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OILFIELD SERVICES

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STATOIL

PVT STUDY ON

A BOTTOM HOLE SAMPLE

FROM

WELL 34/10-4 DST 1A

15 JULI 1980

**REGISTRERT  
OLJEDIREKTORATET**

AFFILIATED WITH

**REDWOOD INTERNATIONAL S.A.**

WORLD WIDE SERVICES FOR THE PETROLEUM PETROCHEMICAL & ALLIED INDUSTRIES

STATOIL

PVT STUDY ON  
A BOTTOM HOLE SAMPLE  
FROM  
WELL 34/10-4 DST 1A

SAMPLE CONTAINER NO. 73 FA 230-26

# OILFIELD SERVICES

# mbor

Reservoir Fluids Division

FILE NO. OA/526-79

STATOIL,  
Stavanger, Norway.

Gentlemen,

## WELL 34/10-4 DST 1A

Analysis of the Bottom Hole Sample consigned to us has been carried out as per your telex of 20th November, 1979 and the results are contained in the following report.

After determination of the Ambient Bubble Point of the sample it was re-pressurized to single phase and part transferred to a PVT cell for the determination of pressure-volume relations at Reservoir Temperature.

This portion of the sample was then used for the differential liberation experiment. The viscosities of the equilibrium gases at each pressure stage are calculated figures using the method of Carr, Kobayashi, and Burrows in Trans AIME (1954) 201 264-272.

Further portions were used for the determination of liquid viscosity in a rolling ball viscometer at reservoir temperature, and for the single stage separation followed by distillation and compositional analysis.

We have determined the composition of the reservoir fluid and the distribution of hydrocarbon types in the distillate, but were unable to detail the composition of the distillation residue.

The distillation residue is being sent to you and the remainder of the sample will be held here at our Ellesmere Port Laboratory until we receive further instructions from you.

If you have any queries, or we can be of any further assistance, please do not hesitate to contact us.

Yours faithfully,



P. L. Thomas

JOB NO. OA/526-79

WELL NO. 34/10-4 DST 1A

SUMMARY

Saturation Pressure at Ambient Temperature	Bar Gauge	212.6
Saturation Pressure at 72.2°C	Bar Gauge	235.5

Thermal expansion of reservoir oil at 344.7 bar gauge :

From 15.5°C to 72.2°C	% per °C	0.926
Vol. at 72.2°C/Vol. at 15.5°C		1.0525

Compressibility of Reservoir Oil at 72.2°C :

<u>From Bar Gauge</u>	<u>To Bar Gauge</u>	<u>Vol./Vol./Bar x 10<sup>6</sup></u>
344.7	327.5	114
327.5	310.3	119
310.3	293.0	125
293.0	275.8	133
275.8	258.6	142
258.6	246.8	152
246.8	235.5	163

Saturated oil at 235.5 bar gauge and 72.2°C :

Density kg/m <sup>3</sup>	756.0
Viscosity Ns/m <sup>2</sup>	0.0011784
Formation Volume Factor of Oil	1.2816
Gas liberated by single stage separation:	
Vol. gas at 1.013 bar 15°C/Vol. residual oil	106.7

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WELL. 34/10-4 DST 1A

TABULAR DATA

Pressure Bar Gauge	Pressure-Volume Relations @ 72.2°C V/V Sat	Viscosity of Oil @ 72.2°C Ns/m <sup>2</sup>	Differential Liberation at 72.2°C		
			Liberated Gas Vol.	Solution Gas Volume	Vol. Reservoir Oil Vol. Residual Oil = Formation Volume Factor
344.7	0.9856	0.00171			1.2631
327.5	0.9875	0.00163			1.2656
→ 310.3	0.9895	0.00154			1.2682
293.0	0.9917	0.00146			1.2710
275.8	0.9939	0.00137			1.2738
258.6	0.9964	0.00129			1.2770
241.3	0.9981	0.00121			1.2792
* 235.5	1.0000	0.00118	0	100.29	1.2816
234.4	1.0009	0.00118	-	-	-
227.7	1.0067	-	-	-	-
220.6	1.0134	-	-	-	-
206.8	1.0284	0.00124	13.74	86.55	1.2471
186.2	1.0573	0.00128	21.74	78.55	1.2297
165.5	1.0964	0.00134	29.85	70.44	1.2122
144.8	1.1510	0.00141	37.47	62.82	1.1962
124.1	1.2296	0.00149	45.72	54.57	1.1779
103.4	1.3476	0.00159	53.96	46.33	1.1617
82.7	1.5370	0.00170	62.17	38.12	1.1452
62.1	-	0.00188	70.47	29.82	1.1303
41.4	-	0.00212	78.87	21.42	1.1132
20.7	-	0.00262	-	-	-
6.8	-	-	94.50	5.79	1.0730
0	-	0.00354	100.29	0	1.0437

\* Saturation Pressure

Density of Residual Oil at 15°C 881.4 kg/m<sup>3</sup>

V Sat = Volume of Reservoir Oil at 235.5 Bar Gauge and 72.2°C.

V = Volume at any other pressure.

Gas and Residual Oil Volumes are at 1.013 Bar and 15°C.

## INDEPENDENT ANALYSIS

Job No. OA 526-79

Well 34/10-4 DST

### TABULAR DATA II

1A

P.V. "Y" FUNCTION :-		DIFFERENTIAL LIBERATION GAS :-		
PRESSURE BAR GAUGE	$Y = \frac{(P_{SAT} - P)}{(P)(V/V_{SAT} - 1.000)}$	COMPRESSIBILITY FACTOR $Z = \frac{PV}{NRT}$	B <sub>g</sub>	SPECIFIC GRAVITY LIBERATED GAS (AIR = 1.000)
235.5	Saturation Pressure			
206.8	4.841	0.8690	193.9	0.7025
186.2	4.600	0.8680	174.4	0.6932
165.5	4.358	0.8676	155.3	0.6848
144.8	4.118	0.8677	135.3	0.6777
124.1	3.876	0.8686	116.1	0.6732
103.4	3.636	0.8706	96.3	0.6717
82.7	3.395	0.8738	77.1	0.6725
62.1	-	0.8796	58.0	0.6775
41.4	-	0.8903	38.5	0.6898
6.8	-	-	-	0.7642
0	-	-	-	0.9603

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TABULAR DATA III

CALCULATED VISCOSITY OF GASES AT 72.2°C FROM DIFFERENTIAL LIBERATION

<u>PRESSURE</u> Bar Gauge	<u>VISCOSITY</u> Ns/m <sup>3</sup> x 10 <sup>-5</sup>
206.8	2.09
186.2	1.93
165.5	1.80
144.8	1.67
121.1	1.55
103.4	1.47
82.7	1.38
62.1	1.32
41.4	1.28
6.8	1.16
0	1.08

Job No. OA 526-79Well 34/10-4 DST 1ADENSITY OF OIL AT 72.2°C AS A FUNCTION OF PRESSURE

PRESSURE BAR GAUGE	DENSITY kg/m <sup>3</sup>
344.7	767.1
327.5	765.5
310.3	764.0
293.0	762.3
275.8	760.6
258.6	758.7
241.3	757.4
* 235.5	756.0
<hr/>	
206.8	767.4
186.2	772.8
165.5	778.3
144.8	783.4
124.1	789.8
103.4	795.0
82.7	800.5
62.1	805.0
41.4	811.0
20.7	827.8
0	844.5

\* Saturation Pressure



JOB No. 0A/526-79

WELL No. 34/10 -4 DST 1A

SEPARATOR TESTS

Separator Pressure Bar Gauge	Gas/Oil Ratios See Footnote (A)		Stock Tank Gravity °API at 60°F	Shrinkage Factor Vsto/Vsat See Footnote (B)	Vsat/Vsto See Footnote (B)	Specific Gravity of Flashed Gas See Footnote (C)	Separator Temp °C
	1st Stage	Total					
0	-	106.67	28.59	0.7735	1.293	0.658	15

NOTES :

- (A) Gas/Oil ratio in volumes of gas at 1.013 bar and 15°C relative to volume of Stock Tank Oil at atmospheric pressure and 15°C.
- (B) Vsto is the volume of Stock Tank Oil at 15°C and atmospheric pressure produced by one volume of reservoir oil, Vsat, at saturation pressure and reservoir temperature.
- (C) Specific gravity of gas relative to air 15°C/15°C

FILE NO. OA/526-79

WELL NO. 34/10-4 DST 1A

COMPOSITIONAL ANALYSIS OF RESERVOIR FLUID

<u>COMPONENT</u>	<u>% MOLE</u>		
Nitrogen			1.54
Carbon Dioxide			0.58
Hydrogen Sulphide			0.00
Methane			50.28
Ethane			3.64
Propane			1.35
Iso-Butane			0.59
N-Butane			0.77
Iso-Pentane			0.61
N-Pentane			0.30
Hexanes			0.87
Heptanes	0.698	100.198	3.55
Octanes	0.707	114.224	3.40
Nonanes	0.722	128.250	3.60
Decanes	0.734	142.276	3.30
Undecanes Plus	0.903	372	25.62

} 39.47

Density of undecanes plus =  $903.0 \text{ kg/m}^3$  at  $15^\circ\text{C}$

Average molecular weight of undecanes plus = 372

Asphaltenes = 0.13% by weight

FILE NO. OA/526-79

WELL NO. 34/10-4 DST 1A

COMPOSITIONAL ANALYSIS OF DISTILLATE

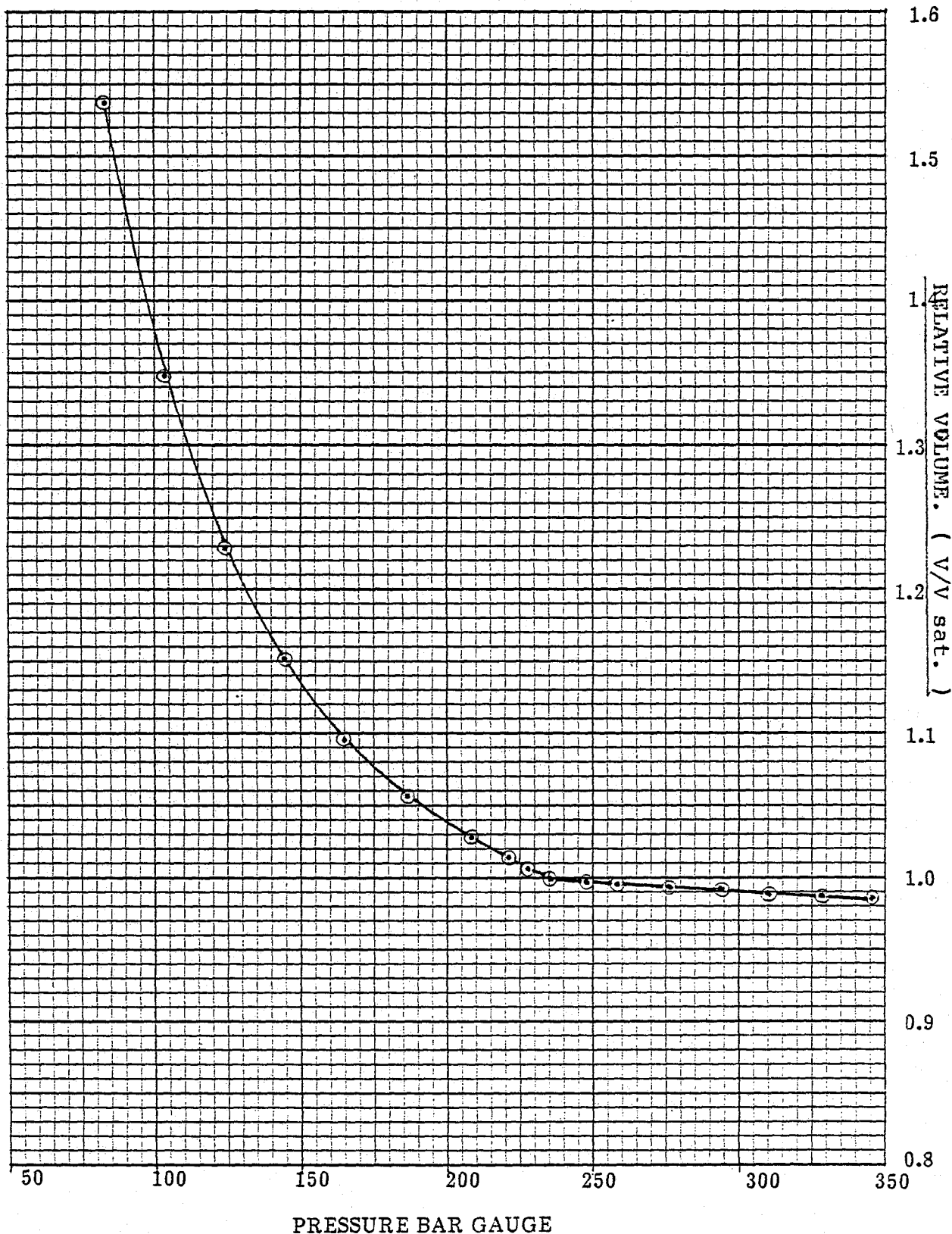
<u>CARBON NUMBER</u>	<u>HYDROCARBON TYPE % WEIGHT</u>		
	<u>AROMATICS</u>	<u>NAPHTHENES</u>	<u>PARAFFINS</u>
C3	-	-	0.04
C4	-	-	0.36
C5	-	0.31	1.60
C6	0.32	4.35	3.02
C7	2.99	8.20	4.09
C8	5.37	9.48	4.79
C9	13.61	9.64	5.37
C10	12.12	9.02	5.32
	<hr/>	<hr/>	<hr/>
	34.41	41.00	24.59



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RELATIVE VOLUMES DURING PRESSURE VOLUME RELATIONS AT 72.2°C

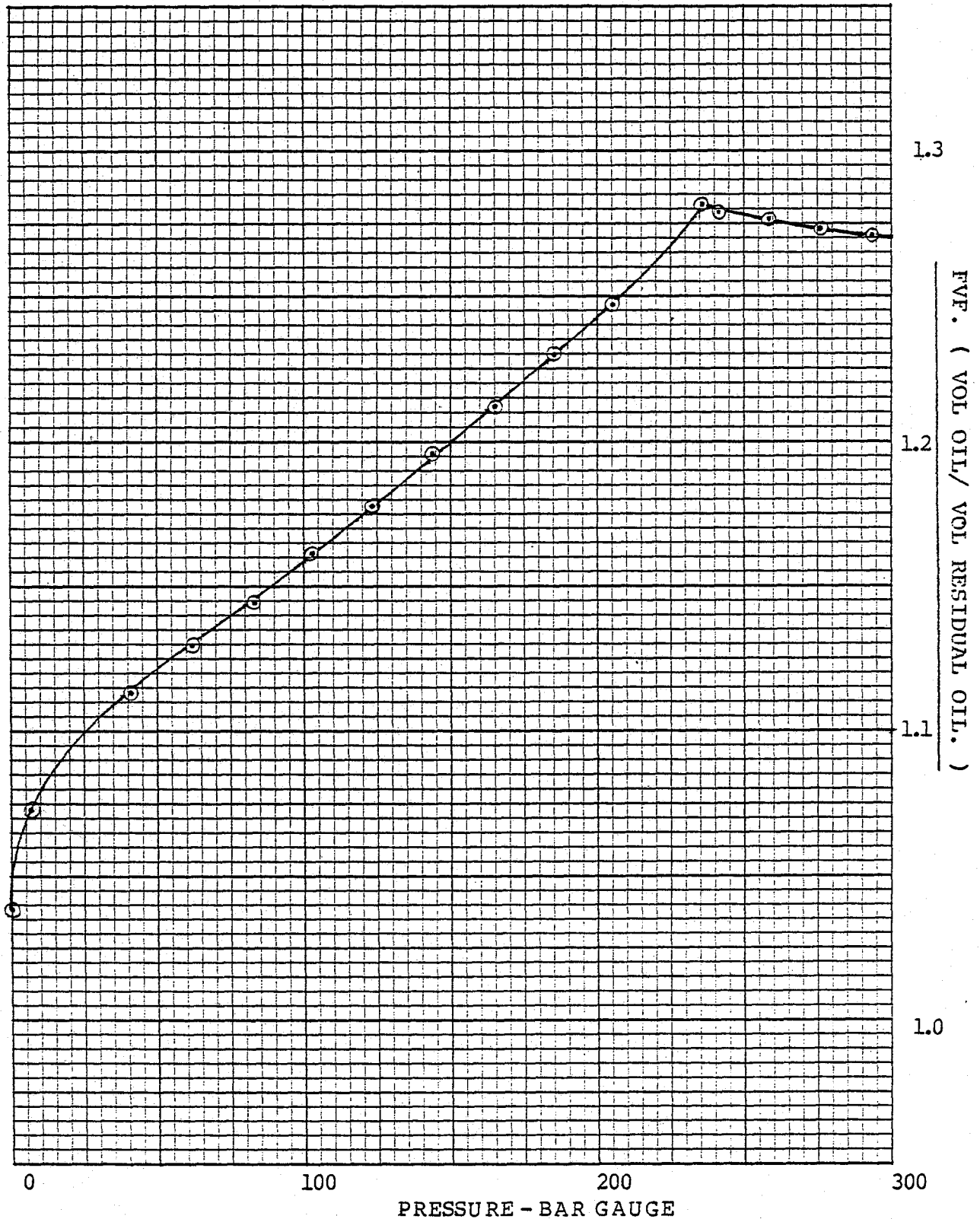


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FORMATION VOLUME FACTOR DURING DIFFERENTIAL LIBERATION AT 72.2°C

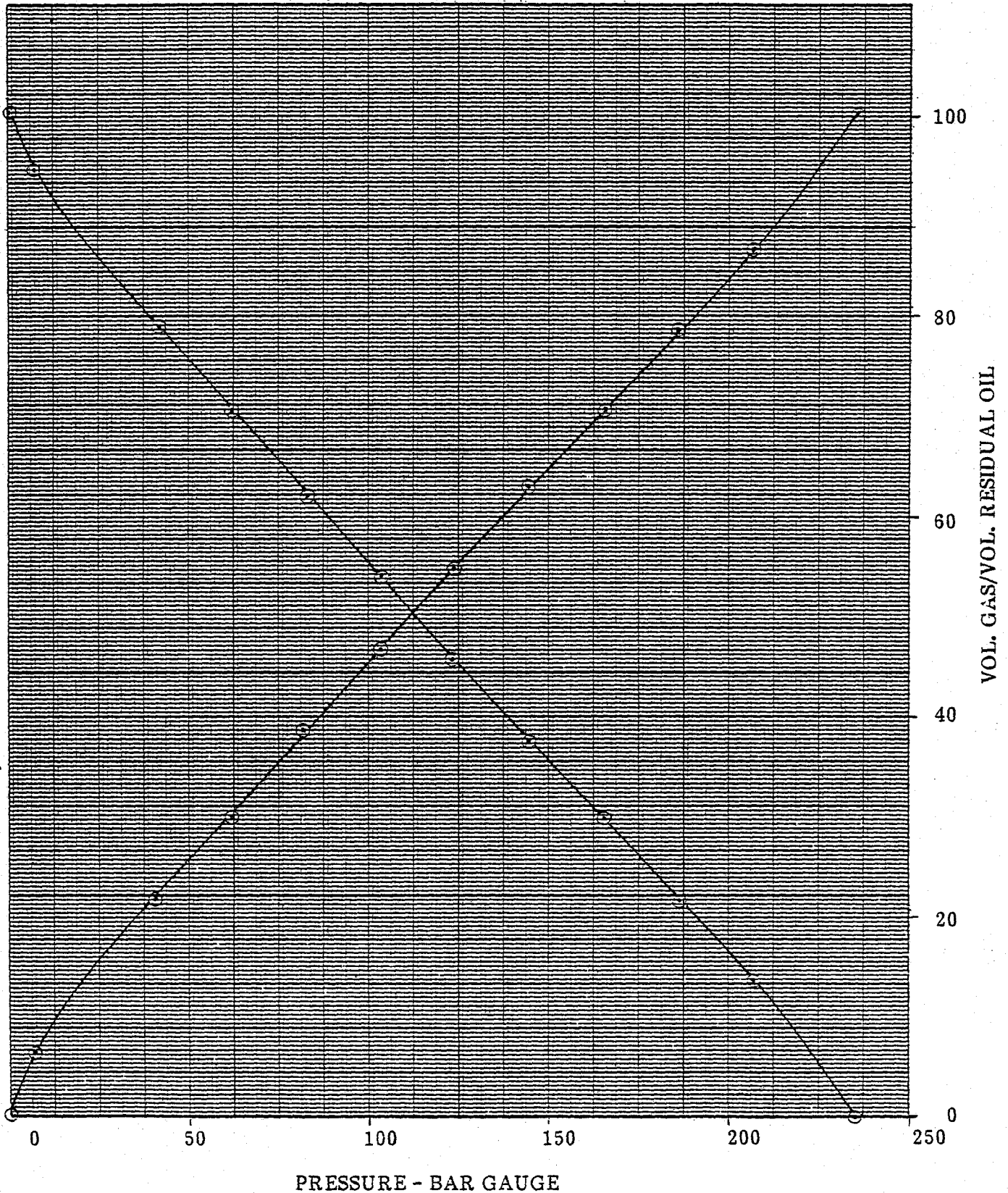


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LIBERATED GAS & SOLUTION GAS DURING DIFFERENTIAL LIBERATION @ 72.2°C

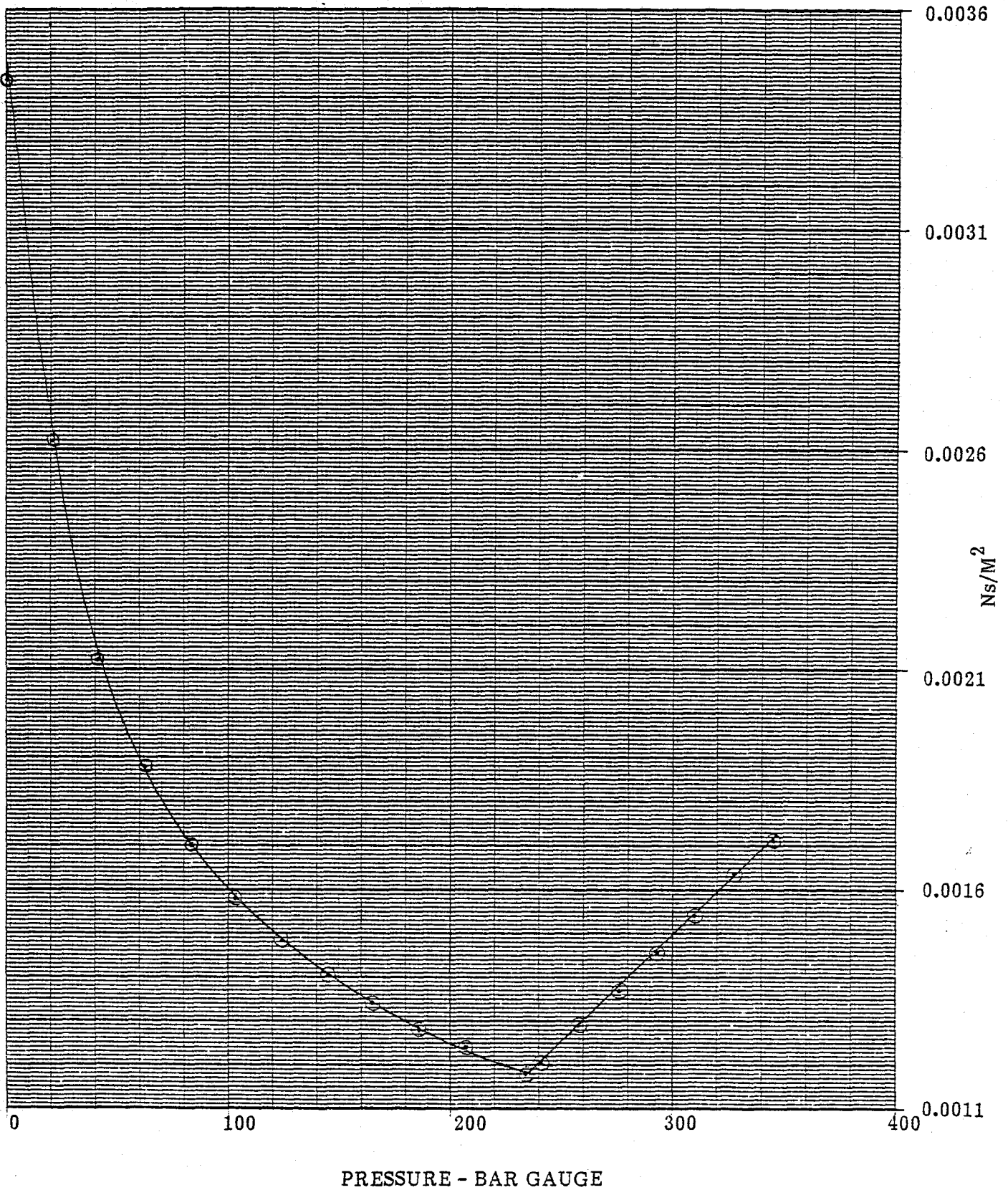


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VISCOSITY OF OIL DURING DIFFERENTIAL LIBERATION @ 72.2°C

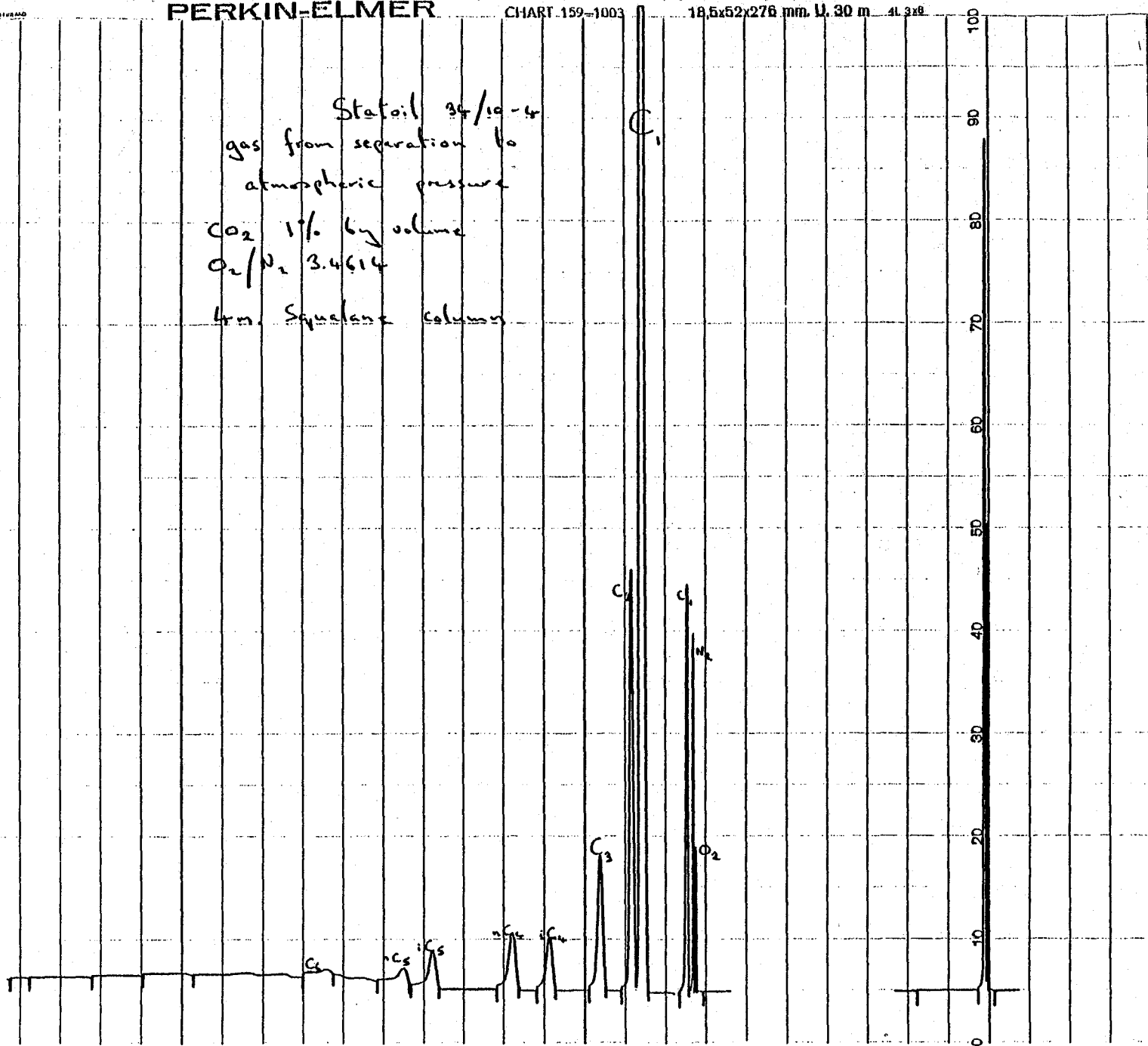


Statoil 34/10-4  
gas from separation to  
atmospheric pressure

CO<sub>2</sub> 1% by volume

O<sub>2</sub>/N<sub>2</sub> 3.4614

4m. Squalane column



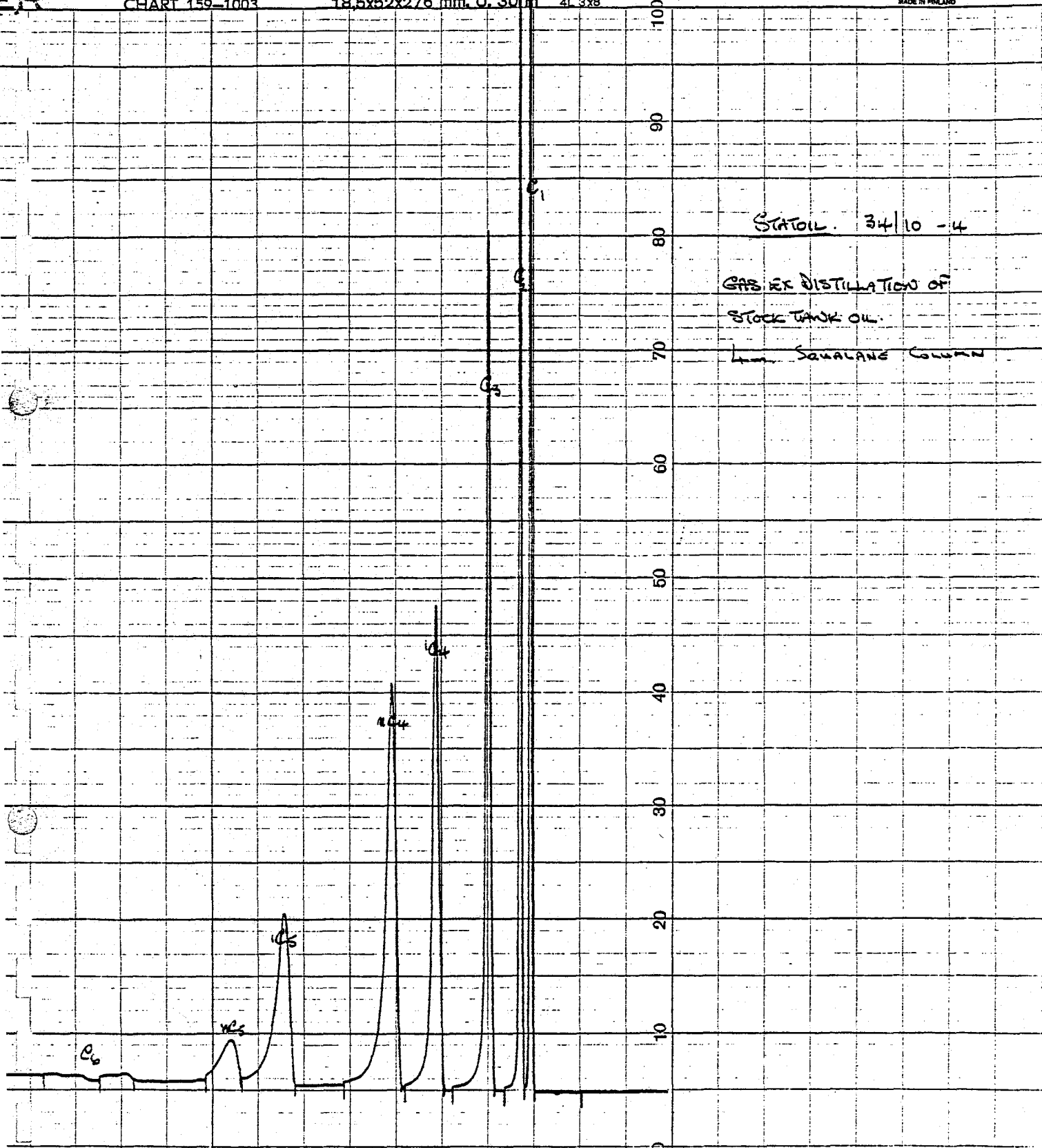


ER

CHART 159-1003

18.5x52x276 mm. U. 30µm 4L 3x8

MADE IN FINLAND



STATOIL. 34/10-4

GAS EX DISTILLATION OF  
STOCK TANK OIL.

LOW SQUALANE COLUMN

ER

CHART 159-1003

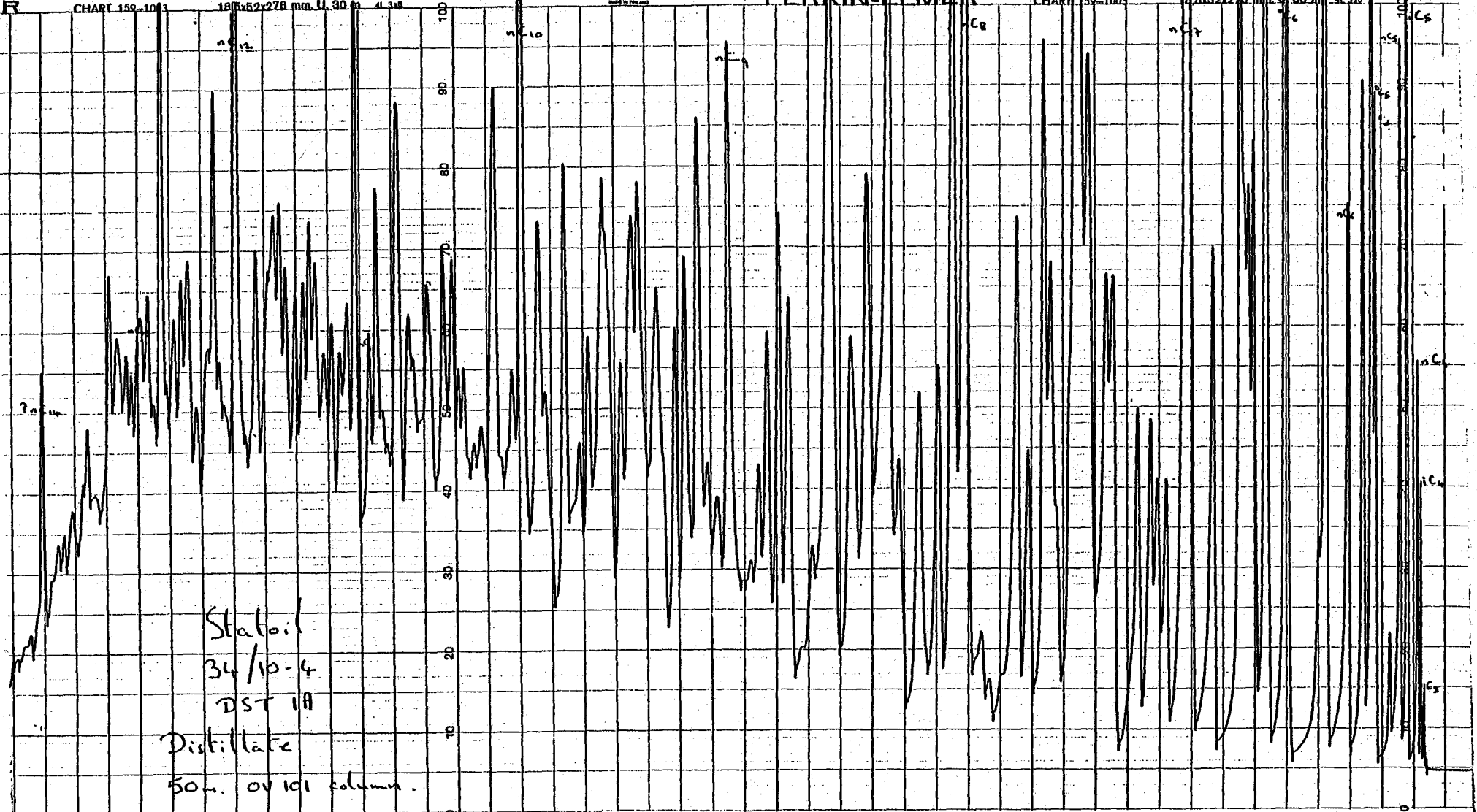
18.5x62x278 mm. U. 30 m. 4L 318

PERKIN-ELMER

CHART 159-1003

18.5x62x278 mm. U. 30 m. 4L 318

100  
90  
80  
70  
60  
50  
40  
30  
20  
10  
0



Station  
34/10-4  
DST 1A

Distillate  
50m. OV 101 column.