Petroleum Reservoir Engineering
ABERDEEN, SCOTLAND

Supplementary Report for

STATOIL

Well: 34/10-1 DST 2 Flow 3 North Sea, Norway

Petroleum Reservoir Engineering
ABERDEEN, SCOTLAND
4 th December, 1978.

Statoil, Lagardsveien 78 P.O. Box 300, 4001 Stavanger, Norway.

Attention: Mr. Per Thomassan.

Subject: Supplementary Report
Well: 34/10-1 DST 2 Flow 3
North Sea, Norway.
Our File Number: RFLA-78059A

Gentlemen:

On August 24th 1978, a subsurface sample was collected from the subject well and forwarded to our Aberdeen laboratory. This report presents the results of analyses performed on this sample

A portion of the reservoir fluid was placed in a high pressure visual cell and thermally expanded to the reservoir temperature of 161°F. At this temperature a constant composition expansion was conducted during which a bubble point pressure of 3558 psig was observed. The results of the volumetric data is presented on page two.

A two-stage flash separation was conducted in the laboratory at the following conditions; 615 psia at 103°F., 15 psia at 60°F. The ratios and factors derived from this test are presented on page three. Also, gas samples evolved at each stage of separation were collected in the laboratory and analyzed for hydrocarbon composition. These compositions are listed on page four.

Additionally, the <u>primary stage</u> flash separation was repeated and the primary separator liquid was analyzed for hydrocarbon composition using low temperature fractional distillation apparatus. The results of this test are given on page five. Using the experimentally determined compositions of the primary separator gas and liquid a well stream composition was calculated and the results presented on page six.

In addition, the stock tank oil was collected and analyzed for hydrocarbon composition using low temperature fractional distillation apparatus. Using the experimentally determined compositions of the separator gas and stock tank oil, in conjunction with the factors and ratios derived from the flash separation, we were able to calculate a well stream composition. The resulting calculated well stream composition is given on page eight.

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Statoil:

Well: 34/10-1 DST 2 Flow 3.

Page Two.

Thank you for the opportunity to perform this fluid study. It is always a pleasure to be of service to Statoil, and should you have any questions or if we may be of further assistance, please do not hesitate to contact us.

Very truly yours

Core Laboratories U.K. Limited

John D. Oven

JDO/rmb: 7cc/Addressee:

John D. Owen. Supervisor.

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Company STATOIL	Date Sampled24th August, 1978.
Well 34/10-1 DST 2 Flow 3	County NORTH SEA
the state of the s	State NORWAY.
Field	StateNORMAL.
FORMATION CHA	RACTERISTICS
Formation Name	
Date First Well Completed	, 19
Original Reservoir Pressure	PSIG @Ft.
Original Produced Gas-Liquid Ratio	SCF/Bbl
Production Rate	Bbl/Day
Separator Pressure and Temperature	PSIG° F.
Oil Gravity at 60°F.	• АРІ
Datum	Ft. Subsea
Original Gas Cap	••••••
WELL CHARA	
Elevation	Ft.
Total Depth	Ft.
Producing Interval	1839-1844 M
Tubing Size and Depth	In. toFt.
Productivity Index	Bbl/D/PSI @Bbl/Day
Last Reservoir Pressure	PSIG @Ft.
Date	, 19
Reservoir Temperature	° F. @ Ft.
Status of Well	***************************************
Pressure Gauge	***************************************
Normal Production Rate	Bbl/Day
Gas-Oil Ratio	SCF/Bbl
Separator Pressure and Temperature	PSIG° F.
Base Pressure	PSIA
Well Making Water	% Cut
SAMPLING Co	
Sampled at	1530 M
Status of Well	COTION
Gas-Oil Ratio	SCF/Bbl
Separator Pressure and Temperature	PSIG° F.
Tubing Pressure	PSIG
Casing Pressure	PSIG
	Flopetrol
Sampled by	***************************************

REMARKS:

Received cylinder 20475-74 Sample 2a upper. Ambient bubble point is 3167 psig at 67°F.

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VOLUMETRIC DATA OF Reservoir Fluid SAMPLE

Taluma Dalationa

1.	Saturation pressure	(bubble-point pressure)	3558 PSIG @	161 °F.
_ •				

۷.	Pressure-volume Relations.	TICSSOFC	KCIC
		PSIG	<u>Volum</u>
			•
		F000	0 000

Pressure	Relative
PSIG	Volume (1)
	•
5000	0.9886
4700	0.9908
4400	0.9931
4000	0.9962
3900	0.9971
3800	0.9979
3700	0.9988
3558	1.0000

(1) Relative Volume is barrels of oil at indicated pressure and $161^{\circ}F$. per barrel of saturated oil at 3558 psig and $161^{\circ}F$.

7.9969.

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SEPARATOR TESTS OF Reservoir Fluid SAMPLE *

separator pressure PSIA	SEPARATOR TEMPERATURE ° F.	GAS/OIL RATIO	GAS/OIL RATIO (2)	STOCK TANK GRAVITY API @ 60° F.	FORMATION VOLUME FACTOR (3)	SEPARATOR VOLUME FACTOR (4)	SPECIFIC GRAVITY OF FLASHED GAS
615	103	367	421			1.145	0.610 +
to	•						
11/8	60	127	127	28.9	1.246	1.000	0.786 +
			548	0 2822			



- (2) Gas/Oil Ratio in cubic feet of gas @ 60° F. and14.73... PSI absolute per barrel of stock tank oil @ 60° F.
- (3) Formation Volume Factor is barrels of saturated oil @ ...3558. PSI gauge and ...161... ° F. per barrel of stock tank oil @ 60° F.
- (4) Separator Volume Factor is barrels of oil @ indicated pressure and temperature per barrel of stock tank oil @ 60° F.

These analyses, opinions or interpretations are based on observations and material supplied by the client to whom, and for whose exclusive and confidential use, this report is made. The interpretations or opinions expressed represent the best judgement of Core Laboratories, Inc. (all errors and employees, assume no responsibility and make no warranty or representations as to the productivity, proper operation, or profitableness of any oil, gas or other mineral well or sand in connection with which such report is used or relied upon.

^{*} Flow 3 (cylinder 2**047**5-74)

⁺ Gas and liquid collected for hydrocarbon analysis.

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HYDROCARBON ANALYSIS OF MULTI-STAGE SEPARATOR GASES

Separator Conditions:	615 PSIA @ 10	3°F.	15 PSIA @ 60	OF.
Component:	Mol Percent	<u>GPM</u>	Mol Percent	<u>GPM</u>
Hydrogen Sulfide	NIL		NIL	
Carbon Dioxide	1.63		2.79	
Nitrogen	0.92		0.32	
Methane -	91.70		72.34	
Ethane	4.74		15.67	
Propane	0.49	0.135	3.52	0.968
iso-Butane	0.18	0.059	1.70	0.556
n-Butane	0.12	0.038	1.45	0.457
iso-Pentane	0.09	0.033	0.96	0.351
n-Pentane	0.04	0.015	0.51	0.185
Hexanes	0.04	0.016	0.44	0.180
Heptanes plus	0.05	0.023	0.30	0.136
•	100.00	0.319	100.00	2.833
			•	
Calculated gas gravity (air=1	.000) 0.610		0.786	
Calculated gross heating valu	e = 1045 BT	U	1299	вти
per cubic foot of dry gas at	14.73 p	sia @ 60°F.	14.73	psia @6

Collected in the laboratory.

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Well3	STATOIL 34/10-1 DST 2 F1c	w 3 Cou	e Sampled nty	NORT)	H SEA	1978.
	HYDROCARBON AN	ALYSIS OFSei	parator Liquid	SAMPL	E *	
COMPONENT	MOL PERCENT	WEIGHT PERCENT	DENSITY @ 60° GRAMS PER CU CENTIMETER	BIC @	° API 60° F.	MOLECULAR WEIGHT
				v.		
Hydrogen Sulfide Carbon Dioxide	NIL 0.49	NIL 0.12				
Nitrogen Methane Ethane	0.06 15.45 3.55	0.01 1.32 0.56				
Propane iso-Butane	1.04 0.76	0.24	•			
n-Butane iso-Pentane	0.69 1.03	0.21 0.39				
n-Pentane Hexanes Heptanes plus	0.43 1.58 74.92	0.16 0.72 96.04	0.8873		27.8	243
rropuntoo prao	100.00	100.00		•• • • • • • • • • • • • • • • • • • •		

^{*} Collected in the laboratory at 615 psia and $103^{\circ}F$.

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r ee		.*		File .	RFLA-78059A	
11022	TOIL 10-1 DST 2 Flow 3		te Sampled	NORTH S		•••••
Field		Sta	.te	NORWAY		•••••
HYD	ROCARBON ANALYSIS	5 OF	Calculated .Wellstream	SAMPLE	<u> </u>	
COMPONENTS:			MOL PER CE	NT		
Hydrogen Sulfide	~		NIL			
Carbon Dioxide			0.92			
Nitrogen	•		0.39			
Methane		4	44.48			
Ethane			4.00			
Propane			0.83			
iso-Butane			0.54			
n-Butane			0.47			
iso-Pentane			0.67	•		
n-Pentane		* .	0.28			
Hexanes Heptanes plus		•	0.99 46.43			
			100.00			
Properties of Hept	anes Plus:					
API gravity at 60°	F.		27.8			
Specific Gravity a	t 60/60 ⁰ F		0.8881	•	•	
Molecular Weight			243			

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^{*} Calculated from two-stage separator test data-based on primary stage separator ratios and compositions of primary liquid and primary gas.

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Company Well	STATOIL 34/10-1 DST 2 1	Flow 3 Cou	nty	4th Augus ORTH SEA ORWAY	t, 1978.
	HYDROCARBON A	NALYSIS OFSto	ck Tank Oil SA	MPLE	
COMPONENT	MOL PERCENT	WEIGHT PERCENT	DENSITY @ 60° F. GRAMS PER CUBIC CENTIMETER	° API @ 60° F.	MOLECULAR WEIGHT
			c.		
Hydrogen Sulfide Carbon Dioxide Nitrogen	~ NIL Trace Trace	NIL Trace Trace			
Methane Ethane Propane so-Butane	0.22 0.55 0.44	0.02 0.07 0.08	•		
so-Butane n-Butane so-Pentane n-Pentane	0.55 0.53 1.03 0.58	0.14 0.14 0.33 0.18			
Hexanes Heptanes plus	2.03 94.07	0.75 98.29	0.8864	28.0	241

100.00

100.00

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Company		Sampled	24th August, 1978.		
Well 34/10-1 DST 2 Flow Field		ty	NORWAY.		
HYDROCARBON ANAL	YSIS OF Calcu	lated Wells	tream.		
COMPONENTS:		MOL PER CEN	NT ·		
Hydrogen Sulfide	•	NIL			
Carbon Dioxide		0.95			
Nitrogen		0.39			
Methane	* · · · · · · · · · · · · · · · · · · ·	43.92			
Ethane		4.01			
Propane		0.84			
iso-Butane		0.55			
n-Butane		0.49			
iso-Pentane	· · · · · · · · · · · · · · · · · · ·	0.67			
n-Pentane		0.37			
Hexanes		1.07		· · · · · · · · · · · · · · · · · · ·	
Heptanes plus	·	46.74			
		100.00	•		
Properties of Heptanes Plus:	*1				
API Gravity at 60°F.	· ·	28.0			
Specific Gravity at 60/60°F.		0.8871	•		
Molecular Weight.	•	241	_		

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^{*} Calculated from two-stage separator test data - based on stock tank ratios and compositions of stock tank oil.

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STATOIL

Well: 34/10-1 DST 2 Flow 3

Core Laboratories U.K. Limited Reservoir Fluid Analysis

John D. Owen

John D. Owen. Supervisor.