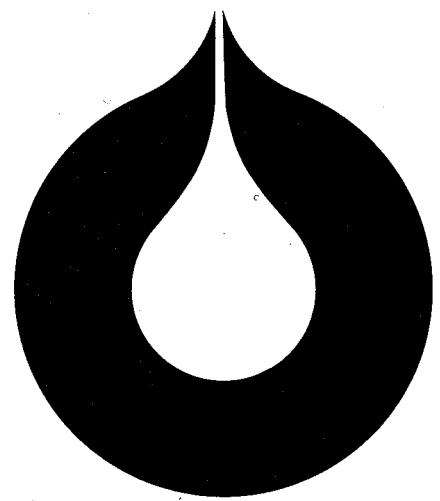


L-222

725.5

S

CD



**statoil**

**FORTROLIG**

i h.t. Beskyttelsesinstruksen,  
jfr. offentlighetslovens

§..... nr.....

**WELL TEST REPORT**

PL. 050

10 OKT. 1980

WELL NO. 34/10-4

**REGISTRERT**  
**OLJEDIREKTORATET**

SEPTEMBER 1980

**Den norske stats oljeselskap a.s**

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WELL TEST REPORT

PL. 050

10 OKT. 1980

WELL NO. 34/10-4

**REGISTRERT**  
**OLJEDIREKTORATET**

SEPTEMBER 1980

LEIF MAGNE MELING

## WELL DATA

Operator : Den norske stats oljeselskap  
Well name : 34/10-4  
Location : 61°12' 15.12"N  
              02°13' 55.73"E  
Classification : Exploration well  
Drilling rig : Ross Rig  
Spudded : 12. Aug. 1979  
Completed : 17. Oct. 1979  
RKB elevation : 25 m  
Water depth : 197 m  
Total depth : 2600 m  
Objective : Jurassic sanstone  
Status : Plugged and abandonned

TEST REPORT 34/10-4

CONTENTS:

PAGE :

1. INTRODUCTION	1-1
2. OBJECTIVES	2-1
3. CONCLUSIONS	3-1
4. DISCUSSION	4-1
4.1 DST analysis	4-1
4.2 Sand test	4-2
4.3 Deliverability during the sand test	4-2
4.4 RFT analysis	4-2
4.5 Reservoir temperature	4-3
4.6 Reservoir fluid	4-3

APPENDICES

A1 DST no. 1A	A1-1
Analysis of DST no. 1A	A1-2
Rate data	A1-9
Perforation and test string	A1-10
Separator and bottom hole sampling	A1-12
Test sequence	A1-13
A2 DST no. 2	A2-1
Analysis of DST no. 2	A2-2
Analysis of deliverability during DST no. 2	A2-9
Rate data	A2-13
Perforation and test string	A2-14
Separator and bottom hole sampling	A2-16
Test sequence	A2-17
A3 RFT data and analysis	A3-1
A4 Reservoir temperature	A4-1
A5 Summary log well 34/10-4	A5-1

## 1. INTRODUCTION

34/10-4 is the third well drilled in the Delta structure in block 34/10. The well penetrated the Etive , Rannoch and Broom members of Brent formation and reached a depth of 2600 m RKB. (The Brent formation is a delta deposition of Jurassic age). The testing of the two previous wells indicated high productivity and good reservoir characteristics. But the data collected and analyzed indicate uncertainty owing to:

- wide spread in the results from PVT-analysis.
- probable variation in fluid properties with depth.
- problems with sand production.

## 2. OBJECTIVES

The purpose of testing 34/10-4 were therefore to:

- get an indication in the variations of fluid properties with depth by perforating two intervals one at the top and one at the bottom of the Rannoch facies
- investigate sand production and strength in more details. (In this facies with good reservoir properties this is done by perforating a short interval (2 m) to get a high production pr. perforation).

## 3. CONCLUSIONS

1. Well 34/10-4 can be considered as a high capacity well. The permeability thickness varies between 220 000 and 340 000 md-ft. This results in a permeability range of 850 to 1300 md. These values also correlate well with the measured core permeabilities.
2. The three "tight zones" in Rannoch formation seem not to be continuous. The permeability thickness calculated from the two drill stem tests (DST 1 at the bottom and DST 2 at the top) represent the total permeability thickness in the Rannoch formation.
3. The skin values calculated are mainly dominated by skin due to partial penetration. Small completion ratios make it difficult to separate true formation damage from the effect of partial penetration.
4. The pressure at -1800 m ss in Rannoch formation is estimated to 4428 psig or 306.3 bar. The gradient is estimated to 0.32 psi/ft or 0.072 bar/m. Indicating only a +-2 psi difference between the RFT data and the pressures obtained from the DST analysis.
5. The "sand test" during DST no. 2 was negative. Rannoch formation produced without sand at a rate of 2500 BOPD/m perforations or 3200 res. bbl/D/m perforations.
6. The sand test was analysed as a deliverability test and indicated non Darcy flow with an IT flow factor (D) of  $2.70 \times 10^{-3}$  STBPD $^{-1}$ . At a rate of 4050 STB/D the skin due to turbulence was approximately + 11. The magnitude of this turbulence factor is probably due to the small completion ratio.
7. Samples show a uniform reservoir hydrocarbon system through the Rannoch formation.

8. The maximum temperature recorded during DST no. 1 was  $72.4^{\circ}\text{C}$  or  $162.3^{\circ}\text{F}$  and  $71.5^{\circ}\text{C}$  or  $160.7^{\circ}\text{F}$  during DST no. 2.
9. No water was produced.

#### 4. DISCUSSION

##### 4.1 DST analysis

Two drill stem tests were run in well 34/10-4 and both in the Rannoch formation (1821 m RKB - 1905m RKB). DST no. 1 was run at the bottom (1880 m RKB - 1885 m RKB) and DST no. 2 was run at the top (1824 m RKB - 1826 m RKB).

In the middle of the Rannoch formation the summary log indicated three "tight zones" with a measured core permeability of 2 md. The two DST analysis indicated a permeability of 850 - 1300 md by using the net pay thickness of the formation. These values corresponds well with the measured horizontal core permeabilities. The calculated permeability thickness must therefore represent the total zone and indicating that tight zones is probably not continuous. (A summary log for well 34/10-4 can be found in the appendix A5).

The skin values calculated was high and are mainly caused by the small completion ratios. In this report no attempt was made to separate formation damage from the effect due partial penetration. Since the completion ratios are small, it is difficult to separate skin due to partial penetration by the commenly used methodes.

A reduced production time was used in the DST analysis. Cummulative production was calculated from the latest average pressure stabilization prior to the analyzed pressure build up.

A thickness of 79 m, an average porosity of 32.7% and a water saturation of 12.7% was used for both DST no. 1 and DST no. 2. These values are taken from the Petrophysical evaluation for this well. PVT Properties were taken from the Core lab. report RFLA 79192 based on a sample taken during DST no. 2. The Lynes gauge no. 1054 was used in the analysis for both DST's. The individual DST analysis, test sequence and rate data etc. can be found in the appendix A1 and A2.

#### 4.2 Sand test

The intention of DST no. 2 was besides of collecting fluid samples to increase the flow rate in steps by changing choke size to obtain a critical rate/drawdown for sand production or until a rate of 5000 STB/D was reached.

During this test the flow rate did not reach the critical level for total failure of the sand. It was observed no sand slug production to the surface.

Therefore it could be concluded that wells from this formation (Rannoch members of Brent) will probably produce sand free at 2500 BOPD/m perforations (3200 res. bbl/D/m perf.) or 230 BOPD/perf. (290 res. bbl/perf.) if 11 of 13 perforations are open for each perforated meter. This rate corresponds to a drawdown of approx. 260 psi.

#### 4.3 Deliverability during the sand test.

The data collected during the sand test was analyzed as an flow after flow test. Both rate and bottom hole pressure stabilized quickly and therefore pseudo-steady state flow was assumed. The laminar - inertial - turbulent (LIT) flow equation was used in the calculations. At a rate of 4050 STBPD the skin factor due to turbulence was calculated to +11 and the IT flow factor (D) was calculated to  $2.70 \times 10^{-3}$  (STBPD) $^{-1}$ . Only a small interval was perforated during the sand test (2 m) and the rate per meter perforations was high (3200 res. bbl/D/m perforations). This gave a high fluid velocity close to the wellbore and probably led to turbulence in this region. At larger completion ratios the turbulence will probably be minimized.

The analysis of this sand test can be found in appendix A2.

#### 4.4 RFT analysis

The repeat formation tester was run in the Brent formation and good data was obtained from 1906.5 m RKB to 1821.5 m RKB. The data was corrected +26 psi due to temperature and pressure.

The RFT data and the pressures obtained from the DST analysis compare perfectly. (+-2 psi difference).

A gradient of 0.32 psi/ft or 0.072 bar/m and a pressure of 4428 psig or 306.3 bar at 1800 m ss has been estimated in the Rannoch formation.

The RFT pressures from this well also compare excellent with other wells located on this structure in the Brent formation (34/10-1, 3, 5, 6, 7, 8, 9). There is approximately +-12 psi range between the RFT pressures from the different wells in the Brent formation.

The RFT data and analysis can be found in appendix A3.

#### 4.5 Reservoir temperature

A maximum bottom hole temperature of about  $72^{\circ}\text{C}$  ( $162^{\circ}\text{F}$ ) was recorded in both tests. This value are within the range  $68\text{--}77^{\circ}\text{C}$  ( $155\text{--}170^{\circ}\text{F}$ ) of the temperature measurements in 34/10-1 and 34/10-3, but they are scattered and it is difficult to draw a correct line in the temp. vs. depth plot.

A plott of the measured reservoir temperature vs. depth from wells 34/10-1, 3 and 4 can be found in appendix A4.

#### 4.6 Reservoir fluid

In order to obtain good information about the properties of the reservoir fluid in 34/10-4, four bottom hole samples from DST no. 1 and three from DST no. 2 were analyzed by Statoil Production Laboratory. For this well the bubble point, GOR and  $B_o$  lay nearest to the mean of all the samples. The variation in composition are only slight and well within the error limits of the analysis. The samples show a uniform reservoir hydrocarbon system throughout the Rannoch.

APPENDIX A1

DST no. 1A

## BOTTOM HOLE PRESSURE REPORT

Well 34/10-4Test no. DST no. 1ATest Date 5.10.79-7.10-79Date of analysis 29.7.79Gauge no. 1054

## SUMMARY OF THE RESULTS

	Semilog Analysis	Type Curve Analysis
$Kh \text{ md} \cdot \text{ft}$	221538	
$K \text{ md}$	855	
$S$	+ 175	
$\bar{P} \text{ (psia) at } -1832.3 \text{ mss}$	4478	

Max recorded Temp. 72.4°C (162.3°F)Remarks


Signature

Well 34/10-4 DST#1ATest date 5.10.79-7.10.79Reservoir ParametersPerforations 1880-1885m RKBZone(s) Rannoch (Brent)Wellbore radius 0.35 feetRKB Elev 25mMidpoint Production -1857.5m ss Bomb at 1857.3m RKB - 1832.3m ss

Pressure Functions Evaluated at — ss Datum Depth — ss

Delta P required to correct to datum \_\_\_\_\_ psig Gradient \_\_\_\_\_ psi/ft

Estimated Average Pressure 4478 psiaFormation Volume Factor 1.253 vol/vol Viscosity 1.21 cpThickness 79m Porosity 32.7 % Drainage Area — acresOil Saturation 87.7 % Oil Compressibility 8.37  $\times 10^{-6}$  psi<sup>-1</sup>Water Saturation 12.3 % Water Compressibility 3.0  $\times 10^{-6}$  psi<sup>-1</sup>Gas Saturation — % Gas Compressibility —  $\times 10^{-6}$  psi<sup>-1</sup>Formation Compressibility 3.0  $\times 10^{-6}$  psi<sup>-1</sup>System Compressibility  $C_t = S_0 C_0 + S_w C_w + S_g C_g + C_f$ 

$$C_t = 0.877 \times 8.37 \times 10^{-6} + 0.123 \times 3.0 \times 10^{-6} + - \times - \times 10^{-6} + 3.0 \times 10^{-6}$$

$$C_t = 10.7 \times 10^{-6} \text{ psi}^{-1}$$

Rates Reported on Test.Choke 20 / 64 inches Oil Rate 1800 STBPD Gas Rate 0.920 MMSCFDFTP \_\_\_\_\_ psig Water Rate 0 BWD GOR 510 SCF/STB

0 API \_\_\_\_\_ Gas Spec. Grav. \_\_\_\_\_

Cumulative Production \* Oil 166.25 STB Gas \_\_\_\_\_

Water \_\_\_\_\_

\* Cumulative production from 6.10.79 at 952 to 1205.

Well 34/10-4 DST#1ATest Date 5.10.79 - 7.10.79Horner AnalysisEffective Production Time  $t_p$  = Cumulative Production / Rate Reported on Test.

$$t_p = \frac{166.25}{1800 \times 24 \times 10} = 133 \text{ min}$$

Straight line starts at 25 min Slope 2.003 psi/cycle

$$P_{wf's} = 4160.7 \text{ psia}$$

$$P_{1hr} = 4477.1 \text{ psia}$$

$$P^* = 4478.1 \text{ psia}$$

Calculated Values

$$K_h = \frac{162.6 \text{ O Bu}}{M} = \frac{162.6 (1800)(1.253)(1.21)}{2.003} = 221538 \text{ md.ft}$$

$$K = K_h/h = \frac{221538}{[(79)(3.281)]} = 855 \text{ md.}$$

$$S = 1.1513 \left[ \frac{P_{1hr} - P_{wf's}}{M} + \log \left[ \frac{t_p + 1}{t_p} \right] - \log \left[ \frac{K}{\phi \mu C_t r_w^2} \right] + 3.2275 \right]$$

$$S = 1.1513 \left[ \frac{4477.1 - 4160.7}{2.003} + \log \left[ \frac{133 + 60}{133} \right] - \log \left[ \frac{855}{(1.327)(1.21)(10.7 \times 10^{-6})(.35)^2} \right] + 3.2275 \right]$$

$$S = +175$$

$$t_{DA} = \frac{0.000264 K t}{\phi \mu C_t A} = \frac{0.000264}{0.000264} =$$

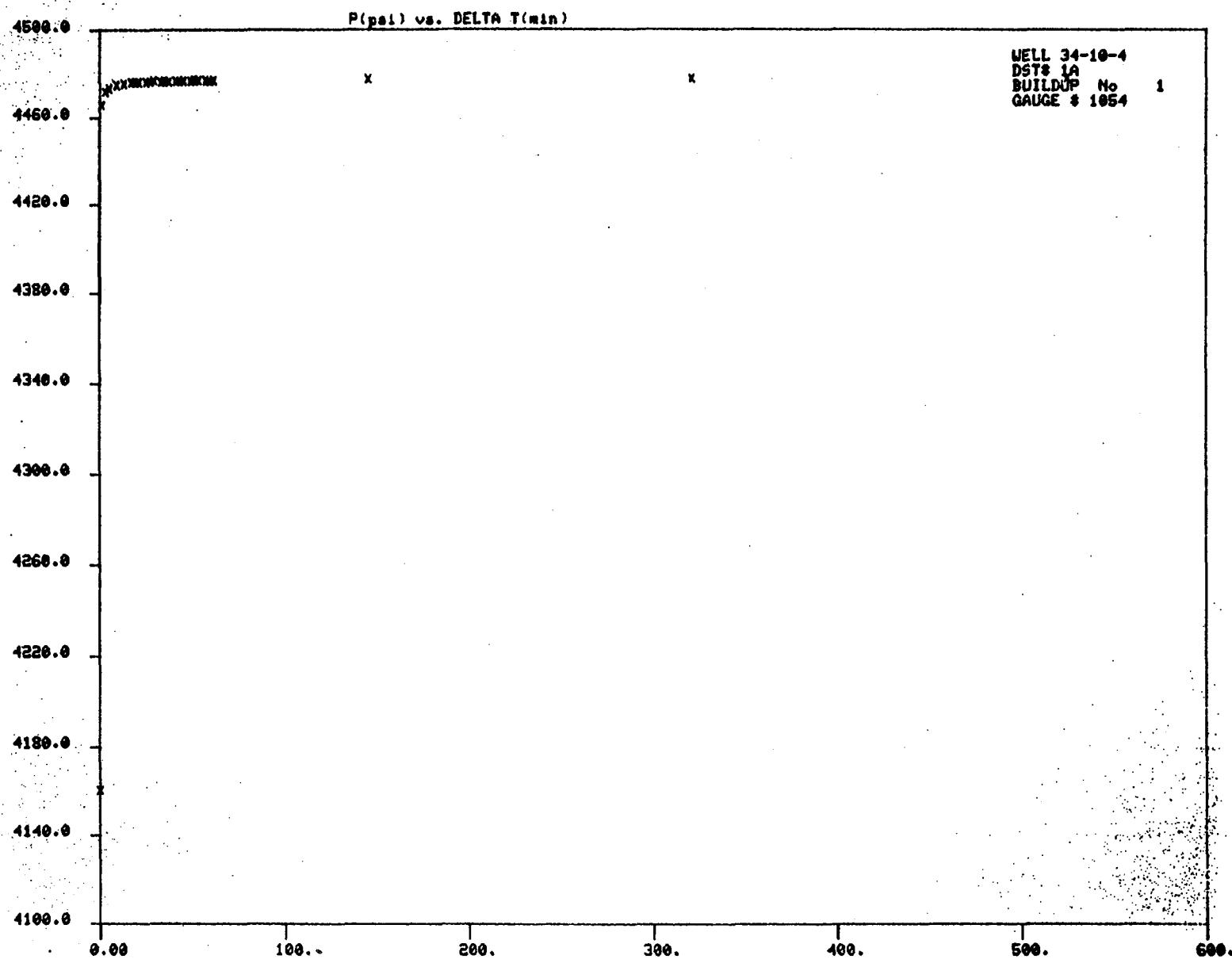
$$P_{DMBH} = 0$$

$$\bar{P} = P^* - P_{DMBH} \left[ \frac{M}{2.303} \right] = 4478 \text{ psia} @ - 1832.3 \text{ m ss}$$

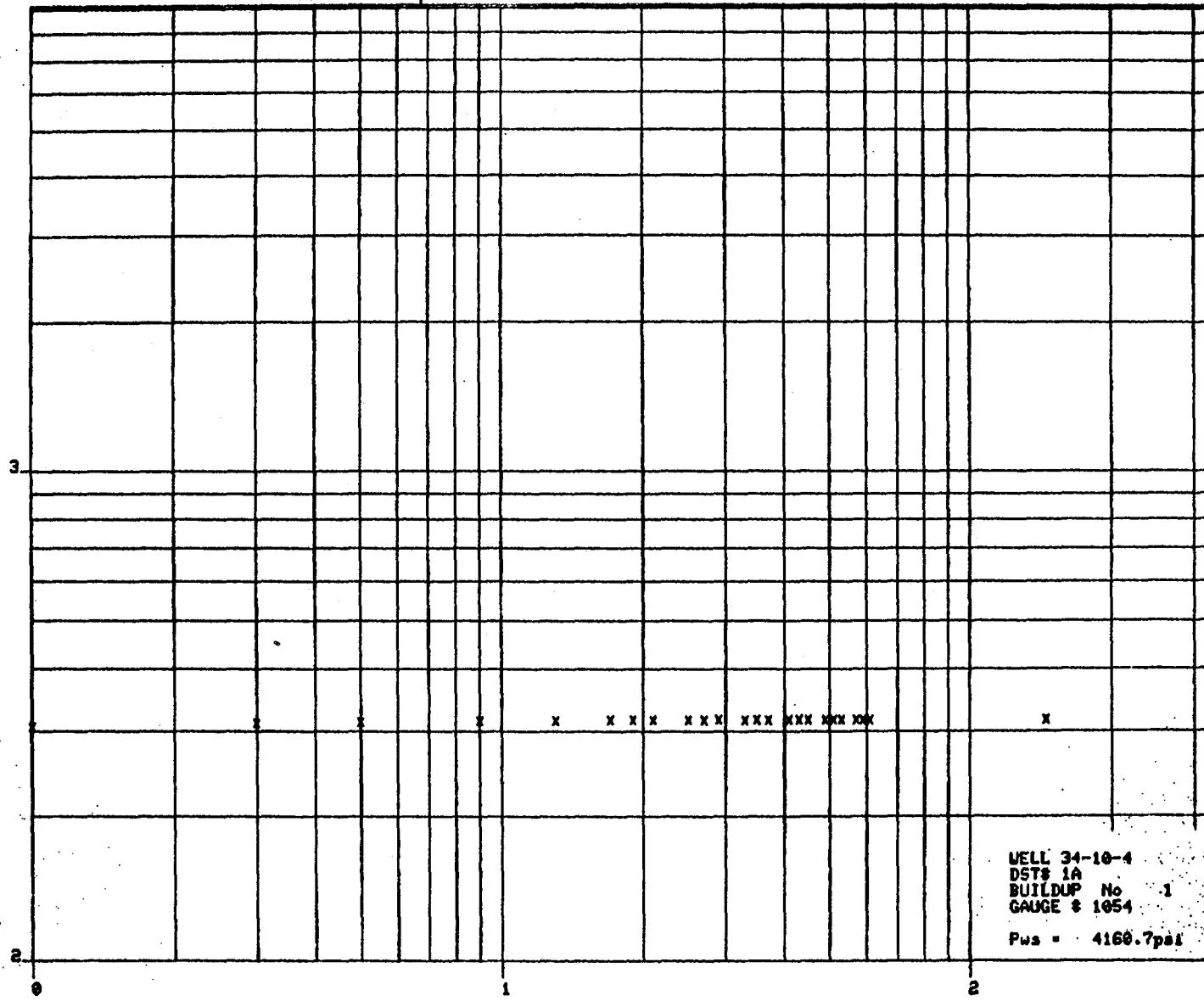
= \_\_\_\_\_ @ - \_\_\_\_\_ ss Datum

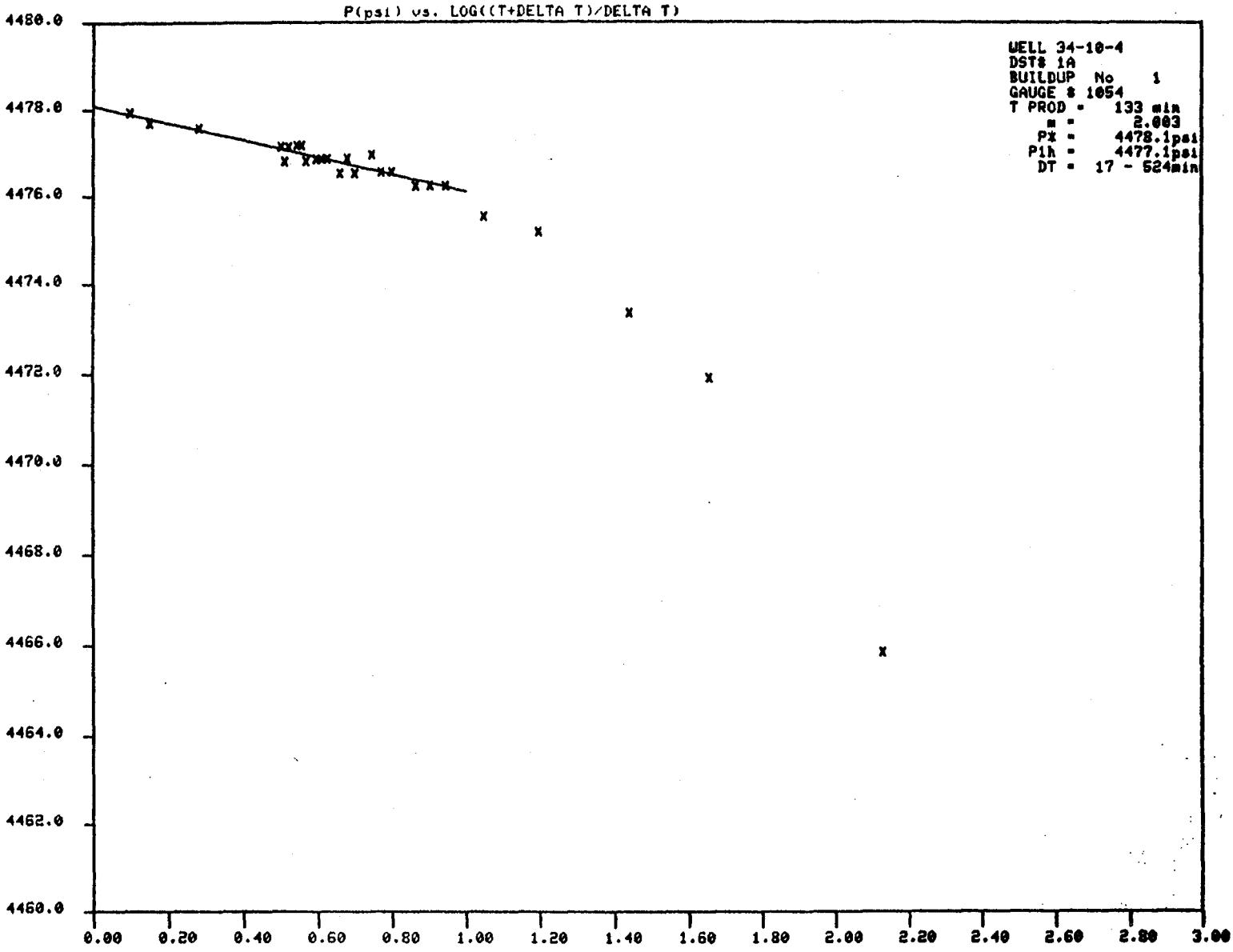
BRÖNN 34-10-4 DST# 1  
BUILDUP NUMBER 1  
GAUGE 1054

NR.	TID	TRYKK
1	0.00	4160.700
2	1.00	4465.880
3	3.00	4471.930
4	5.00	4473.360
5	9.00	4475.170
6	13.00	4475.520
7	17.00	4476.230
8	19.00	4476.230
9	21.00	4476.230
10	25.00	4476.550
11	27.00	4476.550
12	29.00	4476.950
13	33.00	4476.520
14	35.00	4476.870
15	37.00	4476.520
16	41.00	4476.860
17	43.00	4476.860
18	45.00	4476.860
19	49.00	4476.810
20	51.00	4477.170
21	53.00	4477.170
22	57.00	4477.140
23	59.00	4476.800
24	61.00	4477.140
25	145.00	4477.580
26	321.00	4477.700
27	525.00	4477.950



LOG(DELTA P(psi)) vs. LOG(DELTA T(min))





FLOWRATES FROM WELL 34/10-4 DST No. 1A.  
(main flow periods)

<u>Date</u>	<u>Time</u>	<u>Choke (1/64")</u>	<u>Qo (STB/D)</u>	<u>Qy (MMSCF/D)</u>	<u>GOR (SCF/STB)</u>
5/10	18.01-23.34	20	1750	.860	490
6/10	09.52-12.05	20	1800	.920	510

SHEET A: PERFORATION AND TEST STRING

Well no. 34/10-4    DST no. 1A    Date: 5/10

Test engineer in charge: J. Hanstveit

1. Perforated interval: 1880-1885 m Ref. ISF/SONIC
2. Casing size: 7 in 29 lb/ft N-80
3. Depth to top plug (before test): 1930 m  
Tagged bottom at (after test): 1926 m
4. Type of test string: TDS, 3½ in
5. Volume calculations:  
 Volume STT - circ.valve : 6.60 m<sup>3</sup> (41.5 bbl)  
 Volume STT - tester valve (cushion) : 6.76 m<sup>3</sup> (42.5 bbl)  
 Volume tester valve - lowest perf. (rathole): 0.62 m<sup>3</sup> (3.9 bbl)
6. Type of cushion: \_\_\_\_\_ Density: 0.998 g/cc
7. Pressure gauges:

Type	Gauge no	Press.range	Depth	Ran on	Remarks
DMR314	1054	0-5000 psi	1857.25	STRING	7+34h
DMR314	1209	0-5000 psi	1858.75	"	7+68h
DMR312	1092	0-10000 psi	1860.65	"	7+68h
RPG-3	11652N	0-5500 psi	1867.05	"	72h
RPG-3	9058	0-8200 psi	1868.93	"	72h
RPG-3	32328	0-10000 psi	1870.73	"	120h

## Temperature gauges:

Type	Gauge no.	Temp.range	Depth	Ran on	Remarks
Lynes	1054,1209,1092				

Mud 1.85 g/cc

\* Drillers depth, Tagged 8/10

Sam depth, Tagged 4/10. report no. 55

Test string, DST No. 1APerf. interval: 1880-1885 m RKB

Description	ID inch	OD inch	Length m	Depth m RKB
OTIS STT	2.66			
3½ TDS Tubing above RKB	2.75	3.5	5.78	
3½ TDS Tubing below RKB	2.75	3.5	12.90	12.90
OTIS Lubricator Valve	2.88	13.38	2.21	15.11
3½ TDS Tubing (22 jts.)	2.75	3.5	199.12	214.23
OTIS SSTT + x-overs	1.98	13.38	6.17	220.40
3½ TDS Tubing (153 jts.)	2.75	3.5	1373.75	1594.15
x-over	2.38	5.55	.17	1594.32
Slip Joint (open)	2.25	5.00	5.54	1599.86
Slip Joint (closed)	2.25	5.00	4.02	1603.88
6 stds. Drill Collars	2.25	4.75	171.30	1775.18
x-over	2.375	4.75	.24	1775.42
RTTS Circulating Valve	2.44	4.62	.87	1776.29
x-over	2.55	4.75	.21	1776.50
1 std. Drill Collar	2.25	4.75	28.55	1805.05
Slip Joint (closed)	2.25	5.00	4.02	1809.07
Slip Joint (closed)	2.25	5.00	4.02	1813.09
1 std. Drill Collar	2.25	4.75	28.55	1841.64
APR-A Reversing Valve	2.25	5.00	.92	1842.56
APR-N Tester Valve	2.25	5.00	3.89	1846.45
Big John Jars	2.37	4.63	1.57	1848.02
RTTS Circulating Valve	2.44	4.62	.87	1848.89
RTTS Safety Joint	2.44	4.87	.84	1849.73
RTTS Packer above	2.185	5.75	.51	1850.24
RTTS Packer below	2.185	5.75	.82	1851.06
2 7/8 EUE Pup Joint	2.25	2.875	1.14	1852.20
Sand Screen (0.1 gauge)	2.25	3.5	2.89	1855.09
XN Nipple w/x-overs	2.375	1.79	.9	1855.99
2 7/8 Tubing (2 jts.)	2.25	2.875	18.9	1874.88
Bull Plug				

SHEET D: SEPARATOR AND BOTTOM HOLE SAMPLING

Well no. 34/10-4

DST no. 1A

Date: 5.10.79

1. Separator samples

Bottle no.	Oil/gas	Time	Oil rate	Gas rate
22400-104	oil	21.45- 22.20	1750/STB/D	0.86 MMSCF/D
A 10494	gas	"		
22400-107	oil	22.35- 23.10	"	"
A10488	gas	"		

2. Bottom hole samples

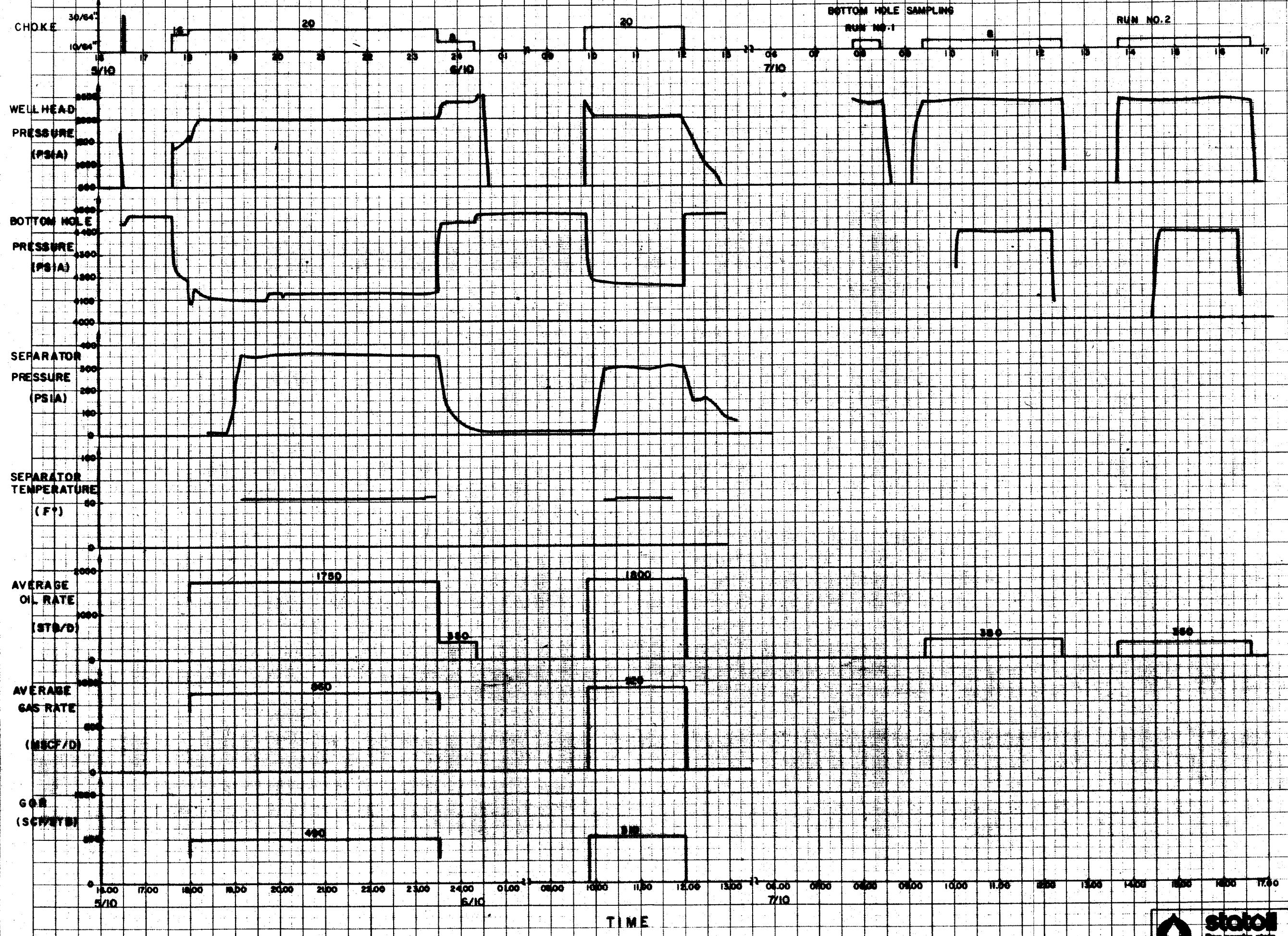
Bottle no.	Sampling depth	Sampling pressure	Operating pressure	Transfer BPP	True BPP (lab)
22024-68	1798 m RKB	4391	2180 @ 52°	2930 @ 54	
73FA230-26	"	"	2040 @ 55	2940 @ 54°	
22024-73	"	"	2120 @ 54°	2950 @ 54°	
2657/30	"	"	2120 @ 54°	2950 @ 54°	

Test sequence, DST No. 1A.

Date	Time	Operations
2/10	13.00-18.00 (5 hrs.)	Ran Schlumberger perforation guns and perforated 1880-1885 m RKB
2-3/10	18.00-18.00 (24 hrs.)	RIH w/teststring. Unable to get through the liner due to a too large outer diameter on the x-over between the top slip joint and the tubing. DST No. 1-a misrun.
3-5/10	18.00-16.29 (46 hrs)	RIH w/teststring. Pressure tested string, test equipment and surface lines. Unable to open APR-N valve. Had to POOH w/teststring. Made a new RIH after circulated bottoms up. Pressure tested again.
5/10	16.29	Opened APR-N tester valve.
	16.35-16.37 (2 mins)	Opened well on 32/64" fixed choke for initial flow. Flowed 4.75 bbls to surge tank.
	16.37-17.37 (60 mins)	Closed APR-N tester valve and choke manifold for initial shut in.
	17.37	Opened APR-N tester valve
	17.39-18.01 (22 mins)	Opened well on 16/64" fixed choke for clean up. Flow directed to burner.
	18.01-23.34 (335 mins)	Flowed through 20/64" fixed choke. Mud and gas to surface after 7 mins. Flow directed through separator at 18.58 hrs. Estimated flow rate: 1750 STB/D

Date	Time	Operations
5-6/10	23.34-00.23 (49 mins.)	Flowed through 8/64" fixed choke. Flow directed through surge tank to measure rate for bottom hole sampling.
6/10	00.23-09.52 (9.5 hrs.)	The well closed in at choke manifold. Waited on the weather to run bottom hole samplers.
	09.52-12.05 (133 mins.)	Opened well on 20/64" fixed choke for 3 rd. flow periode. Flow directed through separator and at 10.45 hrs. from separator to surge tank. The surge tank bypassed at 11.50 hrs. Unable to ignite the burner. Estimated flow rate: 1800 STB/D.
6-7/10	12.05-07.49 (20 hrs.)	The well shut in at APR-N tester valve and choke manifold. Final build up. Waited on the weather.
7/10	07.49	Opened APR-N tester valve.
	07.54-13.46 (352 mins.)	Opened well on 8/64" choke for bottom hole sampling, run no. 1. Flowed approximately 380 STB/D to surge tank.
	13.46-16.41 (175 mins.)	Opened well on 8/64" choke for bottom hole sampling, run no. 2. Flowed approximately 350 STB/D to surge tank.
7-8/10	16.41-03.30	The well shut in at choke manifold and bullheaded. Reverse circulated and POOH with test string and retreived Amerada and Lynes recorders.

34/10-4, DST no. 1A



APPENDIX A2

DST No. 2

## BOTTOM HOLE PRESSURE REPORT

Well 34/10-4Test no. DST no. 2Test Date 10.10.79-13.10.79Date of analysis 29.7.79Gauge no. 1054

## SUMMARY OF THE RESULTS

	Semilog Analysis	Type Curve Analysis
$Kh \text{ md} \cdot \text{ft}$	337760	
$K \text{ md}$	1303	
$S$	+ 76	
$\bar{P} \text{ (psia) at } -1780.3 \text{ m ss}$	4420	

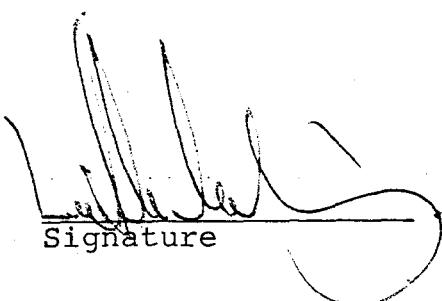
Max recorded Temp.  $71.5^{\circ}\text{C}$  ( $160.7^{\circ}\text{F}$ )Remarks

From deliverability analysis:

$$\bar{P}_r - P_{wf} = 43.1 \times 10^{-3} Q + 1.71 \times 10^{-6} Q^2$$

$$\text{IT flow factor } D = 2.70 \times 10^{-3} \text{ STBPD}^{-1}$$

$$\text{AOF} = 39780 \text{ STB/D}$$



Well 34/10-4 DST#2Test date 10.10.79 - 13.10.79Reservoir ParametersPerforations 1824-1826 m RKBZone(s) Rannoch (Brent)

ss

Wellbore radius 0.35 feet

RKB Elev

25mMidpoint Production - 1800 m ss Bomb at 1805.3 m RKB - 1780.3 m ss

Pressure Functions Evaluated at - \_\_\_\_\_ ss

Datum Depth - \_\_\_\_\_ ss

Delta P required to correct to datum \_\_\_\_\_ psig

Gradient \_\_\_\_\_ psi/ft

Estimated Average Pressure 4420 psiaFormation Volume Factor 1.253 vol/volViscosity 1.21 cpThickness 79.0 m Porosity 32.7 % Drainage Area - \_\_\_\_\_ acresOil Saturation 87.7 % Oil Compressibility 8.37  $\times 10^{-6}$  psi<sup>-1</sup>Water Saturation 12.3 % Water Compressibility 3.0  $\times 10^{-6}$  psi<sup>-1</sup>Gas Saturation - \_\_\_\_\_ % Gas Compressibility - \_\_\_\_\_  $10^{-6}$  psi<sup>-1</sup>Formation Compressibility 3.0  $\times 10^{-6}$  psi<sup>-1</sup>System Compressibility  $C_t = S_o C_o + S_w C_w + S_g C_g + C_f$ 

$$C_t = 0.877 \times 8.37 \times 10^{-6} + 0.123 \times 3.0 \times 10^{-6} + - \times - \times 10^{-6} + 3.0 \times 10^{-6}$$

$$C_t = 10.7 \times 10^{-6} \text{ psi}^{-1}$$

Rates Reported on Test.Choke 32 / 64 inches Oil Rate 4050 STBPD Gas Rate 1.990 MMSCFDFTP \_\_\_\_\_ psig Water Rate 0 BWD GOR 490 SCF/STB0 API 29° Gas Spec. Grav. \_\_\_\_\_Cumulative Production \* Oil 1013.26 STB Gas \_\_\_\_\_

Water \_\_\_\_\_

\* Cumulative production from 12.10.79 at 356 to 1256

Well 34/10 - 4 DST#2Test Date 10.10.79 - 13.10.79Horner AnalysisEffective Production Time  $t_p$  = Cumulative Production / Rate Reported on Test.

$$t_p = \frac{1013.2}{9 \text{ min.}} / \frac{(4050 \times 24 \times 60)}{360 \text{ min.}} = 360 \text{ min.}$$

Straight line starts at 9 min. Slope = 2.956 psi/cycle

$$P_{wf's} = 4204.7 \text{ psia}$$

$$P_{1hr} = 4417.2 \text{ psia}$$

$$P^* = 4419.7 \text{ psia}$$

Calculated Values

$$Kh = \frac{162.6 \text{ O Bu}}{M} = \frac{162.6 (4050)(1.253)(1.21)}{2.956} = 337760 \text{ md.ft}$$

$$K = Kh/h = \frac{337760}{(79 \times 3.281)} = 1303 \text{ md.}$$

$$S = 1.1513 \left[ \frac{P_{1hr} - P_{wf's}}{M} + \log \left[ \frac{t_p + 1}{t_p} \right] - \log \left[ \frac{K}{\phi \mu C_t r_w^2} \right] + 3.2275 \right]$$

$$S = 1.1513 \left[ \frac{4417.2 - 4204.7}{2.956} + \log \left[ \frac{360 + 60}{360} \right] - \log \left[ \frac{1303}{(0.327)(1.21)(10.7 \times 10^{-6})(0.35)^2} \right] + 3.2275 \right]$$

$$S = +76$$

$$t_{DA} = \frac{0.000264 K t}{\phi \mu C_t A} = \frac{0.000264}{=}$$

$$P_{DMBH} = 0$$

$$\bar{P} = P^* - P_{DMBH} \left[ \frac{M}{2.303} \right] = 4420 \text{ psia} @ = 1780.3 \text{ m ss}$$

$$= \text{psig} @ = \text{ss Datum}$$

BRØNN 34-10-4 DST# 2  
 BUILDUP NUMMER 1  
 GAUGE 1054

NR.	TID	TRYKK
1	0.00	4204.660
2	1.00	4408.410
3	3.00	4412.690
4	5.00	4414.100
5	9.00	4414.840
6	11.00	4415.190
7	13.00	4415.560
8	17.00	4415.890
9	19.00	4415.560
10	21.00	4415.890
11	25.00	4416.240
12	27.00	4416.240
13	29.00	4416.590
14	33.00	4416.230
15	35.00	4416.230
16	37.00	4416.230
17	41.00	4416.580
18	43.00	4416.930
19	45.00	4416.930
20	49.00	4416.580
21	51.00	4416.890
22	53.00	4416.890
23	77.00	4417.160
24	81.00	4417.160
25	83.00	4417.160
26	85.00	4417.160
27	97.00	4417.480
28	113.00	4417.800
29	153.00	4412.060
30	189.00	4412.000

4500.0

P(psi) vs. DELTA T(min)

4470.0

4440.0

4410.0

4380.0

4350.0

4320.0

4290.0

4260.0

4230.0

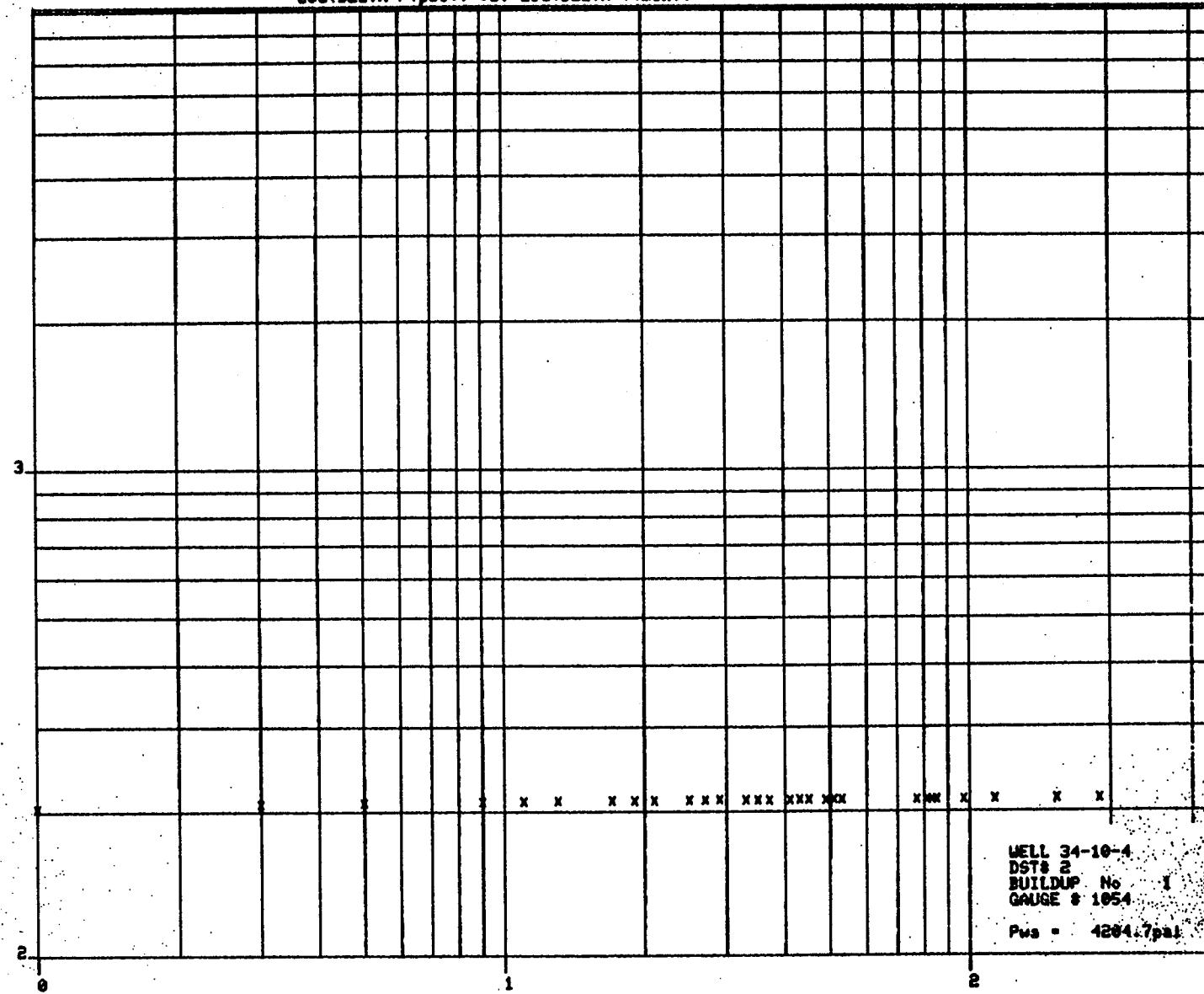
4200.0

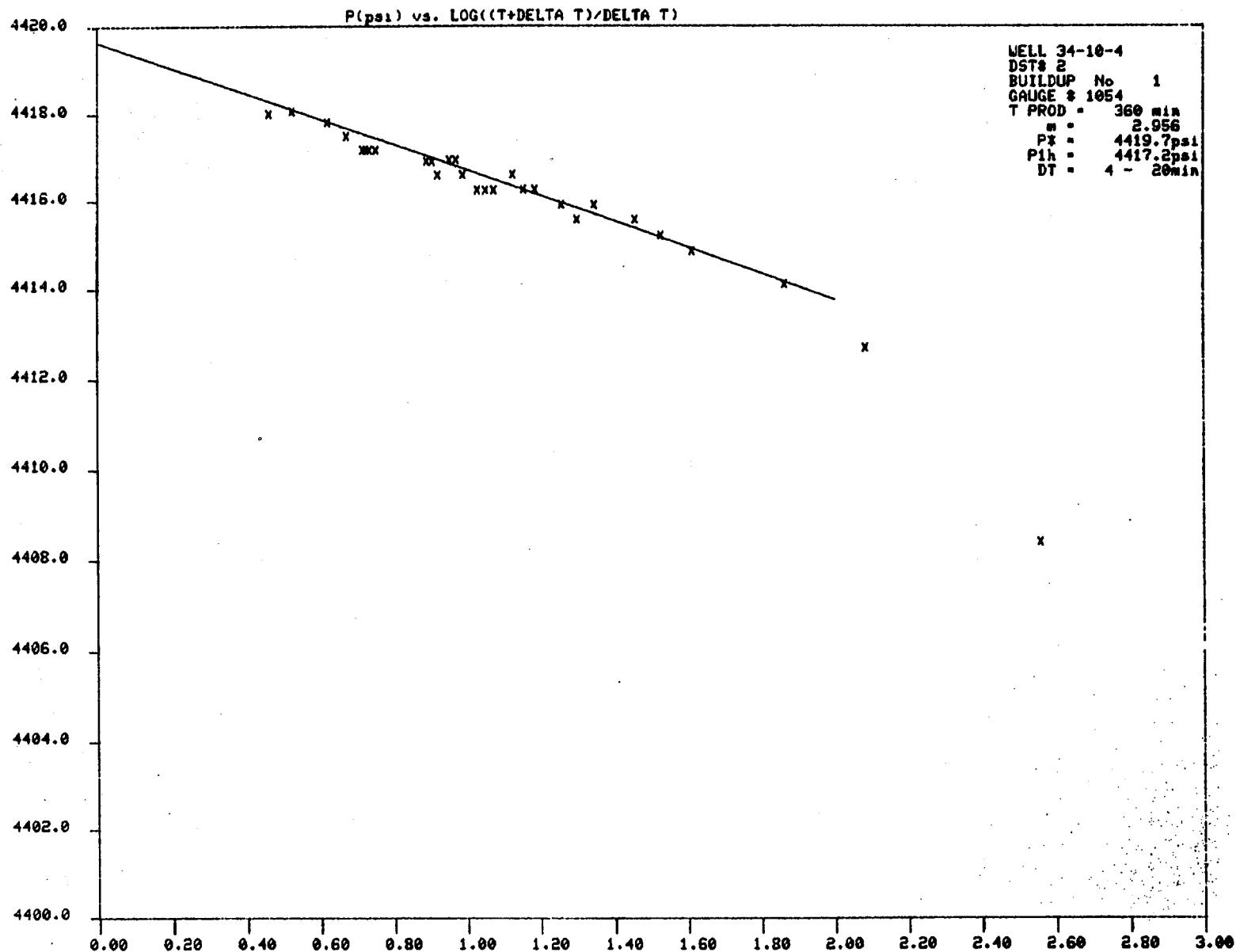
WELL 34-10-4  
DST# 2  
BUILDUP No 1  
GAUGE # 1054

0.00 10.00 20.00 30.00 40.00 50.00 60.00 70.00 80.00 90.00 100. 110. 120. 130. 140. 150. 160. 170. 180. 190. 200.

A2-6

LOG(DELTA P(psi)) vs. LOG(DELTA T(min))





Well 34/10-4 DST no 2Test Date 10.10.79DELIVERABILITY CALCULATIONS, LIT ANALYSIS

$$A = \frac{43.1 \times 10^{-3} \text{ psi}}{\text{STBPD}}$$

$$B = \frac{1.71 \times 10^{-6} \text{ psi}}{\text{STBPD}^2}$$

$$\bar{P}_R - P_{wf} = AQ + BQ^2$$

$$\bar{P}_R - P_{wf} = 43.1 \times 10^{-3} Q + 1.71 \times 10^{-6} Q^2$$

$$AOF = \frac{1}{2B} (-A + (A^2 + 4B\bar{P}_R)^{0.5})$$

$$AOF = \underline{39780 \text{ STBPD}}$$

$$D = \frac{Kh}{141.2 \mu_o B_o} B = \frac{337760}{(141.2)(1.21)(1.253)} 1.71 \times 10^{-6}$$

$$D = \underline{2.70 \times 10^{-3} \text{ STBPD}^{-1}}$$

DATA USED IN THE DELIVERABILITY ANALYSIS.

34/10-4 DST 2

$$P_i = 4419.7 \text{ psia}$$

TIME	CHOKE 1/64"	Qo STBPD	Pwf psia	$\Delta P$ psi	$\Delta P/Qo$ psi/STBPD
23.48-03.00	8	350	4404.5	15.2	43.4 $\times 10^{-3}$
04.07- 5.15	10+16	1800	4336.1	83.6	46.4 $\times 10^{-3}$
05.20-06.45	14+16	2280	4312.2	107.2	47.1 $\times 10^{-3}$
07.00-08.00	12+20	2850	4284.7	135.0	47.4 $\times 10^{-3}$
08.20-09.30	16+20	3280	4260.0	159.7	48.7 $\times 10^{-3}$
09.45-10.00	14+24	3530	4247.9	171.8	48.7 $\times 10^{-3}$
10.15-10.45	16+24	3710	4235.7	184.0	49.6 $\times 10^{-3}$
11.00-11.45	20+24	4020	4205.0	214.7	53.4 $\times 10^{-3}$
12.05-12.15	32	4050	4204.6	215.1	53.1 $\times 10^{-3}$
18.15-18.45	20	2100	4319.7	100.0	47.6 $\times 10^{-3}$
19.00-19.15	24	2750	4287.2	132.5	48.2 $\times 10^{-3}$
19.30-21.00	32	4150	4212.2	207.5	50.0 $\times 10^{-3}$
21.15-23.30	12+32	4300	4199.7	220.0	51.2 $\times 10^{-3}$
24.00-00.30	16+32	4610	4177.2	242.5	52.6 $\times 10^{-3}$
00.45-01.45	20+32	5100	4164.7	255.0	50.0 $\times 10^{-3}$

23.48-12.15 : Gauge no. 1054

18.15-01.45 : Gauge no. 1092 + 19.73 psi

Form A4  
 $\frac{\Delta P}{Q_0}$

50  
 $10^{-9}$

45  
 $10^{-9}$

40  
 $10^{-9}$

0

1000

2000

3000

4000

5000

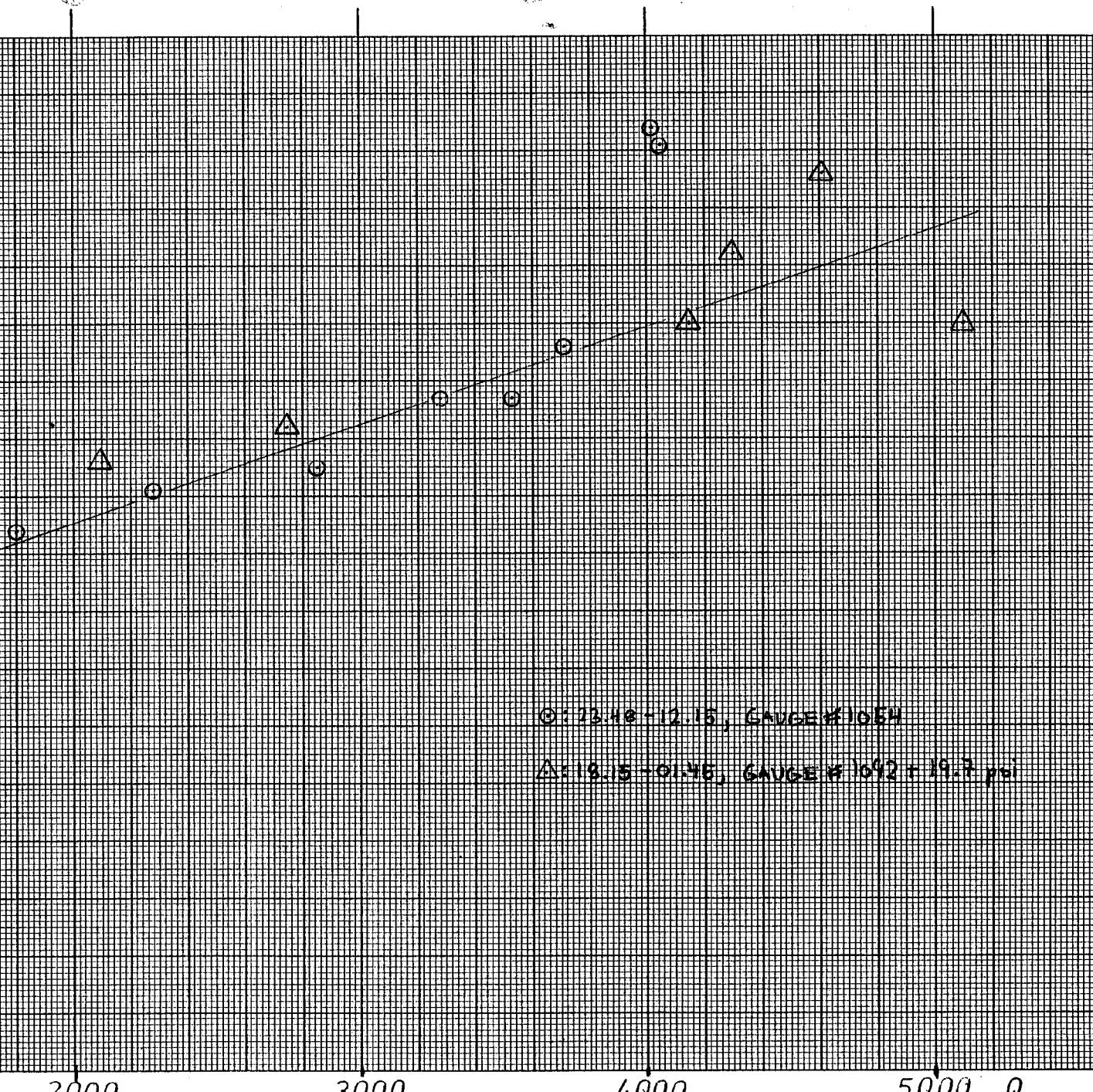
$Q_0$

A2-11

$$A = 43.1 \times 10^{-3} \text{ psi} / \text{deg}$$
$$B = 1.71 \times 10^{-6} \text{ psi}^2 / \text{deg}^2$$

○: 73.40 + 12.15, GAUGE #1064

△: 19.15 - 0.45, GAUGE #1092 + 19.7 psi



34110-4, DST NO.2

 $\Delta P$   
PSI

1000

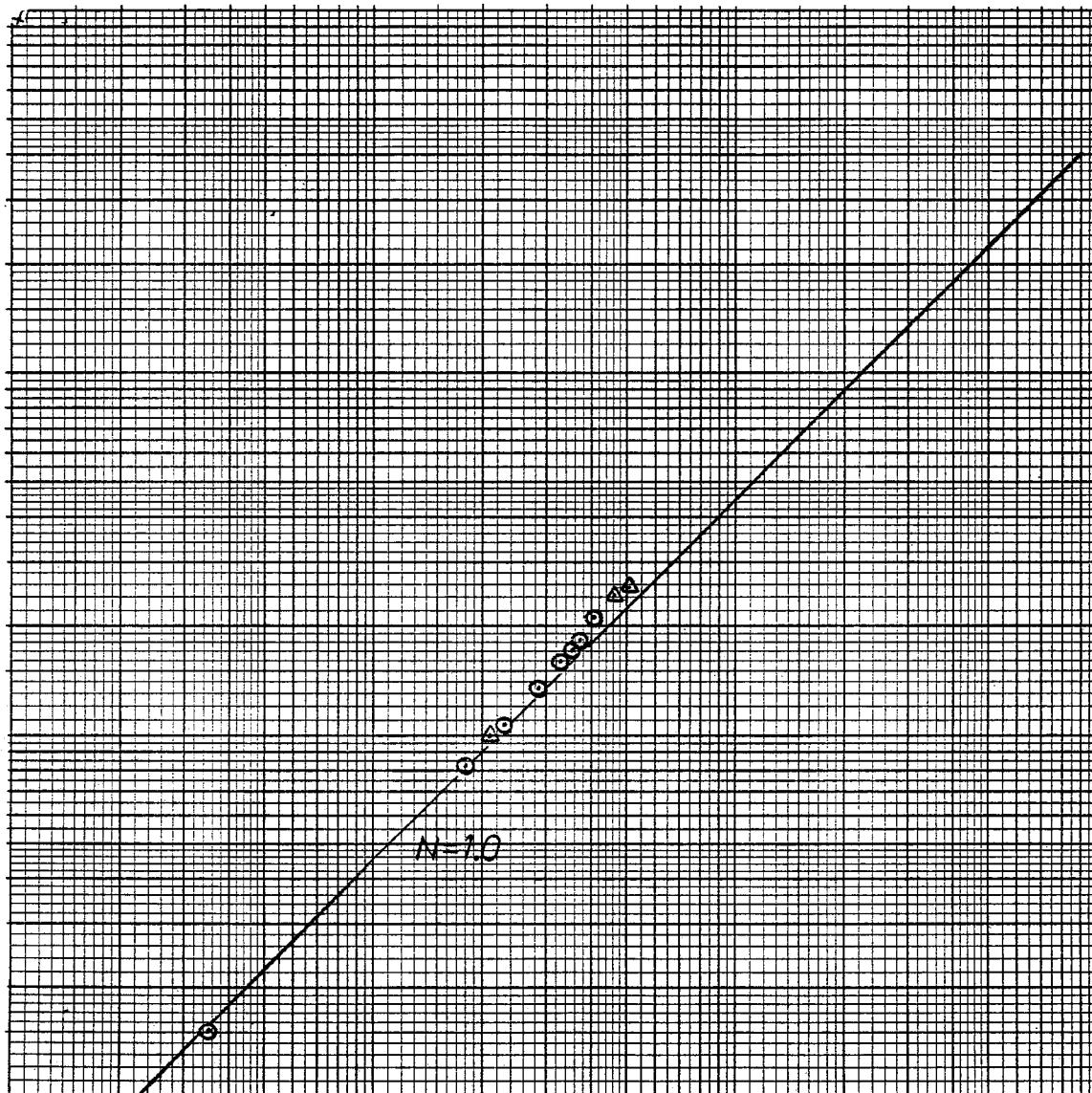
100

10

1000

10000

100000

 $Q_0$   
STBPD $N=1.0$ 

<u>Date</u>	<u>Time</u>	<u>Choke (1/64")</u>	<u>Qo (STB/D)</u>	<u>Qg (MMSCF/D)</u>	<u>GOR (SCF/STB)</u>
11/10	12.24-18.01	16	1250	.585	470
	19.21-22.15	8	365		
11-12/10	23.48-03.00	8	350		
12/10	04.07-05.15	10+16	1800	.775	430
	05.20-06.45	14+16	2280	.975	430
	07.00-08.00	12+20	2850	1.225	430
	08.20-09.30	16+20	3280	1.48	450
	09.45-10.00	14+24	3530	1.61	460
	10.15-10.45	16+24	3710	1.71	460
	11.00-11.45	20+24	4020	1.90	470
	12.05-12.15	32	4050	1.99	490
	18.15-18.45	20	2100	.975	460
	19.00-19.15	24	2750	1.26	460
	19.30-21.00	32	4150	1.85	450
	21.15-23.30	12+32	4300	2.04	470
13/10	24.00-00.30	16+32	4610	2.12	460
	00.45-01.45	20+32	5100	2.38	470

SHEET A: PERFORATION AND TEST STRING

Well no. 34/10-4 ; DST no. 2 Date: 10/10

Test engineer in charge: J. Hanstveit

1. Perforated interval: 1824-1826 m Ref. ISF/SONIC
2. Casing size: 7" in 29 lb/ft N-80
3. Depth to top plug (before test): 1832 m  
Tagged bottom at (after test): 1829 m
4. Type of test string: TDS, 3½ in
5. Volume calculations:  
 Volume STT - circ.valve : 6.42 m³ (40.37 bbl)  
 Volume STT - tester valve (cushion) : 6.60 m³ (41.50 bbl)  
 Volume tester valve - lowest perf. (rathole): 0.52 m³ (3.3 bbl)
6. Type of cushion: Density:
7. Pressure gauges:

Type	Gauge no.	Press.range	Depth	Ran on	Remarks
DMR314	1209	0-5000	1803.83	STRING	7+68h
DMR314	1054	0-5000	1805.33	"	7+34h
DMR312	1092	0-10000	1807.23	"	7+68h
RPG-3	11652N	0-5500	1813.63	"	72h
RPG-3	9058	0-8200	1815.51	"	72h
RPG-3	32328	0-10000	1817.31	"	120h

Temperature gauges:

Type	Gauge no.	Temp.range	Depth	Ran on	Remarks
Lynes	1209,1054and1092				

Test string, DST No. 2Perf. interval: 1824-1826 m RKB

Description	ID inch	OD inch	Length m	Depth m RKB
OTIS STT	2.66			
3½ TDS Tubing above RKB	2.75	3.50	5.40	
3½ TDS Tubing below RKB	2.75	3.50	13.28	13.28
OTIS Lubricator Valve	2.88	13.38	2.21	15.49
3½ TDS Tubing (22 jts.)	2.75	3.50	199.12	214.61
OTIS SSTM + x-overs	1.98	13.38	6.17	220.78
3½ TDS Tubing (147 jts.)	2.75	3.50	1321.70	1542.48
x-over	2.75	5.50	.17	1542.65
Slip joint (open)	2.25	5.00	5.54	1548.19
Slip joint (closed)	2.25	5.00	4.02	1552.21
6 stds. Drill Collar	2.25	4.75	171.30	1723.51
x-over	2.38	4.75	.24	1723.75
RTTS Circulating Valve	2.44	4.62	.87	1724.65
x-over	2.55	4.75	.21	1724.83
1 std. Drill Collar	2.25	4.75	28.55	1753.38
Slip joint (closed)	2.25	5.00	4.02	1757.40
Slip joint (closed)	2.25	5.00	4.02	1761.42
1 std. Drill Collar	2.25	4.75	28.55	1789.97
APR-A Reversing valve	2.25	5.00	.92	1790.89
APR-N Tester valve	2.25	5.00	3.89	1794.78
Big John Jars	2.37	4.63	1.57	1796.35
RTTS Circulating Valve	2.44	4.62	.87	1797.22
RTTS Safety Joint	2.44	4.87	.84	1798.06
RTTS Packer above	2.19	5.75	.51	1798.57
RTTS Packer below	2.19	5.75	.82	1799.39
Perforated 2 7/8 EUE Tubing	2.25	2.875	2.27	1801.66
OTIS XN-nipple + x-overs	1.79	2.375	.90	1802.56
2 jts. 2 7/8 EUE Tubing w/Bull Plug	2.25	2.875	18.9	1821.46

DST SUMMARY DATASHEET D: SEPARATOR AND BOTTOM HOLE SAMPLING

Well no. 34/10-4 DST no. 2 Date: 11/10-79

1. Separator samples

Bottle no.	Oil/gas	Time	Oil rate	Gas rate
2811-13	oil	13.45- 14.40	1250 STB/D	.585MMSCF/D
A10459	gas	"		
22461-14	oil	15.00- 15.45	"	"
A10483	gas	"		
20475-90	oil	16.15- 17.00	"	"
A10462	gas	"	"	"
22461-1	oil	17.10- 17.50		
A10477	gas	"	"	"

2. Bottom hole samples

Bottle no.	Sampling depth	Sampling pressure	Operating pressure	Transfer BPP	True BPP (lab)
22226-116	1737 m RKB	4346	2160	2880@54	
20475-62	"	"	2180	2880@55	
20475-66	"	"	2220	2880@57	
14068/66	"	"	2230	2880@57	

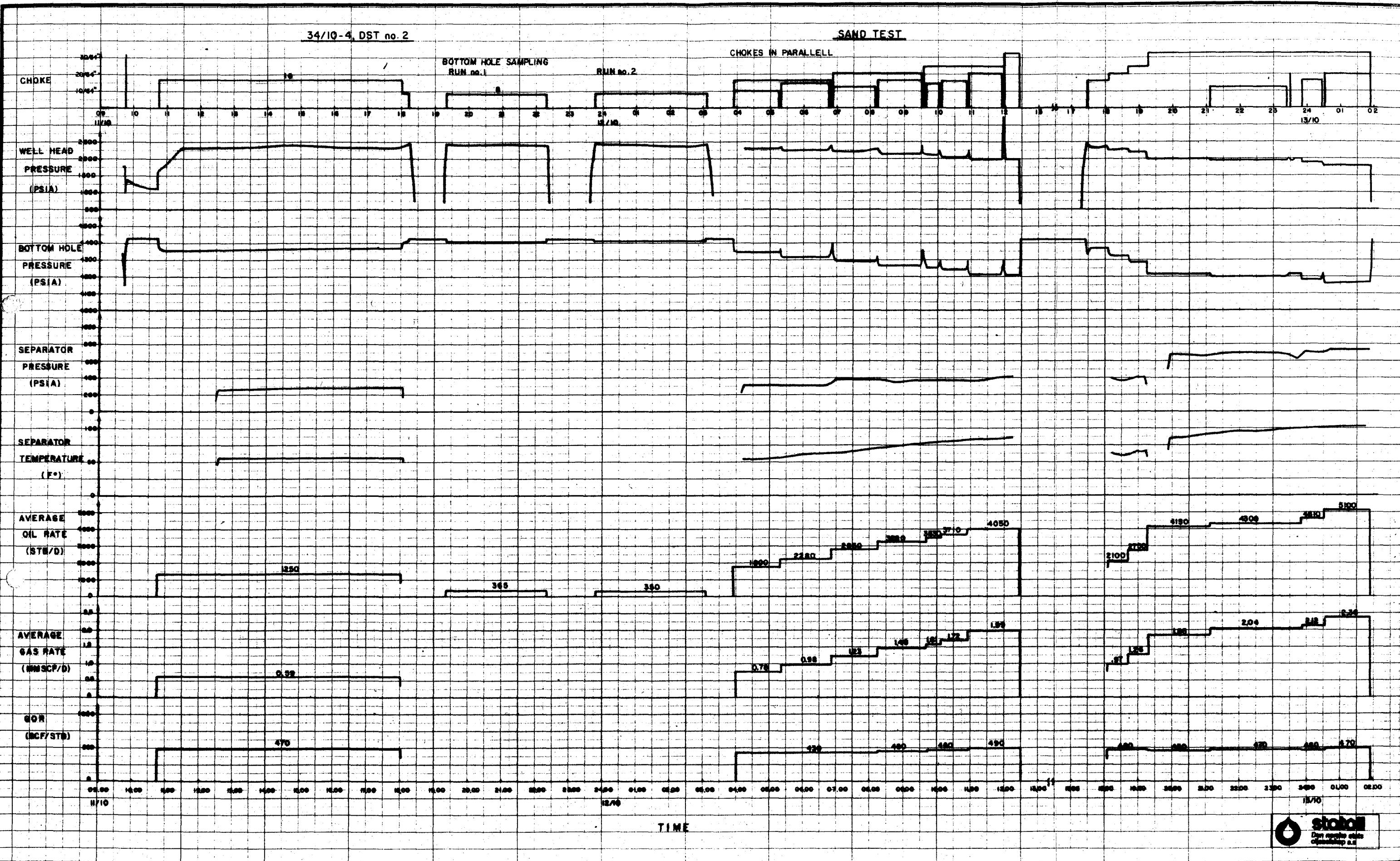
Test sequence, DST No. 2

Date	Time	Operations
10/10	20.45-21.55 (70 mins.)	Ran Schlumberger perforation guns and perforated 1824-1825 m RKB.
10-11/10	21.55-09.43 (12 hrs.)	RIH w/teststring and pressure recorders. Installed surface equipment and pressure testet string, surface lines and test equipment.
11/10	09.43	Opened APR-N tester valve.
	09.40-09.47 (1 min 25 sec.)	Opened well on 32/64" fixed choke for initial flow. Flowed 3.5 bbl to surge tank.
	09.47-10.44 (57 mins.)	Closed APR-N tester valve and choke manifold for initial shut in.
	10.44	Opened APR-N tester valve
	10.46-18.01 (435 mins.)	Opened well on 16/64" fixed choke for clean up. Flow directed through burner and at 12.24 hrs. through separator at an estimated rate of 1250 STB/D. Mud and gas to surface after 30 mins.
	18.01-18.14 (13 mins.)	Flowed through 8/64" choke to surge tank to measure rate for bottom hole sampling.
	18.14-19.21 (67 mins.)	Shut well in at choke manifold and prepared for bottom hole sampling, run no. 1.
	19.21-22.22 (181 mins.)	Opened well on 8/64" choke. Flowed surge tank at an estimated flow rate of 365 STB/D. BHS, run no. 1.
	22.22-23.49 (87 mins.)	Closed well at choke manifold and prepared for BHS, run no. 2.

Date	Time	Operations
11-12/10	23.49-03.07 (198 mins.)	Opened well on 8/63" choke. Flowed to surge tank at an estimated flow rate of 350 STB/D. BHS, run no. 2
12/10	03.07	The well closed at choke manifold.
	03.56-05.22 (86 mins.)	Opened well on 10+ 16/64" positive chokes in parallel for 3rd. flow period which is a test for sandproduction. Flow directed to burner at 04.03 hrs. through separator at an estimated rate of 1800 STB/D.
	05.22-06.55 (93 mins.)	Flowed through 14+ 16/64" chokes in parallel. Estimated flow rate: 2280 STB/D.
	06.55-08.16 (81 mins.)	Flowed through 12+ 20/64" chokes in parallel. Estimated flow rate: 2850 STB/D.
	08.16-09.41 (85 mins.)	Flowed through 16+ 20/64" chokes in parallel. Estimated flow rate: 3280 STB/D.
	09.41-10.09 (28 mins.)	Flowed through 14+ 24/64" chokes in parallel. Estimated flow rate: 3530 STB/D.
	10.09-10.57 (48 mins.)	Flowed through 16+ 25/64" chokes in parallel. Estimated flow rate: 3710 STB/D.
	10.57-12.01 (64 mins.)	Flowed through 20+ 24/64" chokes in parallel. Estimated flow rate: 4020 STB/D.
	12.01-12.26 (25 mins.)	Flowed through 32/64" choke. Estimated flow rate: 4050 STB/D.
	12.26-17.30 (304 mins.)	APR-N tester valve and choke manifold closed due to leak in chicksans. Final build up.
	17.31-18.08	Opened well on 16/64" choke for 4th. flow periode. Flow directed to burner.

Date	Time	Operations
	18.08-18.43	Flowed through 20/64" choke to separator at (35 mins.) an estimated rate of 2100 STB/D.
	18.43-19.19	Flowed through 24/64" choke. (36 mins.) Estimated flow rate: 2750 STB/D.
	19.19-21.09	Flowed through 32/64" choke. (50 mins.) Estimated flow rate: 4150 STB/D.
	21.09-23.53	Flowed through 12+ 32/64" chokes in parallel (104 mins.) Estimated flow rate: 4300 STB/D.
12-13/10	23.53-00.34	Flowed through 16+ 32/64" chokes in parallel (41 mins.) Estimated flow rate: 4610 STB/D.
13/10	00.34-01.56	Flowed through 20+ 32/64" chokes in parallel. (82 mins.) Estimated flow rate: 5100 STB/D. No sand produced.
	01.56-14.00	The well closed at choke manifold. The formation bullheaded, re. circulated and POOH with test string and all pressure recorders.

34/10-4, DST no.



## APPENDIX A3

## RFT DATA AND ANALYSIS, WELL 34/10-4

Pressure corrections,

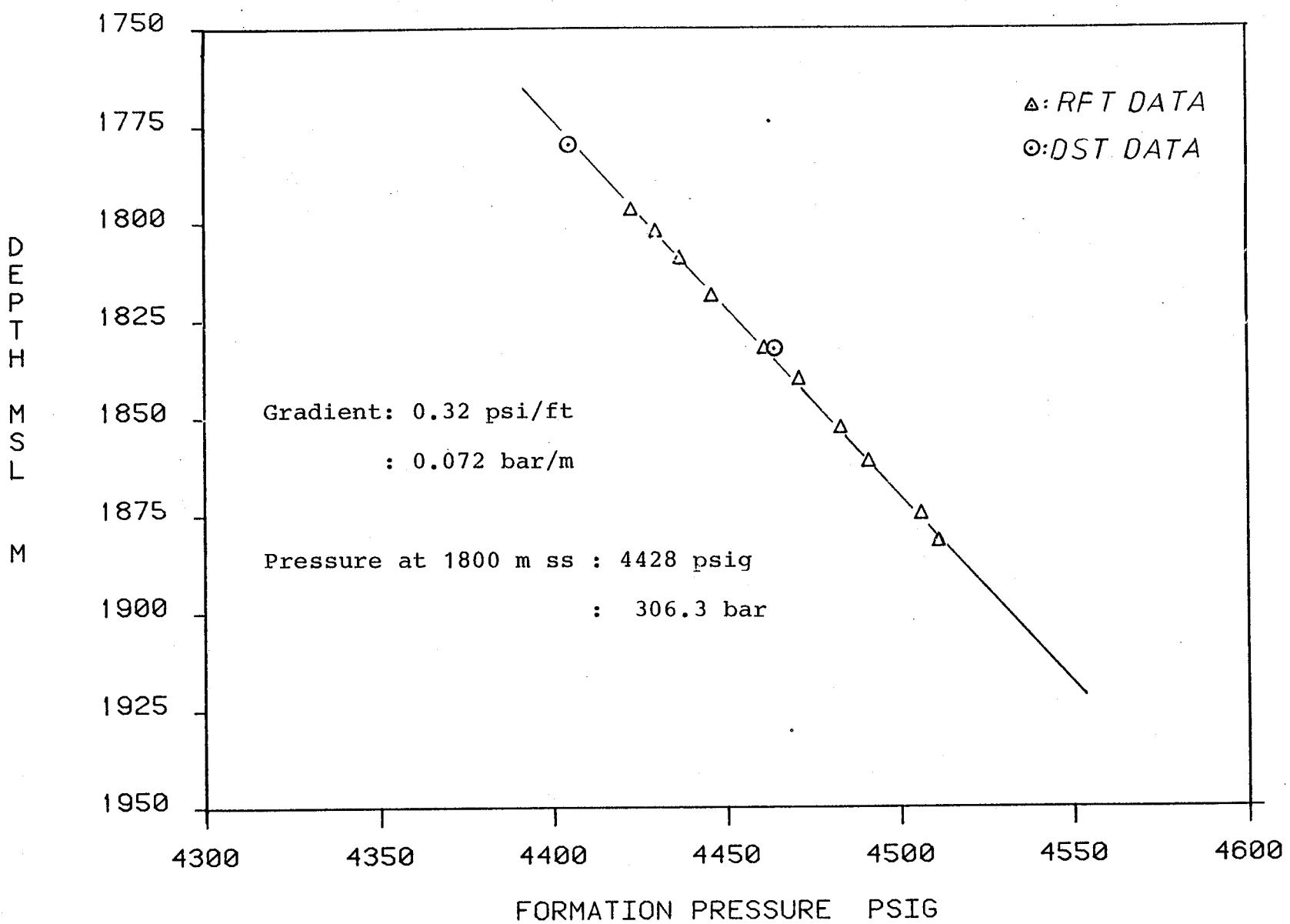
$$P_{TRUE} = P_{LOG} + \Delta P$$

From mastercalibration  $\Delta P = + 25$  psi

Sampling was not succesful due to seal failure.

Test no.	Depth (m ss)	Corr. Pressure (psig)
1	-1881.5	4511
2	-1874.5	4506
3	-1861.0	4491
4	-1852.5	4483
5	-1840.0	4471
6	-1832.0	4461
7	-1818.5	4446
8	-1809.0	4437
9	-1802.0	4430
10	-1796.5	4423
11	-1794.0	Seal failure
DST no. 1A	-1780.5	4405
DST no. 2	-1832.5	4463

RFT 34/10-4 BRENT



## APPENDIX A4

## 34/10 RESERVOIR TEMPERATURE

DEPTH

MSL

34/10-1

⊗ ●

Max. temp. recorded using:

X Sperry-Sun MRPG 6

O Lynes DMR 314

⊗ Sperry-Sun max. temp.

● GRC gauge

1800 34/10-4

DST 2

○

34/10-1

DST 2

⊗

1850

34/10-4

DST 1A

○

34/10-3

DST 3

X O

1900

34/10-3

DST 2

X O

1950

34/10-3

DST 1

X O

65

70

75

°C

150

160

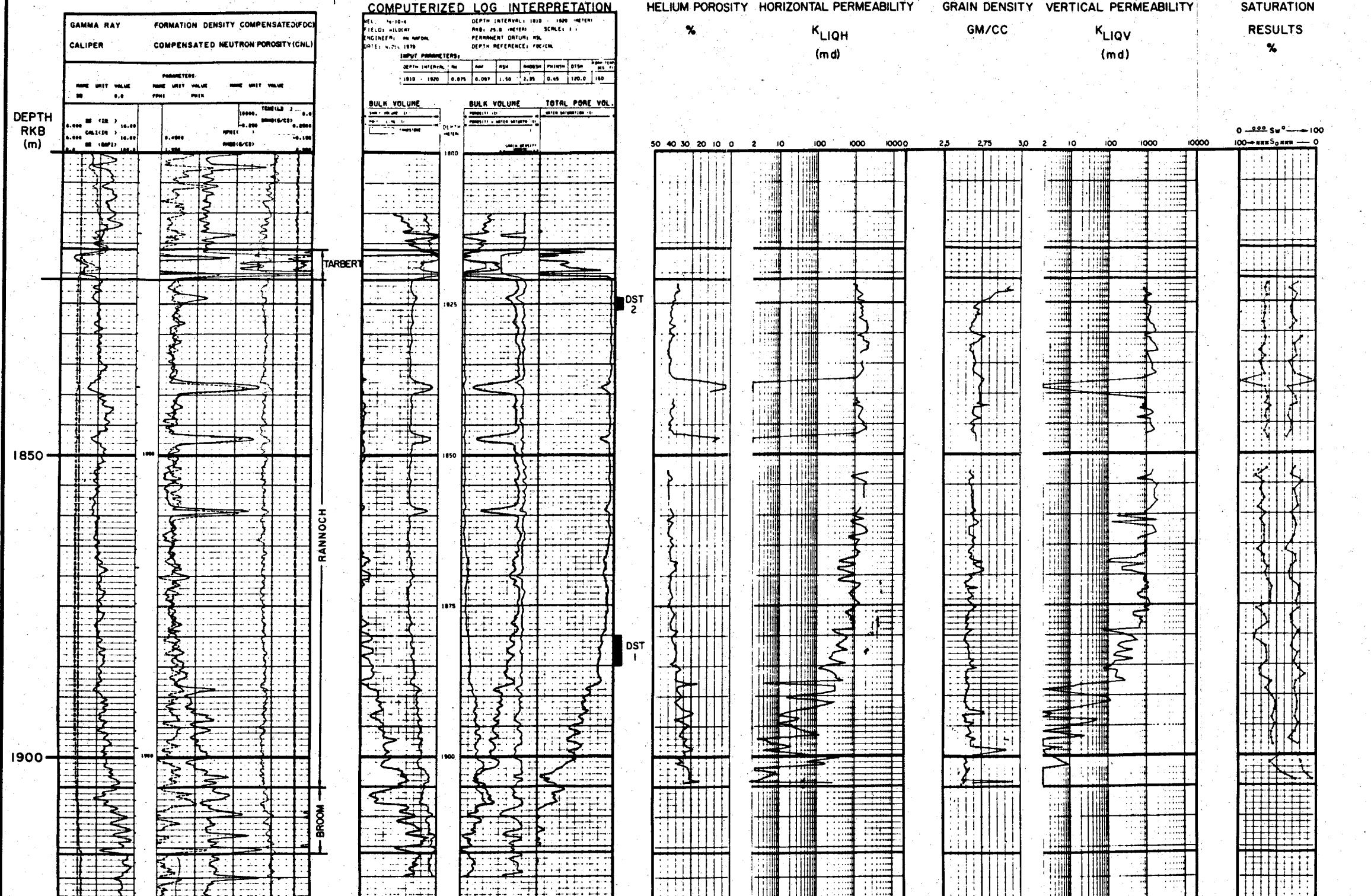
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°F

## APPENDIX A5

## SUMMARY LOG WELL 34/10-4

## BRENT FORMATION



## DST DATA

DST no. 1  
Interval: 1880 - 1885  
Choke: 20/64"  
Production: 1800 STBO/D  
No sand.

DST no. 2  
Interval: 1824 - 1826  
Choke: 20 + 32/64"  
Production: 5100 STBO/D  
No sand.

Location:  
61° 12' 15.12" N  
02° 13' 55.73" E

KBE elevation = 25m  
Water depth = 197m

Spudded: 12. Aug. 1979  
Rig released: 17. Oct. 1979

Dec. 1979  
PE/EVALTEK

JRd/AM

