text{API, } 475 \text{ psia on separator}$

$VCS_2 = 1100 \text{ SCF/STB at } 58.0^\circ\text{API, } 545 \text{ psia on separator}$

$VCS_3 = 1150 \text{ SCF/STB at } 60.5^\circ\text{API, } 570 \text{ psia on separator}$

Flow rates on:

36/64" choke:

$$Qg_1 = 13.79 \times 10^6 \text{ SCF/D} + 1179 \text{ STB/D} \times 1050 \text{ SCF/STB} = \\ 15.03 \times 10^6 \text{ SCF/D} (424800 \text{ Sm}^3/\text{D})$$

$$t_1 = 231 \text{ minutes}$$

56/65" choke:

$$Qg_2 = 25.27 \times 10^6 \text{ SCF/D} + 1811 \text{ STB/D} \times 1100 \text{ SCF/STB} = \\ 27.26 \times 10^6 \text{ SCF/D} (770400 \text{ Sm}^3/\text{D})$$

$$t_2 = 243 \text{ minutes}$$

80/64" choke:

$$Qg_3 = 31.46 \times 10^6 \text{ SCF/D} + 2734 \text{ STB/D} \times 1150 \text{ SCF/STB} = \\ 34.60 \times 10^6 \text{ SCF/D} (977900 \text{ Sm}^3/\text{D})$$

$$t_3 = 236 \text{ minutes}$$

$$t_{\text{eff}} = Qg_1 \times t_1 + Qg_2 \times t_2 + Qg_3 \times t_3 = 529 \text{ minutes}$$

$$\underline{Q_3}$$

Multirate build-up analysis

Results:

$$\begin{aligned} P^* &= 242.88 \text{ bara (3522.7 psia)} \\ P_{1\text{hr}} &= 242.63 \text{ bara (3519.1 psia)} \\ m &= 0.1610 \text{ bar/cycle (2.335 psi/cycle)} \\ P_{wfs} &= 234.05 \text{ bara (3394.6 psia)} \end{aligned}$$

Permeability thickness:

$$kh = \frac{162.6 Qg_3 \times B_g \times u_g}{m} = 16270 \text{ md m (53382 md/ft)}$$

$h = 38 \text{ m}$ , formation height:

Permeability  $K = 428 \text{ md}$

Total skin factor  $= S_t = 54.2$

Pressure drop due to skin:  $\Delta P_s = 7.07 \text{ bar (102.5 psi)}$

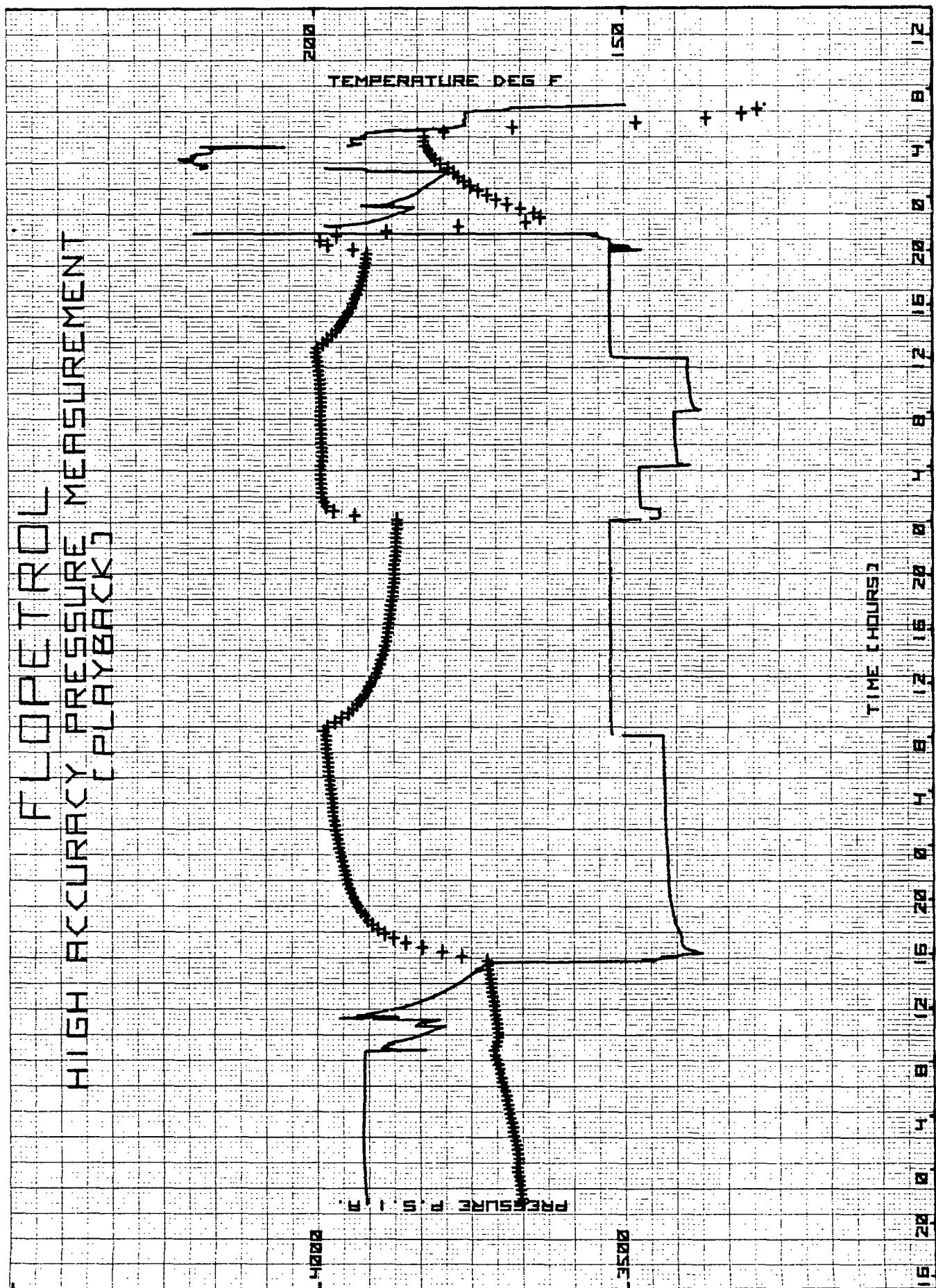
Real productivity index:

$$PI = \frac{Qg_3}{P^* - P_{wfs}} = 111303 \text{ Sm}^3/\text{D/bar (270948 SCF/D/psi)}$$

Ideal productivity index:

$$PI = \frac{Qg_3}{P^* - P_{wfs} - \Delta P_s} = 564025 \text{ Sm}^3/\text{D/bar (1.37 MMSCF/D/psi)}$$

Fig. 4.1.



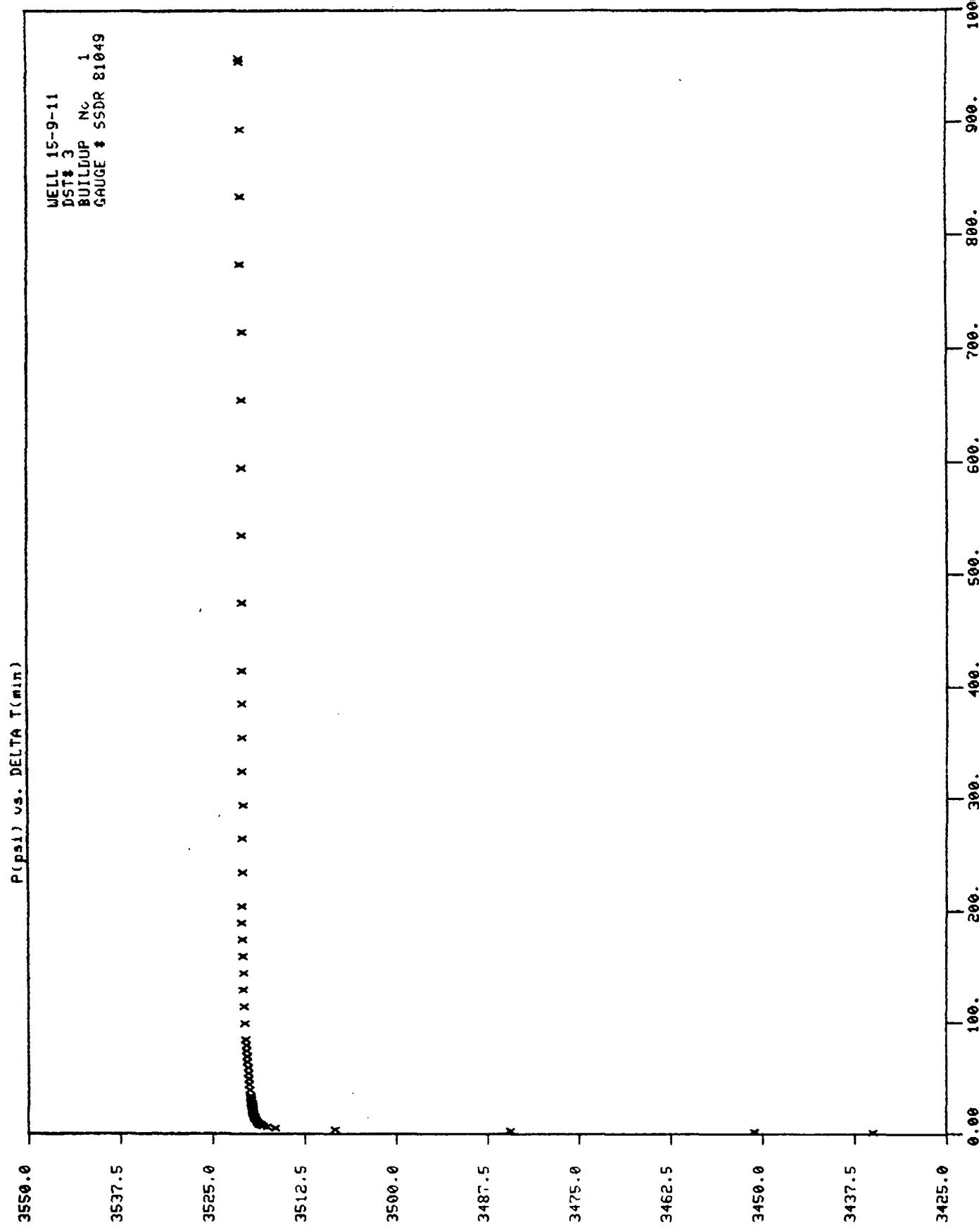
## FIRST BUILD-UP

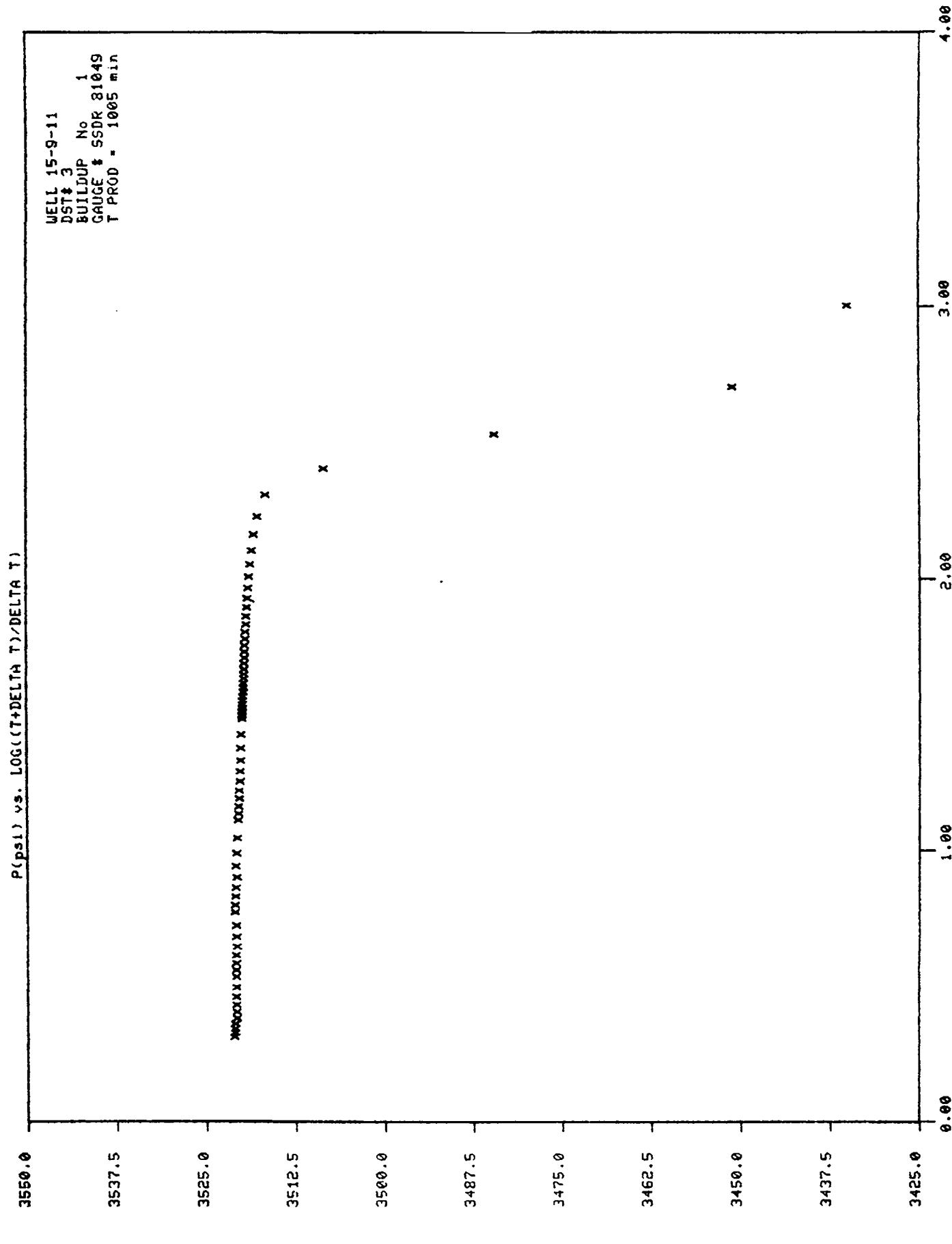
BRÖNN 15-9-11 DST# 3  
 BUILDUP NUMMER 1  
 GAUGE SSDR 81049

NR.	TID	TRYKK			
1	8.07	3435.000	46	10.00	3520.700
2	8.08	3451.100	47	10.15	3520.200
3	8.09	3484.400	48	10.30	3520.700
4	8.10	3508.400	49	10.45	3520.800
5	8.11	3516.500	50	11.00	3520.900
6	8.12	3517.700	51	11.15	3521.000
7	8.13	3518.200	52	11.30	3521.000
8	8.14	3518.500	53	12.00	3520.800
9	8.15	3518.700	54	12.30	3520.800
10	8.16	3518.900	55	13.00	3520.700
11	8.17	3519.000	56	13.30	3520.800
12	8.18	3519.100	57	14.00	3520.800
13	8.19	3519.200	58	14.30	3520.800
14	8.20	3519.300	59	15.00	3520.800
15	8.21	3519.300	60	16.00	3520.800
16	8.22	3519.400	61	17.00	3520.800
17	8.23	3519.400	62	18.00	3520.800
18	8.24	3519.500	63	19.00	3520.800
19	8.25	3519.500	64	20.00	3520.700
20	8.26	3519.500	65	21.00	3521.000
21	8.27	3519.600	66	22.00	3521.000
22	8.28	3519.600	67	23.00	3521.000
23	8.29	3519.600	68	0.00	3521.100
24	8.30	3519.600	69	0.03	3521.100
25	8.31	3519.700		GI TYPE EDITERING	
26	8.32	3519.700	0	= SLUTT	
27	8.33	3519.700	1	= LISTING	
28	8.34	3519.800	2	= SLETTING	
29	8.35	3519.800	3	= ADDERING	
30	8.36	3519.800	4	= ERSTATTING	
31	8.37	3519.800			
32	8.38	3519.800			
33	8.39	3519.900			
34	8.40	3519.900			
35	8.45	3520.000			
36	8.50	3520.100			
37	8.55	3520.100			
38	9.00	3520.200			
39	9.05	3520.200			
40	9.10	3520.300			
41	9.15	3520.300			
42	9.20	3520.400			
43	9.25	3520.400			
44	9.30	3520.500			
45	9.45	3520.600			

Fig. 4.2.

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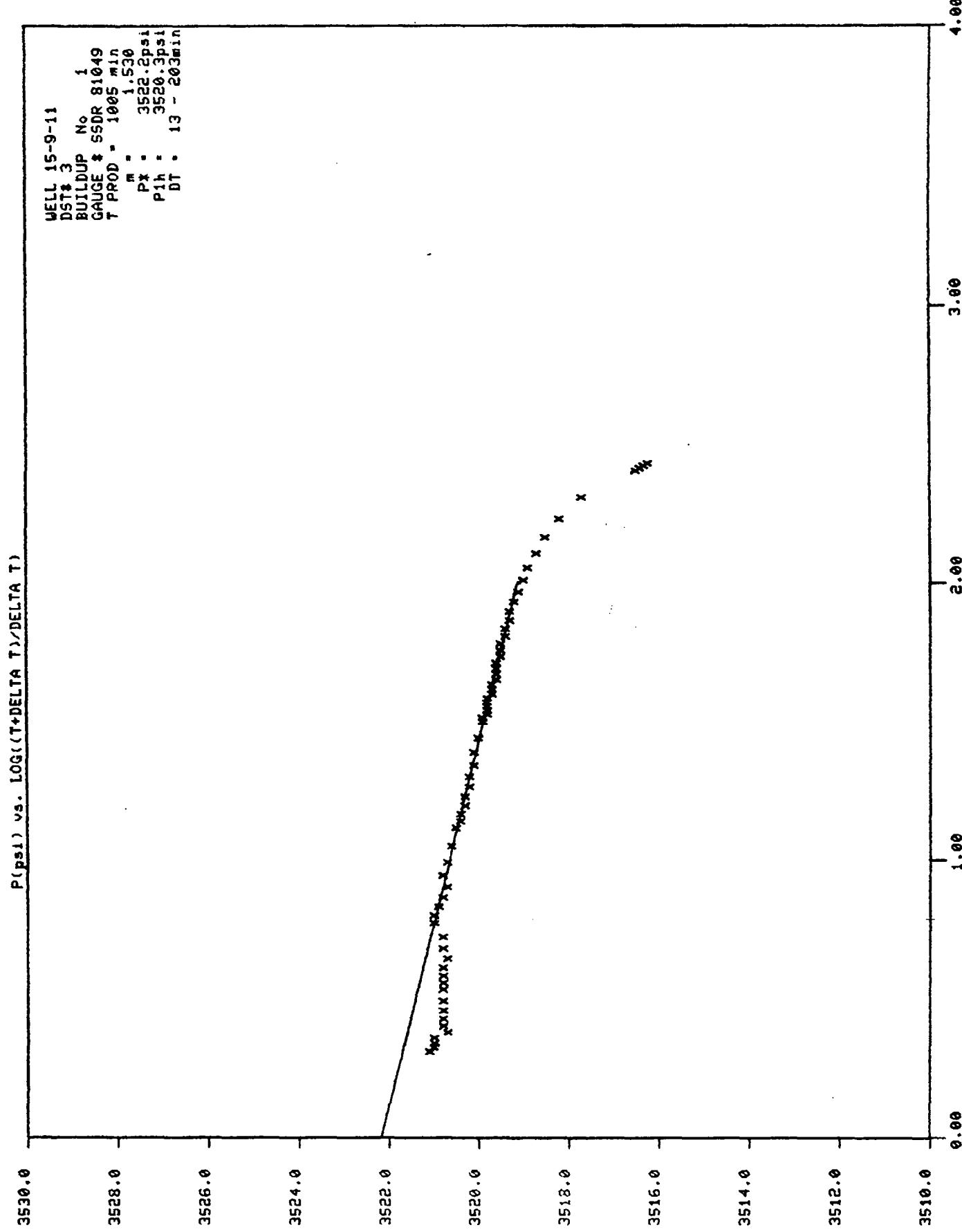
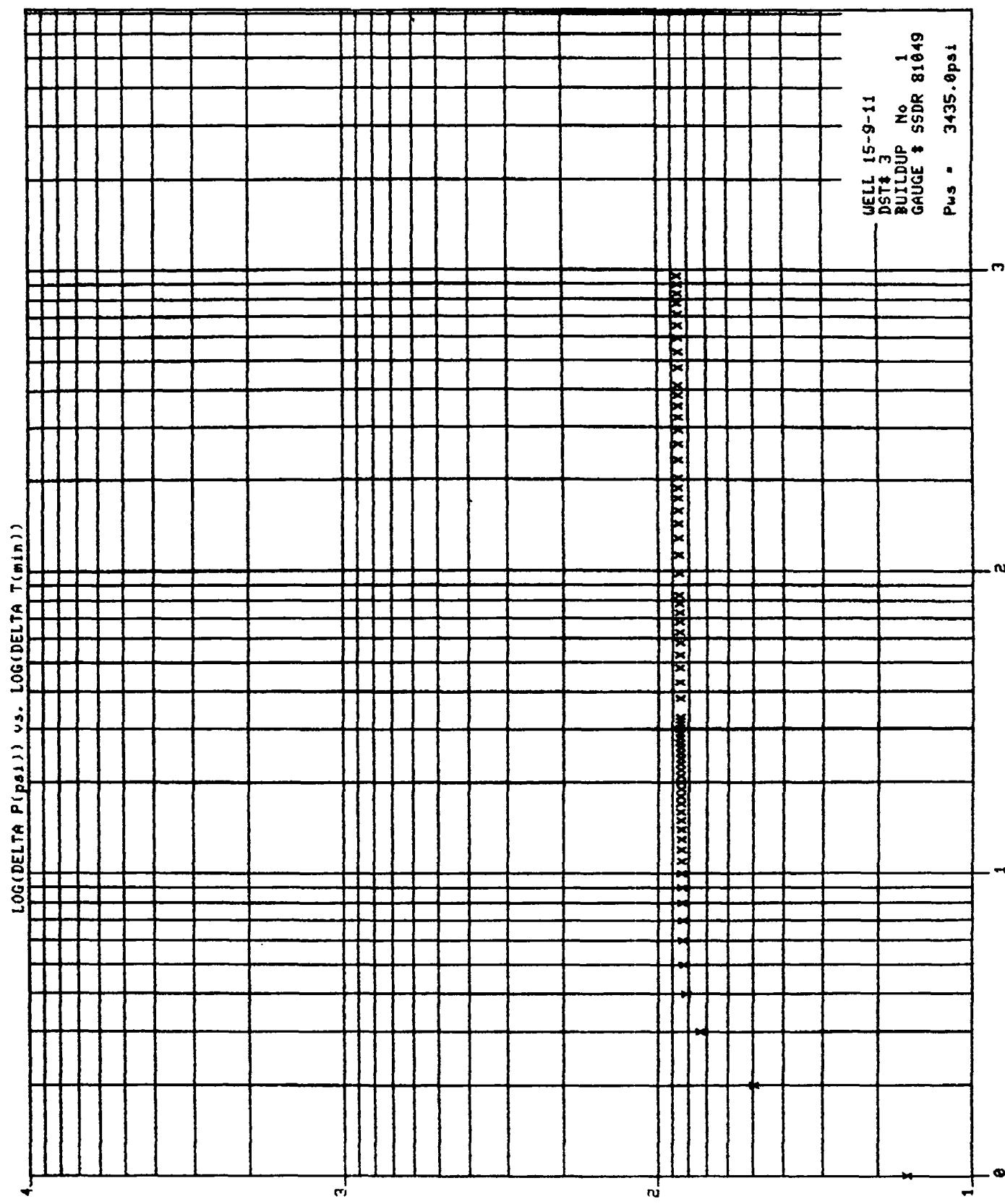


Fig. 4.5.

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## MULTIRATE BUILD-UP

BRÖNN 15-9-11 DST# 3  
 BUILDUP NUMMER 2  
 GAUGE SSDR 81049

NR.	TID	TRYCK			
1	1.00	3426.700	56	184.00	3520.040
2	2.00	3469.890	53	194.00	3520.020
3	3.00	3502.980	54	204.00	3519.970
4	4.00	3514.080	55	214.00	3519.980
5	5.00	3515.400	56	224.00	3520.000
6	6.00	3516.020	57	234.00	3519.970
7	7.00	3516.410	58	244.00	3519.970
8	8.00	3516.680	59	254.00	3519.960
9	9.00	3516.890	60	264.00	3519.960
10	10.00	3517.080	61	274.00	3519.950
11	11.00	3517.220	62	284.00	3519.970
12	12.00	3517.360	63	294.00	3520.000
13	13.00	3517.470	64	299.00	3519.960
14	14.00	3517.560			GI TYPE EDITERING
15	15.00	3517.670			0 - SLUTT
16	16.00	3517.740			1 - LISTING
17	17.00	3517.790			2 - SLETTING
18	18.00	3517.860			3 - ADDERING
19	19.00	3517.930			4 - ERSTATTING
20	20.00	3518.000			
21	22.00	3518.120			
22	24.00	3518.190			
23	26.00	3518.270			
24	28.00	3518.320			
25	30.00	3518.400			
26	32.00	3518.470			
27	34.00	3518.510			
28	36.00	3518.580			
29	38.00	3518.660			
30	40.00	3518.680			
31	45.00	3518.800			
32	50.00	3518.900			
33	55.00	3519.000			
34	60.00	3519.120			
35	65.00	3519.220			
36	70.00	3519.220			
37	75.00	3519.350			
38	80.00	3519.420			
39	85.00	3519.480			
40	90.00	3519.540			
41	95.00	3519.620			
42	100.00	3519.660			
43	105.00	3519.760			
44	110.00	3519.800			
45	115.00	3519.850			
46	124.00	3519.910			
47	134.00	3519.960			
48	144.00	3519.980			
49	154.00	3520.050			
50	164.00	3520.060			
51	174.00	3520.090			

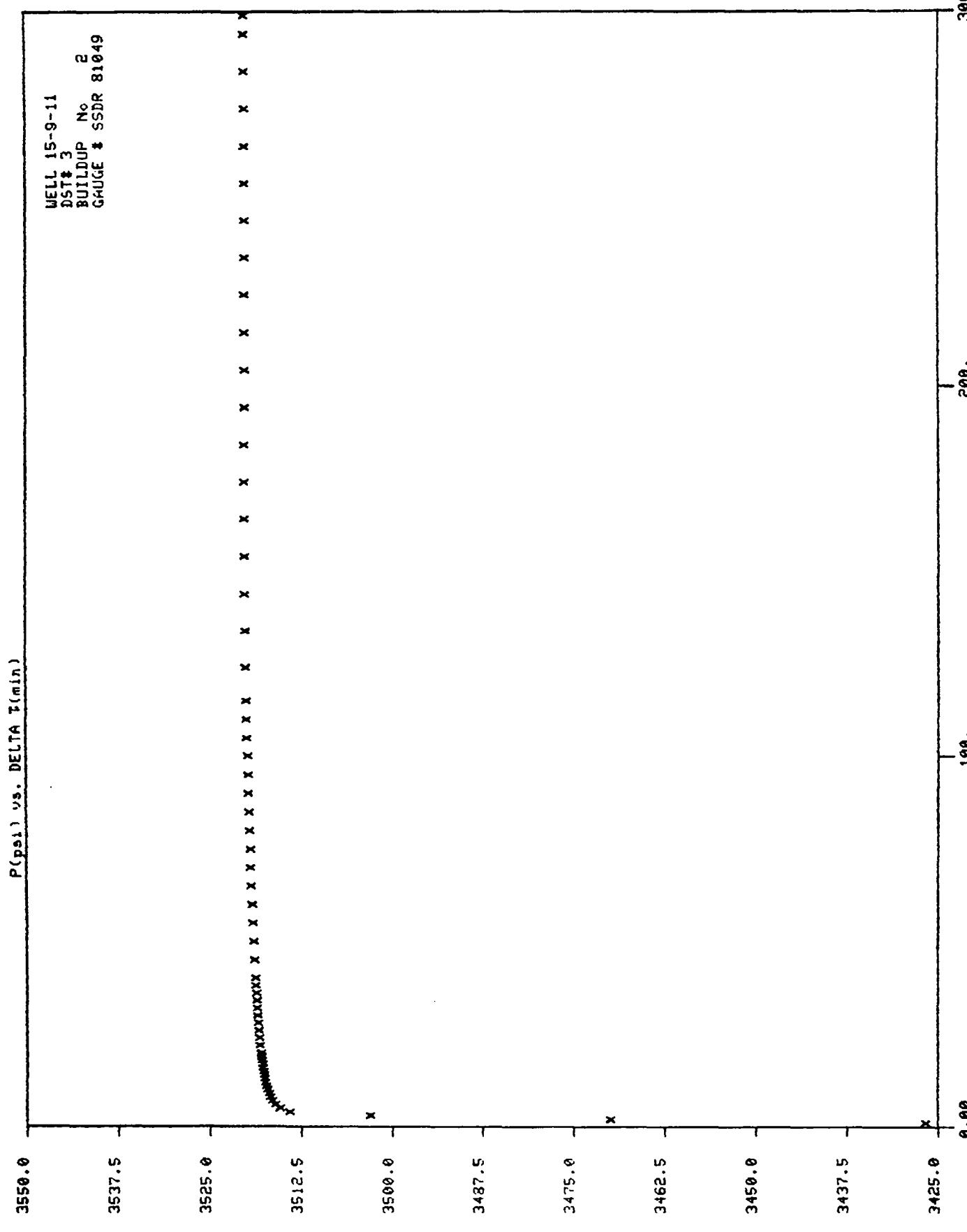


Fig. 4.7.

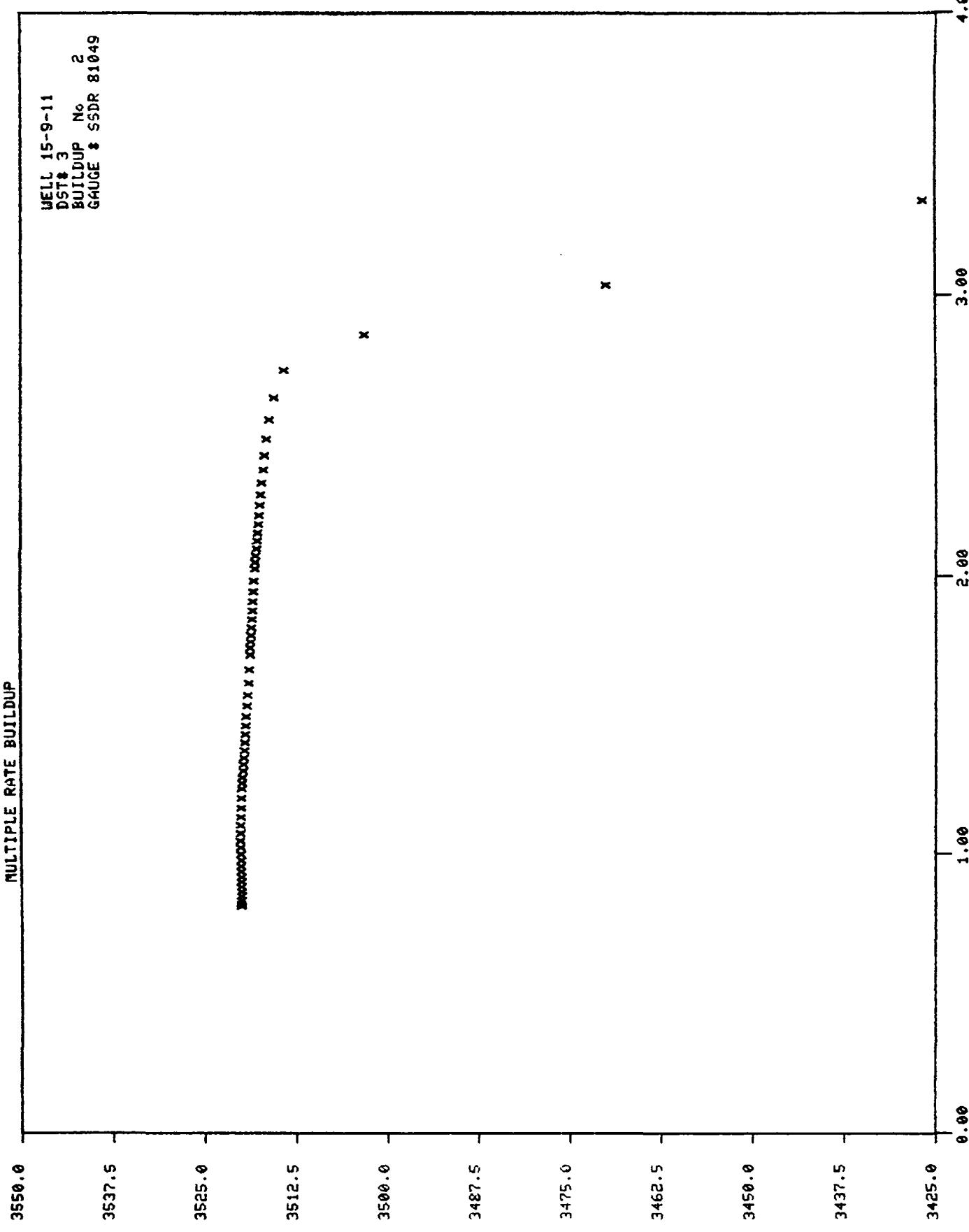


Fig. 4.8.

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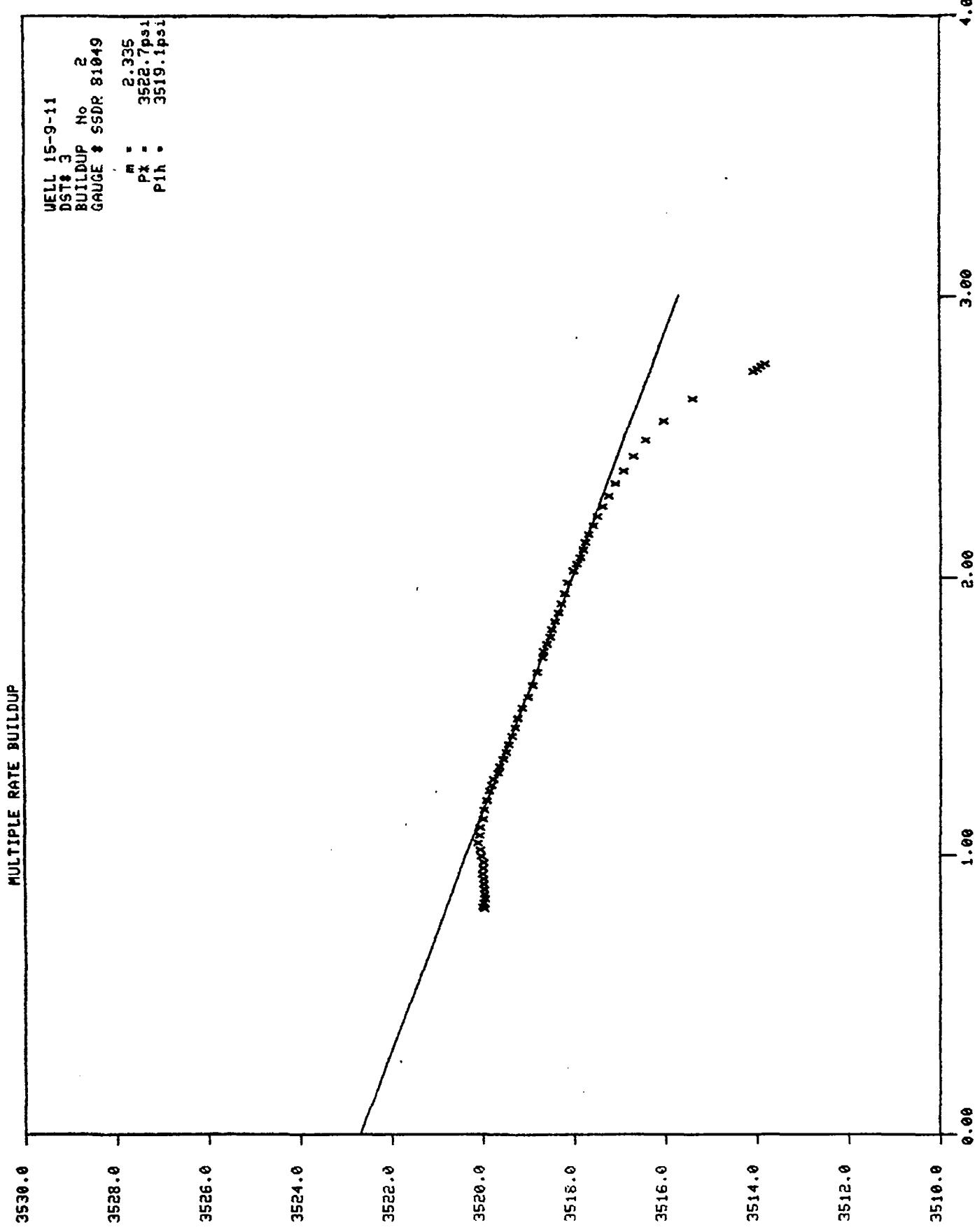


Fig. 4.9.

