

Denne rapport  
tilhører



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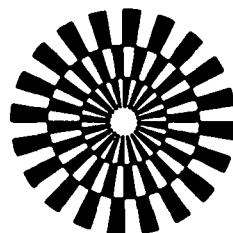
KODE WELL 31/2-11 nr 8

Returneres etter bruk

A/S NORSKE SHELL

WELL: 31/2-11

PVT - STUDY



**GECO**  
GEOPHYSICAL COMPANY  
OF NORWAY AS



A/S NORSKE SHELL

WELL: 31/2-11

PVT - STUDY

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Reservoir Fluid Study  
Well: 31/2-11  
Recombined Sample  
Bottle no. 22478 (oil)  
and no. A 4964 (gas)

## S U M M A R Y

This report present the results of a PVT-study of a recombined sample of reservoir fluid from well: 31/2-11.

Separator gas and liquid samples were analysed and recombined according to a GOR of 62.2 Sm<sup>3</sup>/m<sup>3</sup>.

Single-stage flash, gas composition, viscosity, differential liberation, pressure-volume relations and separator tests were determined on the recombined sample at 67.8°C.

Main results are:

Bubble point at 67.8°C	:	157.0 barg
Density at bubble point	:	794.2 kg/m <sup>3</sup>
Compressibility at bubble point:		1.21 x 10 <sup>-4</sup> bar <sup>-1</sup>
Viscosity at bubble point	:	1.545 cp

From single-stage flash:

Gas/oil ratio	:	66.3 Sm <sup>3</sup> /m <sup>3</sup>
Bo at bubble point	:	1.189 m <sup>3</sup> /m <sup>3</sup>
Density of oil at 15°C:	:	886.7 kg/m <sup>3</sup>

Standard conditions: for gas volumes = 15°C and 1 atm  
for oil volumes = 15°C and atmospheric pressure



## SAMPLE

The recombination samples, bottle 22478 (oil) and no. A-4964 (gas) were supplied by A/S NORSKE SHELL and contained fluids sampled from the production separator on well 31/2-11. Separator conditions were 90 psig and 92°F. Opening pressure of separator gas sample at 35°C were 91 psig. Bubble point of separator oil sample was 87 psig at 33.3°C.

## LABORATORY PROCEDURE

### PVT-analysis

Pressure-volume relations were determined in a Ruska visual liquid PVT cell-oil bath at 67.8°C. Single flash to 150°C and atmospheric pressure and separator tests were performed in a Ruska Flash Separator. Gas volumes were measured by a Ruska Gasometer. Gas samples for analysis were collected in a gas sampling tube (250 ml) connected between the separator and gasometer.

### Gas analysis

Gas analysis up to and including nonanes was carried out with a Perkin Elmer Sigma gaschromatograph equipped for automatic gas analysis and column switching. The analysis was carried out isothermally at 65°C with FID and hot wire detector at 150 and 100°C respectively. Columns were 1: 15% squalane on Chromosorb P, 2: Poropak N, 3: Molecular Sieve 5 A.

The C<sub>6+</sub> fraction is determined by backflushing from column 1 through the FID detector. The separation of the hydrocarbon groups in this fraction is performed in a column filled with 10% SP-2100 on Supelcoport in another P.E. Sigmagaschromatograph, temperature programmed from 40 to 180°C. The determination is done by a FID at 190°C.

The system is calibrated before and after each working day with a calibration gas (Air Products) containing hydrocarbons from methane through pentane, and helium, nitrogen and carbondioxide.

### Density and Molecular Weight

Density of stock tank oil was determined at 15°C with an AP Paar Density meter, calibrated with dry air and distilled water before each measurement. Molecular weight was determined by freezing point depression of benzene.



Viscosity

Liquid viscosities were determined with a ROP rolling ball viscosimeter calibrated with viscosity standards from Cannon Instrument Co.

Gas viscosities are calculated from molecular composition according to Lee, A.L., Gonzales, M.H. and Eakin, B.E., J. Petr. Techn. 1966, 977-1000.



FLASH SEPARATION OF SEPARATOR LIQUID  
TO STOCK TANK CONDITIONS.

Flash conditions : 100 barg, 33.3°C to atmosphere and 15°C.

Gas oil ratio : 2.20 sm<sup>3</sup>/m<sup>3</sup>

Gas gravity : 0.984

Bo at 100 barg : 1.026

Bo at bubble point : 1.033

Density of oil at 15°C : 885.1 kg/m<sup>3</sup>  
28.37 °API

Density of separator liquid  
at bubble point : 859.4 kg/m<sup>3</sup>

Molecular weight of oil : 233

Molecular weight of C<sub>10</sub>+ (calculated) : 294

Separator gas properties calculated from molecular composition.

Gas gravity (air = 1) : 0.679

Compressibility factor : 0.9836

MOLECULAR COMPOSITION OF SEPARATOR LIQUID, SEPARATOR  
GAS AND MATHEMATICALLY RECOMBINED RESERVOIR FLUID.

Component	Stock tank oil (mol %)	Gas from separator liq. (mol %)	Recombined separator liq. (mol %)	Separator gas (mol %)	Recombined reservoir fluid (mol %)
Nitrogen		0.27	0.01	0.65	0.27
Carbon dioxide		3.14	0.07	1.66	0.71
Methane		51.14	1.22	85.45	35.19
Ethane	0.43	24.95	1.02	7.80	3.76
Propane	0.94	9.67	1.15	1.85	1.43
iso-Butane	1.55	4.35	1.62	1.00	1.37
n-Butane	0.62	2.86	0.68	0.30	0.52
iso-Pentane	1.69	1.39	1.68	0.35	1.15
n-Pentane	0.31	1.05	0.33	0.06	0.22
Hexanes	4.99	0.61	4.88	0.42	3.08
Heptanes	11.85	0.40	11.58	0.40	7.07
Octanes	5.06	0.13	4.94	0.05	2.97
Nonanes	3.35	0.04	3.27	0.01	1.95
Decanes plus	69.21	0.00	67.55	0.00	40.32



FLASH OF RECOMBINED RESERVOIR FLUID TO STOCK TANK CONDITIONS

Flash conditions : 300 barg, 67.8°C to atmosphere and 15°C.

Gas oil ratio	: 66.3    sm <sup>3</sup> /m <sup>3</sup>
Bo at 300 barg	: 1.171    m <sup>3</sup> /m <sup>3</sup>
Bo at bubble point	: 1.189    m <sup>3</sup> /m <sup>3</sup>
Density of oil at 15°C	: 886.7    kg/m <sup>3</sup> , 28.08 °API
Density at bubble point	: 794.2    kg/m <sup>3</sup>
Molecular weight of oil	: 236
Gas gravity (air=1)	: 0.679
Molecular weight of C <sub>10</sub> + (calculated)	: 285



FLASH OF RECOMBINED RESERVOIR LIQUID TO STOCK TANK CONDITIONS.  
MOLECULAR COMPOSITION OF RECOMBINED RESERVOIR FLUID.

Component	Stock tank oil (mol %)	Separator gas (mol %)	Recombined reservoir fluid (mol %)
Nitrogen		0.74	0.32
Carbon dioxide		1.64	0.70
Methane		83.07	35.49
Ethane	0.08	8.39	3.63
Propane	0.30	2.44	1.21
iso-Butane	0.68	1.49	1.03
n-Butane	0.34	0.48	0.40
iso-Pentane	1.16	0.58	0.91
n-Pentane	0.23	0.11	0.18
Hexanes	4.65	0.29	2.78
Heptanes	11.16	0.76	6.72
Octanes	5.41	0.01	3.10
Nonanes	2.26	0.00	1.30
Decanes plus	73.73	0.00	42.23



PRESSURE-VOLUME RELATION AT CONSTANT MASS OF RECOMBINED  
RESERVOIR LIQUID AT 67.8°C.

Pressure bar gauge	Relative volume V/V <sub>sat</sub>	Isothermal compressibility bar <sup>-1</sup>	"Y"
300.6	0.9847	0.94•10 <sup>-4</sup>	
274.5	0.9871	0.99•10 <sup>-4</sup>	
250.8	0.9895	1.03•10 <sup>-4</sup>	
226.9	0.9919	1.08•10 <sup>-4</sup>	
203.9	0.9948	1.12•10 <sup>-4</sup>	
176.1	0.9976	1.17•10 <sup>-4</sup>	
157.0	1.0000	1.21•10 <sup>-4</sup>	
128.5	1.0573		3.872
103.1	1.1461		3.580
77.3	1.3113		3.312
54.6	1.6066		3.092



DIFFERENTIAL LIBERATION OF RESERVOIR FLUID AT 67.8°C

Pressure (barg)	Oil Formation Volume Factor $B_o$ ( $m^3/m^3$ )	Solution gas oil ratio $Rs$ ( $Sm^3/m^3$ )	Gas Formation Volume Factor $B_g$ ( $m^3/Sm^3$ )	Density of sat oil ( $kg/m^3$ )
300.6	1.166			804.3
274.5	1.169			802.4
250.8	1.172			800.4
226.9	1.174			798.5
203.9	1.178			796.1
176.1	1.181			793.9
157.0	1.184	63.4		792.0 *)
133.5	1.164	53.7	$7.79 \times 10^{-3}$	799.2
109.6	1.147	45.1	$9.56 \times 10^{-3}$	805.2
82.2	1.126	34.5	$13.03 \times 10^{-3}$	813.0
53.4	1.104	23.6	$20.43 \times 10^{-3}$	821.6
32.4	1.088	15.4	$34.08 \times 10^{-3}$	827.7
17.9	1.074	9.3	$60.65 \times 10^{-3}$	833.9
0	1.047			845.8

Residual oil density at 15°C : 885.1  $kg/m^3$

\*) Density at bubble point from single flash: 794.4  $kg/m^3$

## DIFFERENTIAL LIBERATION OF RECOMBINED RESERVOIR FLUID AT 67.8°C

## MOLECULAR COMPOSITION OF LIBERATED GASES (MOL %)

Pressure/barg:	133.5	109.6	82.2	53.4	32.4	17.9	0
Nitrogen	1.64	1.22	0.87	0.52	0.36	0.17	0.00
Carbon dioxide	1.13	1.18	1.29	1.48	1.73	2.10	2.90
Methane	91.63	91.93	91.76	90.86	88.75	85.15	55.50
Ethane	3.49	3.71	4.17	5.08	6.64	9.02	25.07
Propane	0.64	0.66	0.72	0.87	1.15	1.69	8.64
iso-Butane	0.32	0.32	0.33	0.39	0.51	0.75	4.57
n-Butane	0.10	0.09	0.10	0.12	0.14	0.20	1.19
iso-Pentane	0.13	0.12	0.11	0.12	0.15	0.21	1.08
n-Pentane	0.02	0.02	0.02	0.02	0.03	0.04	0.16
Hexanes	0.14	0.11	0.10	0.09	0.12	0.15	0.43
Heptanes	0.63	0.52	0.38	0.30	0.34	0.42	0.39
Octanes	0.13	0.12	0.14	0.13	0.07	0.09	0.07
Nonanes	0.00	0.00	0.01	0.01	0.01	0.01	0.00
Decanes-plus	0.00	0.00	0.00	0.01	0.00	0.00	0.00

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DIFFERENTIAL LIBERATION OF RECOMBINED FLUID AT 67.8°C

(Gas properties calculated from molecular composition)

Pressure (barg)	Gas viscosity (cP)	Gas Gravity (Air=1)	Compressibility factor, Z
133.5	0.0161	0.630	0.8678
109.6	0.0152	0.625	0.8791
82.2	0.0143	0.624	0.8992
53.4	0.0136	0.629	0.9277
32.4	0.0131	0.644	0.9521
17.9	0.0127	0.673	0.9705
0	0.0114	0.919	0.9975



VISCOSITY OF RECOMBINED FLUID AT 67.8°C

Pressure (barg)	Viscosity (centipoise)
306.6	1.814
276.2	1.758
250.3	1.721
225.2	1.682
200.0	1.625
178.0	1.580
150.9	1.750
127.8	1.891
104.1	2.138
77.1	2.397
50.6	2.723



SEPARATOR TESTS OF RECOMBINED FLUID AT DIFFERENT PRESSURES  
AND AMBIENT TEMPERATURE

Separator conditions	Separator gas oil ratio $\text{sm}^3/\text{m}^3$	Bo $\text{m}^3/\text{m}^3$	Density of oil at 15°C $\text{kg}/\text{m}^3$	Gas gravity Air = 1
300 psig	20°C	64.8	1.162	0.658
200 psig	20°C	65.2	1.172	0.618
100 psig	20°C	63.5	1.178	0.629
50 psig	20°C	65.4	1.185	0.654
0 psig	15°C	66.3	1.189	0.679



SEPARATOR TESTS OF RECOMBINED FLUID AT DIFFERENT  
PRESSURES AND AMBIENT TEMPERATURE.

Molecular composition of liberated gases (Mol %)

Sep. pressure	300 psig	200 psig	100 psig	50 psig
Nitrogen	1.11	1.03	0.89	0.79
Carbon dioxide	1.59	1.44	1.53	1.63
Methane	87.22	90.71	89.37	86.72
Ethane	6.67	5.36	6.25	7.59
Propane	1.49	0.80	1.07	1.69
iso-Butane	0.63	0.30	0.44	0.80
n-Butane	0.35	0.09	0.13	0.25
iso-Pentane	0.23	0.08	0.11	0.21
n-Pentane	0.13	0.02	0.02	0.05
Hexanes	0.10	0.03	0.04	0.10
Heptanes	0.46	0.13	0.14	0.15
Octanes	0.02	0.01	0.01	0.02
Nonanes	0.00	0.00	0.00	0.00
Decanes plus	0.00	0.00	0.00	0.00

FIG. 1

PRESSURE-VOLUME RELATIONS OF  
RECOMBINED LIQUID AT 67.8 °C



$$P_b = 157.0 \text{ barg}$$

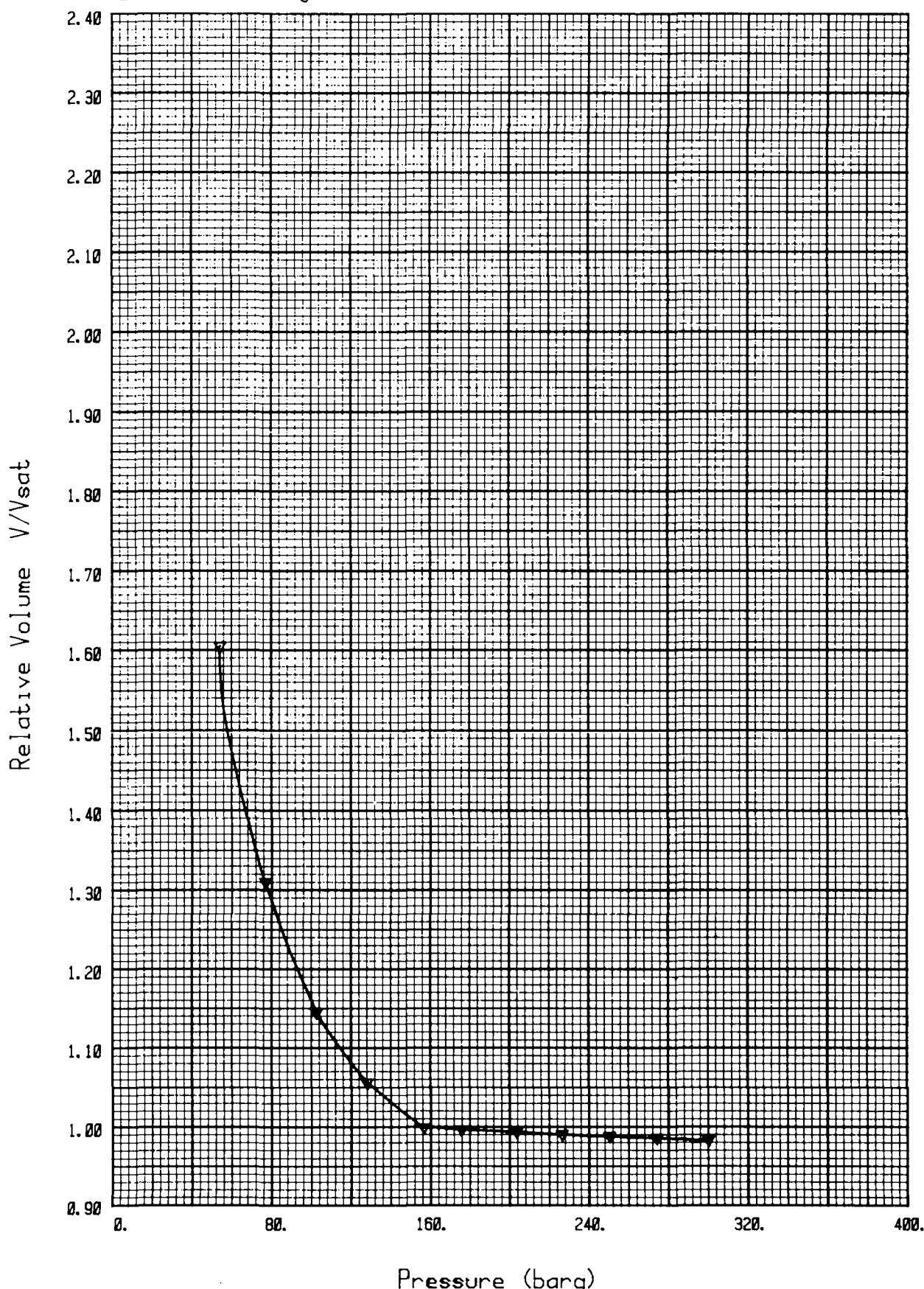


FIG. 2

DIFFERENTIAL LIBERATION AT 67.8°C  
OIL FORMATION VOLUME FACTOR

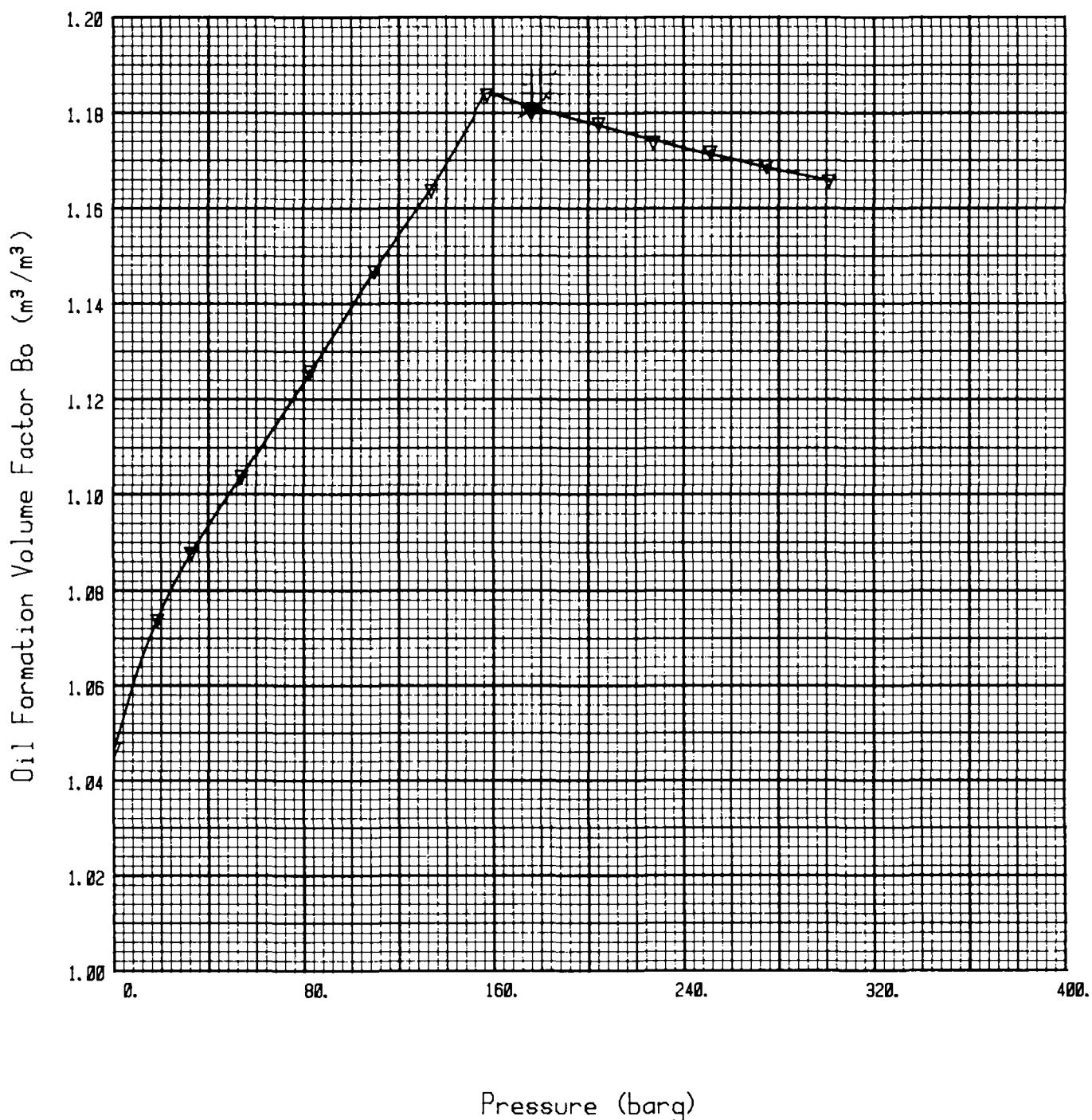
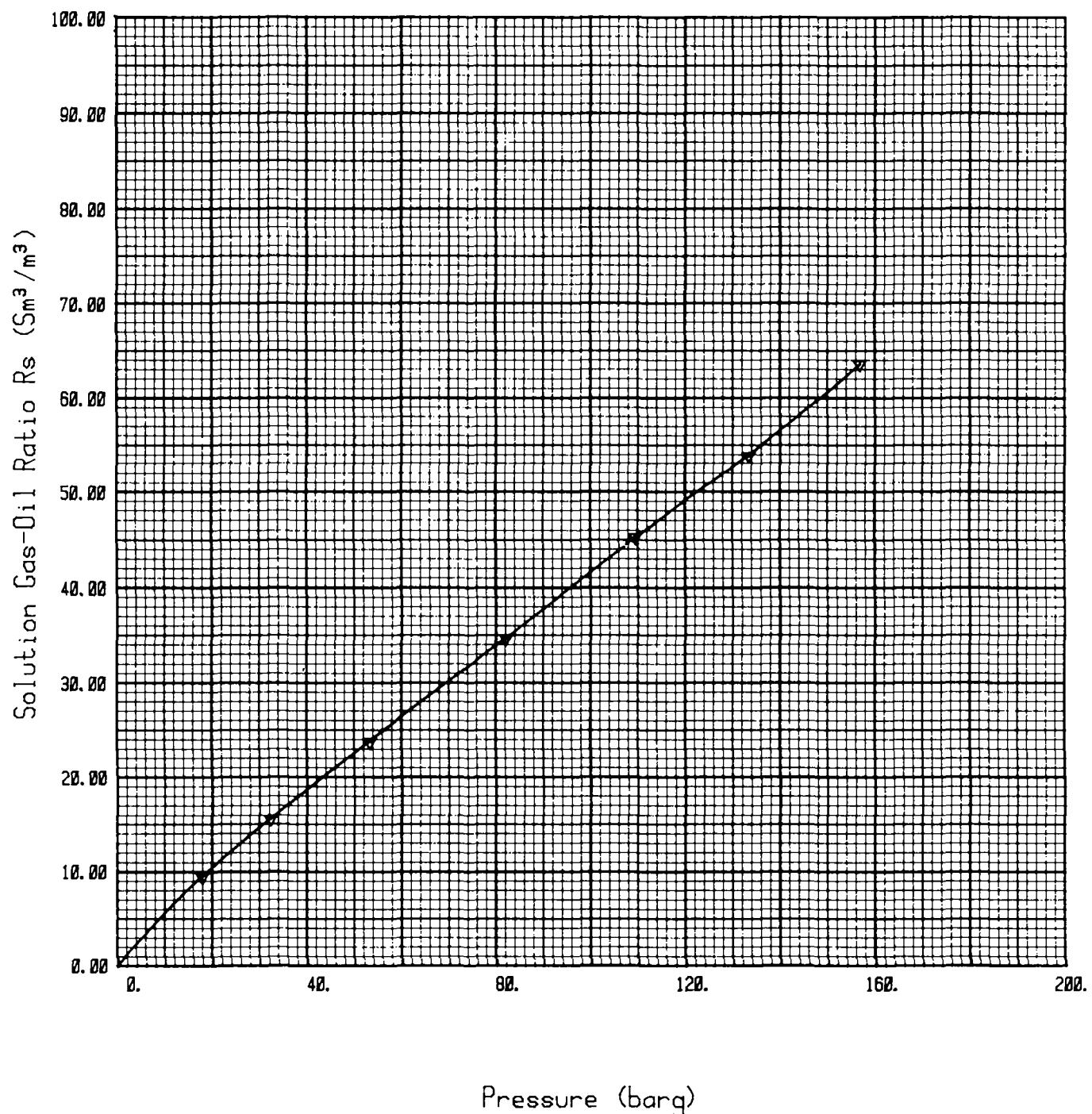


FIG. 3

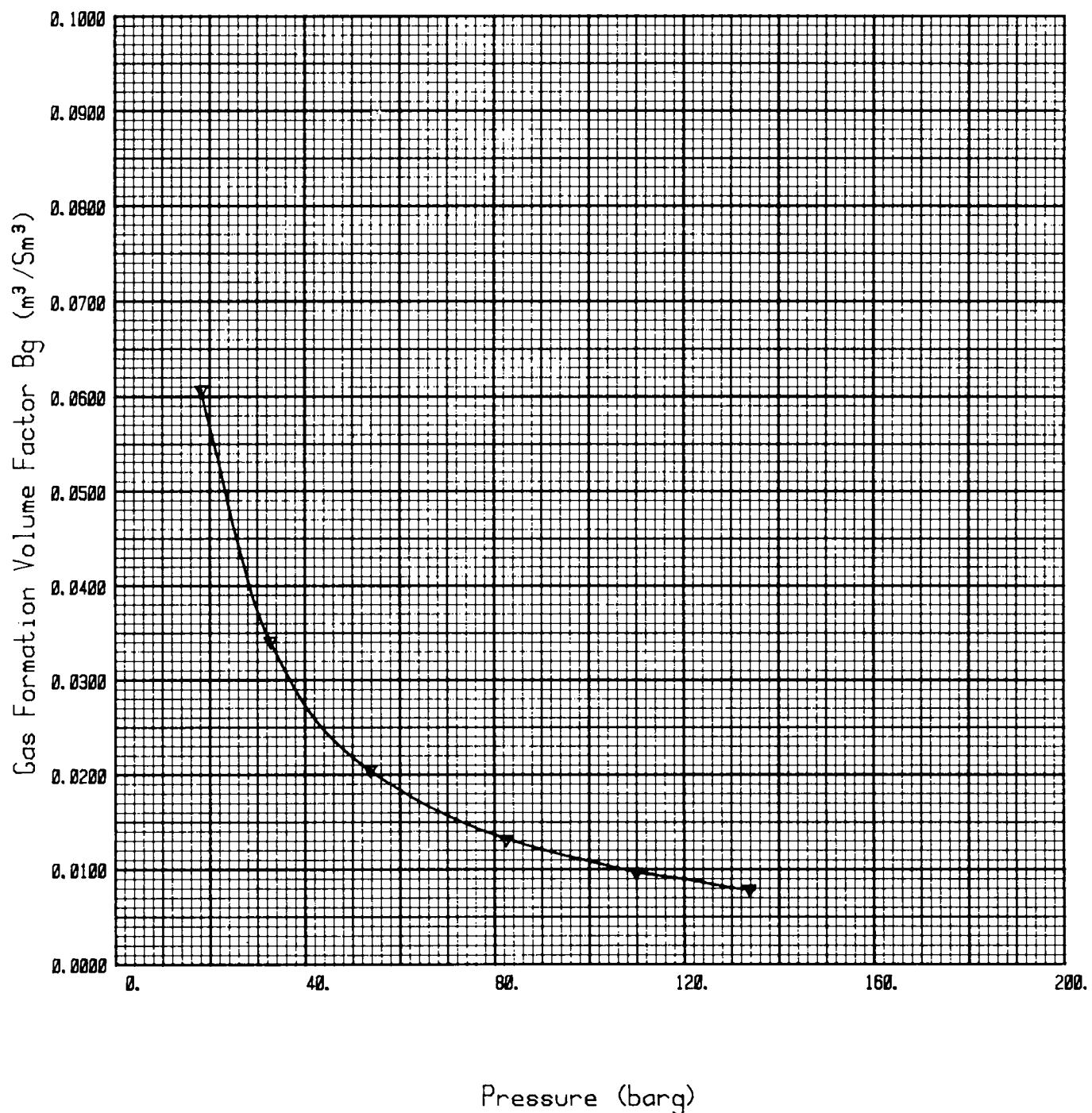
DIFFERENTIAL LIBERATION AT 67.8°C  
SOLUTION GAS-OIL RATIO



Pressure (barg)

FIG. 4

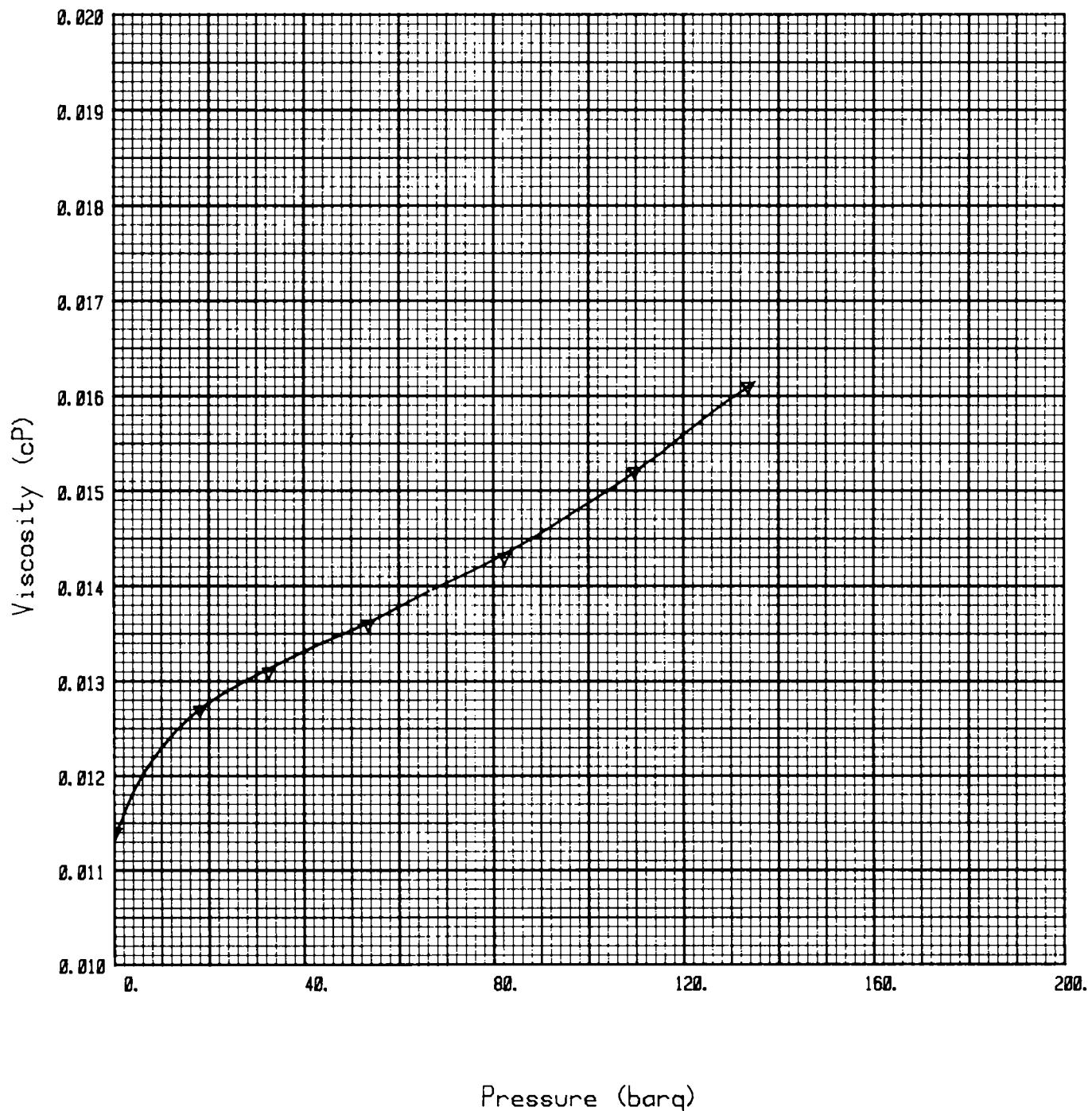
DIFFERENTIAL LIBERATION AT 67.8°C  
GAS FORMATION VOLUME FACTOR



Pressure (barg)

FIG. 5

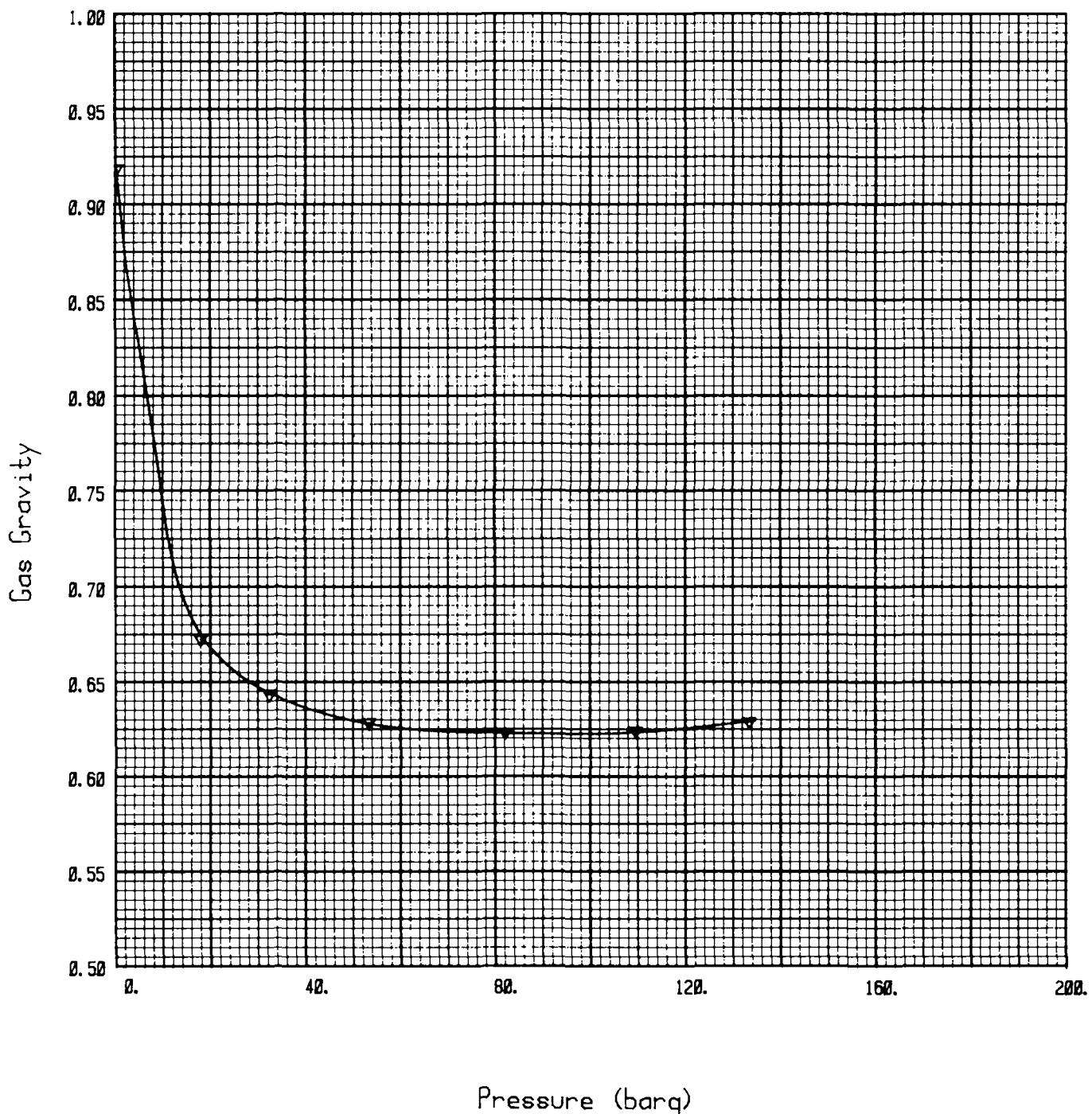
DIFFERENTIAL LIBERATION AT 67.8<sup>0</sup>C  
LIBERATED GAS VISCOSITY



Pressure (barg)

FIG. 6

DIFFERENTIAL LIBERATION AT  $67.8^{\circ}\text{C}$   
LIBERATED GAS GRAVITY



Pressure (barg)

FIG. 7

VISCOSITY OF RECOMBINED LIQUID AT 67.8 °C

