

**CORE LABORATORIES UK LTD.**  
*Petroleum Reservoir Engineering*  
**ABERDEEN, SCOTLAND**

SPECIAL STUDY

for

Statoil A/S

Well: 34/10-4 DST 1

North Sea, Norway.

**CORE LABORATORIES UK LTD.**  
*Petroleum Reservoir Engineering*  
**ABERDEEN, SCOTLAND**

28th February 1981

Statoil A/S  
P.O. Box 300  
4001 Stavanger  
Norway

Subject: Special Study  
Well: 34/10-4 DST 1  
North Sea, Norway.  
Our File Number:  
RFLA 80201C

Attention: Per Thomassen.

Gentlemen,

The following report contains the details of a revaporization study performed on samples from the subject well as requested by a representative of Statoil A/S.

The hydrocarbon composition of both the initial reservoir fluid and the injection gas previously reported are given on pages two and three.

The measured deviation factor  $Z$  of the synthesised injection gas may be found on page four.

A portion of the reservoir fluid was placed in a high pressure visual cell and thermally expanded to the operating temperature of 73°C. During a constant composition expansion at this temperature, the fluid was observed to have a saturation pressure of 239.6 Bar G. The partial pressure-volume relations, and the associated compressibility data for the undersaturated fluid may be found on page six.

The revaporization study was then performed contacting the reservoir fluid with the injection gas at 330.9 Bar G and 73.0°C and after equilibration the excess gas was removed at constant pressure and analysed for hydrocarbon composition. This process was repeated for a series of nine injections, at which point the test was terminated. The factors and data derived from this test, and the hydrocarbon composition of each effluent may be found on pages seven and eight of the report.

The hydrocarbon composition of the residual fluid was determined by low temperature fractional distillation, and this composition in terms of both mol and weight percent is presented on page nine.

A single stage flash separation (zero shrinkage) was performed on a portion of the residual oil and the factors and data derived from this test are presented on page ten.

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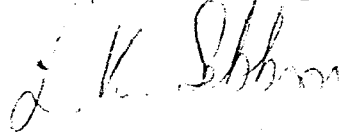
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It has been a pleasure to be of service to Statoil A/S. Should any questions arise concerning data presented in this report please do not hesitate to contact us.

Yours very truly

Core Laboratories UK Limited  
Reservoir Fluid Analysis



Les K. Sebborn  
Laboratory Manager

LKS/STB  
10CC/ADDRESSEE

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Company Statoil A/S Date Sampled \_\_\_\_\_

Well 34/10 - 4 DST 1 State North Sea

Field \_\_\_\_\_ Country Norway

**FORMATION CHARACTERISTICS**

Formation Name	_____
Date First Well Completed	_____, 19__
Original Reservoir Pressure	_____ PSIG @ _____ Ft.
Original Produced Gas-Oil Ratio	_____ SCF/Bbl
Production Ratio	_____ Bbl/Day
Separator Pressure and Temperature	_____ PSIG _____ °F.
Oil Gravity at 60°F.	_____ °API
Datum	_____ Ft. Subsea
Original Gas Cap	_____

**WELL CHARACTERISTICS**

Elevation	_____	Ft.
Total Depth	_____	Ft.
Producing Interval	_____	Ft.
Tubing Size and Depth	_____ In. to _____	Ft.
Productivity Index	_____ Bbl/D/PSI @ _____	Bbl/Day
Last Reservoir Pressure	_____ PSIG @ _____	Ft.
Date	_____, 19__	
Reservoir Temperature	73 _____ °C. @ _____	Ft.
Status of Well	_____	
Pressure Gauge	_____	
Normal Production Rate	_____	Bbl/Day
Gas-Oil Ratio	_____	SCF/Bbl
Separator Pressure and Temperature	_____ PSIG, _____	°F.
Base Pressure	_____	PSIA
Well Making Water	_____	% Cut

**SAMPLING CONDITIONS**

Sampled at	_____	Ft.
Status of Well	_____	
Gas-Oil Ratio	_____	SCF/Bbl
Separator Pressure and Temperature	_____ PSIG, _____	°F.
Tubing Pressure	_____	PSIG
Casing Pressure	_____	PSIG
Sampled by	FLOPETROL	
Type Sampler	FOLPETROL	

REMARKS: Cylinder Numbers 2657-30 and 20475-62

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Company Statoil A/S Formation \_\_\_\_\_  
 Well 34/10-4 DST 1 County North Sea  
 Field \_\_\_\_\_ State Norway

HYDROCARBON ANALYSIS OF Reservoir Fluid SAMPLE

COMPONENT	MOL PERCENT	WEIGHT PERCENT	DENSITY	API	MOL WEIGHT
Hydrogen Sulfide	NIL	NIL			
Carbon Dioxide	1.07	0.39			
Nitrogen	0.25	0.06			
Methane	44.98	5.95			
Ethane	3.05	0.76			
Propane	0.99	0.36			
iso-Butane	0.54	0.26			
n-Butane	0.91	0.43			
iso-Pentane	0.63	0.37			
n-Pentane	0.49	0.29			
Hexanes	1.32	0.93			
Heptanes plus	45.77	90.20	0.8880	27.7	239
	<u>100.00</u>	<u>100.00</u>			

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Company Statoil A/S Formation

Well 34/10-4 DST 1 County North Sea

Field  State Norway

HYDROCARBON ANALYSIS OF Synthesised Injection GAS SAMPLE

<u>COMPONENT</u>	<u>MOL PERCENT</u>	<u>GPM</u>
Hydrogen Sulfide	NIL	
Carbon Dioxide	1.79	
Nitrogen	1.17	
Methane	85.47	
Ethane	6.93	
Propane	2.15	0.590
iso-Butane	0.77	0.251
n-Butane	0.86	0.270
iso-Pentane	0.41	0.150
n-Pentane	0.17	0.062
Hexanes plus	0.28	0.119
	<u>100.00</u>	<u>1.442</u>

Calculated gas gravity (air = 1.000) = 0.673

Calculated gross heating value = 1131 BTU per cubic foot of dry gas at 14.696 psia and 60°F.

Collected at 0 psig and 65°F.

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Well 34/10-4 DST 1

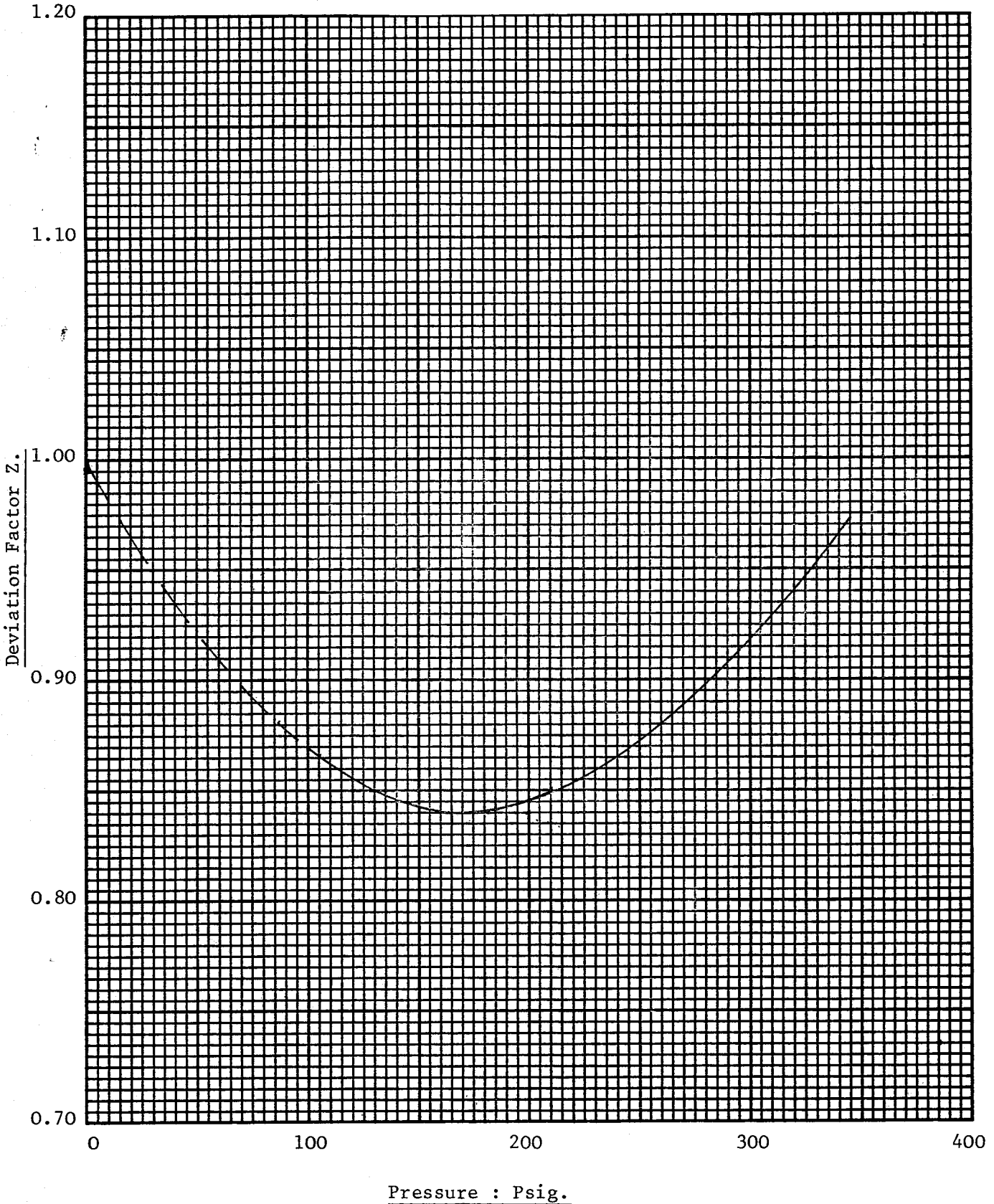
MEASURED GAS DEVIATION FACTOR Z OF  
SYNTHESISED INJECTION GAS AT 73.0°C.

<u>Pressure Bar G</u>	<u>Deviation Factor Z</u>
344.7	0.972
330.9	0.954
310.3	0.928
296.5	0.913
275.8	0.894
241.3	0.866
206.8	0.847
172.4	0.840
137.9	0.845
103.4	0.866

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Deviation Factor Z of Synthesized Injection Gas at 73.0°C.

Company Statoil A/S Formation \_\_\_\_\_  
Well 34/10 - 4 DST 1 County North Sea  
Field \_\_\_\_\_ State Norway





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VOLUMETRIC DATA OF Original Reservoir Fluid SAMPLE

1. Saturation pressure (bubble-point pressure) 239.6 BAR G @ 73.0 °C.  

$$\frac{V @ 73.0 \text{ °C.}}{V @ 17.8 \text{ °C.}} = 1.05059$$
2. Thermal expansion of saturated oil @ 344.7 BAR G =  $\frac{V @ 73.0 \text{ °C.}}{V @ 17.8 \text{ °C.}} = 1.05059$
3. Compressibility of saturated oil @ reservoir temperature: Vol/Vol/BAR G:
  - From 344.7 BAR G to 310.3 BAR G =  $11.07 \times 10^{-5}$
  - From 310.3 BAR G to 275.8 BAR G =  $12.07 \times 10^{-5}$
  - From 275.8 BAR G to 239.6 BAR G =  $12.58 \times 10^{-5}$
4. Pressure-Volume Relations:

<u>Pressure Bar G</u>	<u>Relative Volume (l)</u>
344.7	0.9875
310.3	0.9913
275.8	0.9954
262.0	0.9971
255.1	0.9980
248.2	0.9989
241.3	0.9998
<u>239.6</u> Saturation Pressure	1.0000

- (1) Relative Volume:  $V/V_{\text{sat}}$  is cubic metres at indicated pressure per cubic metre at saturation pressure.

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REVAPOORIZATION STUDY AT 330.9 BAR G AND 73.0°F.

Basis: 1 mol of original reservoir fluid.  
 Volume of original reservoir fluid at 330.9 Bar G and 73.0°F = One pore volume.

Injection Number	Gas Injected				Incremental Mols of Gas Produced	Mols of Liquid Phase Remaining	Relative Liquid Phase
	Pore Volumes		Mols				
	Incremental	Cumulative	Incremental	Cumulative			
0	0.0000	0.0000	0.0000	0.0000	0.0000	1.0000	1.0000
1	0.5187	0.5187	0.9811	0.9811	0.8439	1.1372	1.0412
2	0.5187	1.0374	0.9811	1.9622	1.0711	1.0471	1.0193
3	0.5187	0.5561	0.9811	2.9433	1.0306	0.9976	0.9940
4	0.5187	2.0748	0.9811	3.9244	1.0203	0.9584	0.9655
5	0.5187	2.5935	0.9811	4.9055	1.0172	0.9222	0.9343
6	0.5187	3.1122	0.9811	5.8866	1.0140	0.8893	0.9040
7	0.5187	3.6309	0.9811	6.8677	1.0112	0.8591	0.8760
8	0.5187	4.1496	0.9811	7.8488	1.0088	0.8314	0.8510
9	0.5187	4.6683	0.9811	8.8299	1.0050	0.8074	0.8271

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Well 34/10-4 DST 1

REVAPORIZATION STUDY AT 330.9 BAR G and 73.0°C.

Hydrocarbon Analyses of Produced Gases - Mol Per Cent

<u>Component</u>	<u>Injection Number</u>								
	<u>1</u>	<u>2</u>	<u>3</u>	<u>4</u>	<u>5</u>	<u>6</u>	<u>7</u>	<u>8</u>	<u>9</u>
Carbon Dioxide	1.39	1.50	1.57	1.62	1.66	1.69	1.71	1.73	1.74
Nitrogen	0.93	1.01	1.08	1.14	1.17	1.20	1.20	1.21	1.21
Methane	83.16	83.44	83.68	83.88	84.04	84.18	84.30	84.30	84.41
Ethane	5.62	6.04	6.38	6.60	6.80	6.91	6.98	7.00	7.02
Propane	1.39	1.63	1.85	1.98	2.07	2.14	2.20	2.25	2.28
iso-Butane	0.53	0.60	0.67	0.72	0.75	0.78	0.79	0.80	0.80
n-Butane	0.62	0.70	0.77	0.83	0.86	0.89	0.90	0.91	0.91
iso-Pentane	0.45	0.41	0.38	0.36	0.35	0.34	0.33	0.33	0.32
n-Pentane	0.23	0.20	0.18	0.17	0.16	0.15	0.15	0.14	0.14
Hexanes	0.43	0.33	0.28	0.24	0.22	0.20	0.19	0.18	0.18
Heptanes Plus	5.26	4.47	3.44	2.70	1.93	1.53	1.26	1.07	0.90
	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>	<u>100.00</u>
Molecular weight of heptanes plus	126	129	131	133	135	136	137	138	139
Specific gravity of heptanes plus	0.765	0.768	0.770	0.772	0.774	0.775	0.776	0.777	0.778

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Company Statoil A/S Formation \_\_\_\_\_  
 Well 34/10-4 DST 1 County North Sea  
 Field \_\_\_\_\_ State Norway

HYDROCARBON ANALYSIS OF Residual Oil SAMPLE\*

COMPONENT	MOL PERCENT	WEIGHT PERCENT	DENSITY	API	MOL WEIGHT
Hydrogen Sulfide	NIL	NIL			
Carbon Dioxide	2.73	1.09			
Nitrogen	0.46	0.12			
Methane	52.91	7.71			
Ethane	5.73	1.56			
Propane	2.56	1.03			
iso-Butane	1.06	0.56			
n-Butane	1.32	0.70			
iso-Pentane	1.22	0.80			
n-Pentane	0.59	0.38			
Hexanes	0.62	0.48			
Heptanes plus	30.80	85.57	0.9047	24.8	306
	<u>100.00</u>	<u>100.00</u>			

\*From revaporization test at 330.9 BAR G.

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Well 34/10-4 DST 1

SEPARATOR TESTS OF Residual Oil SAMPLE

Separator Pressure, BAR Gauge	Separator Temperature °C.	Separator Gas/Oil Ratio(1)	Stock Tank Gas/Oil Ratio(1)	Stock Tank Density Kg/L @ 15°F.	Shrinkage Factor, Vr/Vsat(2)	Formation Volume Factor Vsat/Vr(3)	Specific Gravity of Flashed Gas
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0	20	142		0.8898	0.7402	1.351	0.742
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- (1) Separator and Stock Tank Gas/Oil Ratio in cubic metres of gas @ 15°C and 1.0132 Bar absolute per cubic metre of stock tank oil at 15°C.
- (2) Shrinkage Factor: Vr/Vsat is cubic metres of stock tank oil at 15°C. per cubic metre of saturated oil at 330.9 Bar gauge and 73.0°C.
- (3) Formation Volume Factor: Vsat/Vr is cubic metres of saturated oil at 330.9 Bar gauge and 73.0°C per cubic metre of stock tank oil at 15°C.

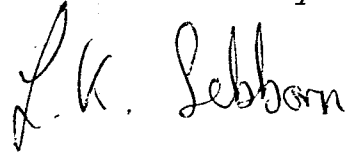
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**ABERDEEN, SCOTLAND**

STATOIL A/S  
Well: 34/10-4 DST 1

RFLA: 80201C

Core Laboratories UK Limited  
Reservoir Fluid Analysis

A handwritten signature in black ink, appearing to read 'L. K. Sebborn'.

Les K. Sebborn  
Laboratory Manager-RFL